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**THE DEVELOPMENT AND OPTIMIZATION OF**  
**LIQUID PISTON STIRLING ENGINES**

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**1995-1996**


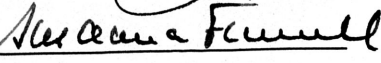
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# ABSTRACT

THE DEVELOPMENT AND OPTIMIZATION OF A LIQUID PISTON STIRLING ENGINE

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The liquid piston Stirling engine is an environmentally conscious technology developed to replace the electric heat pump and the gas furnace. Dr. Holtzapple's innovative modifications to existing Stirling engine technology has lead to promising results. Working engines based on this "bounce chamber" modification have been built; however, they have exhibited poor performance. Rather than investing more funds in equipment modifications, it was decided that the system should first be modeled. This would hopefully provide great insight into what needed to be done to improve engine performance.

A Visual Basic program was developed to model the engine. This graphically oriented program was designed specifically to give the user a clear understanding of how key engine parameters related to engine performance. A FORTRAN multidimensional global optimization program was also written because of the enormous computational requirements required for proper parameter optimization. Results to date show a nine fold increase in engine power. More trials are required before the engine parameters are fully optimized and trends are developed.

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# INTRODUCTION

## REPORT OVERVIEW

The two primary purposes of this report are as follows:

- to present how computer programs were developed to model and optimize a liquid-piston Stirling engine
- to present how to use these programs

Although a summary of the results generated by these programs will be presented, a rigorous analysis of the data and its implications is beyond the scope of this report.

## HISTORY OF STIRLING ENGINE TECHNOLOGY

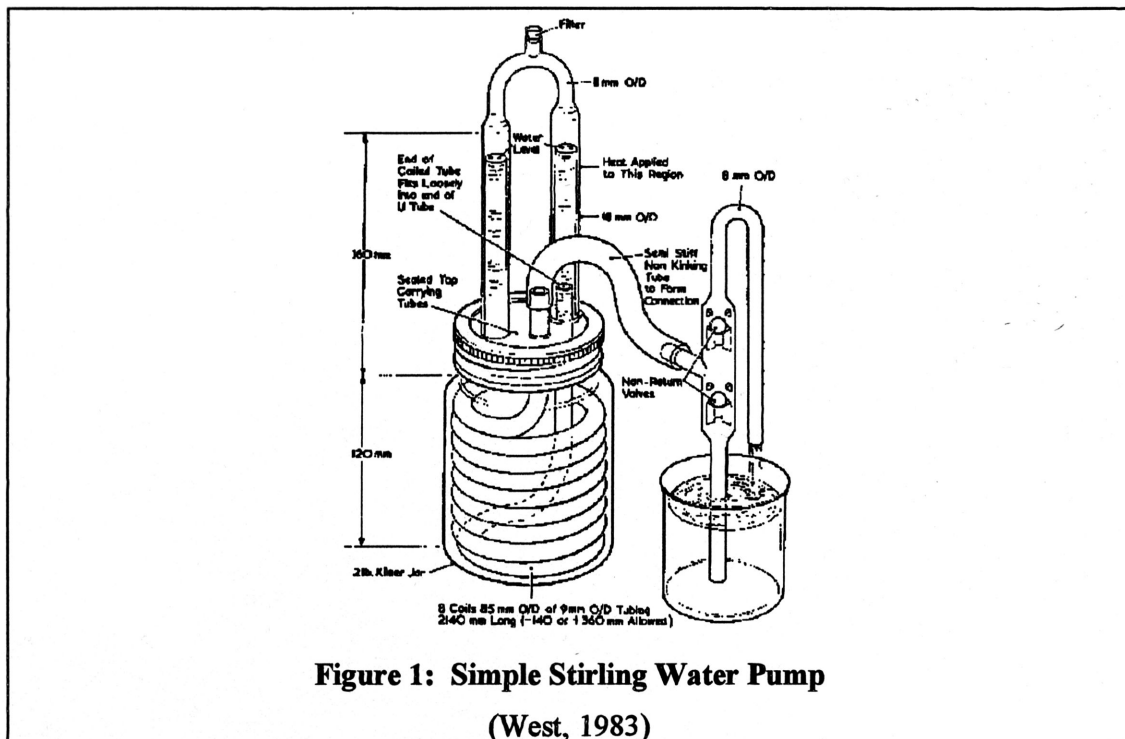
As early as 1698, Thomas Savery developed a commercial business out of heat engines used to pump water (West, 1983). Years later in 1853, Sir William Thomas, Lord Kelvin, formally derived and documented the fact that engine-driven heat pumps could be designed. In the first half of the nineteenth century, Robert Stirling conceived and designed hot-air engines. Engines based on the Stirling cycle named after him have been developed; however, heat pump and refrigeration applications have not been given much attention. The commercial success of Stirling-cycle heat pumps has been limited to cryogenic applications, where they have technological advantages over other practical technologies (Wurm, 1990).

In the 1930's, technological advancements and market conditions were right for the development of small engine-driven air conditioning and heat pump equipment. A heat

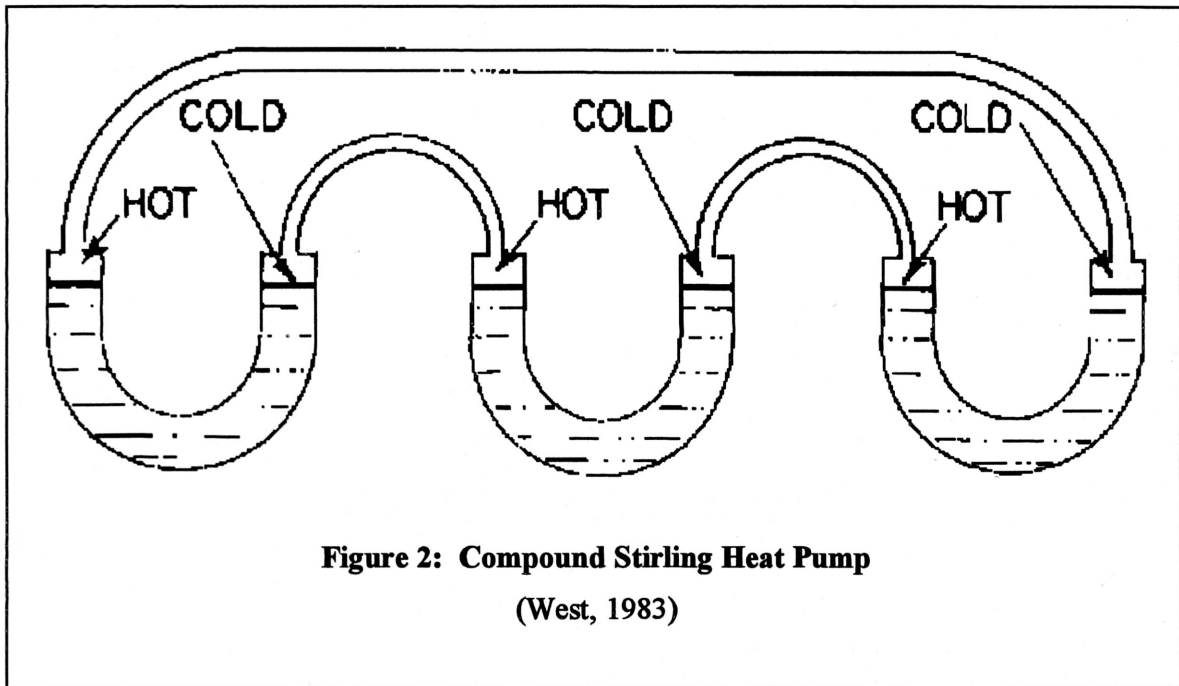
pump is driven by an engine. Attempts were made to integrate these two components into one unit. An integrated unit based on a Stirling cycle has potential efficiency advantages over other practical technologies. Unfortunately, coupling the heat pump with an engine resulted in high overall equipment costs. The cost savings from lower operating costs was not able to sufficiently compensate for the higher equipment costs. Therefore, less expensive vapor-compression heat pumps driven by electric motors dominate today's market (Wurm, 1990).

## APPLICATIONS

Two feasible applications for liquid piston Stirling engines include pumping fluids and replacing the electric heat pump or gas furnace. A simple Stirling engine designed for pumping water is shown in the following figure. The oscillating water columns in the U tube provide the pressure driving force for the water pump.



Stirling engines also have the potential to replace the electric heat pump and gas furnace. To date, no commercial heat pumps and few prototypes have been build serve this end. One potential engine design for this type of application is shown below.



**Figure 2: Compound Stirling Heat Pump**  
(West, 1983)

## ADVANTAGES OF STIRLING ENGINES

### *ENVIRONMENTAL*

#### **ALTERNATIVE ENERGY SOURCES**

In the United States, space conditioning accounts for approximately one third of all the fossil fuel consumed for purposes other than transportation (Wurm, 1990). In recent years, widespread concern that the use fossil fuels has been too profligate has grown.

These concerns are based on a variety of problems commonly associated with fossil fuels, such as global warming and pollution. Only heat is required to power a Stirling engine. This heat could come from a variety of more environmentally friendly sources, such as solar energy.

#### **SAFE WORKING FLUIDS**

Another important advantage of Stirling engine technology is that the working fluids could be composed of safe materials. The liquid pistons in the engine can be made out of water, and helium gas be used as an inter gas above the pistons.

#### *ENGINE DESIGN & MAINTENANCE*

Perhaps the liquid-piston Stirling engine's greatest advantage is its simplicity. It does not require accurately dimensioned cylinders and it permits great flexibility in mechanical design with relatively simple construction. If the liquid piston is water, then the engine and pump can even be integrated into a single system (West, 1983). Liquid piston engines avoid the use of a sliding mechanical seal and have no moving parts. The engine is also self-starting. When the temperature is raised beyond some threshold level, the liquid begins to oscillate of its own accord (West, 1983).

#### *ECONOMIC*

Another problem with conventional space conditioning is the dependence on fossil fuels and electricity for energy. Supply-side forces have played havoc with fossil fuel prices throughout the 1970's and 1980's. Electricity is also an expensive energy supply



for conventional space conditioning equipment. For these reasons, energy should be used as efficiently as possible.

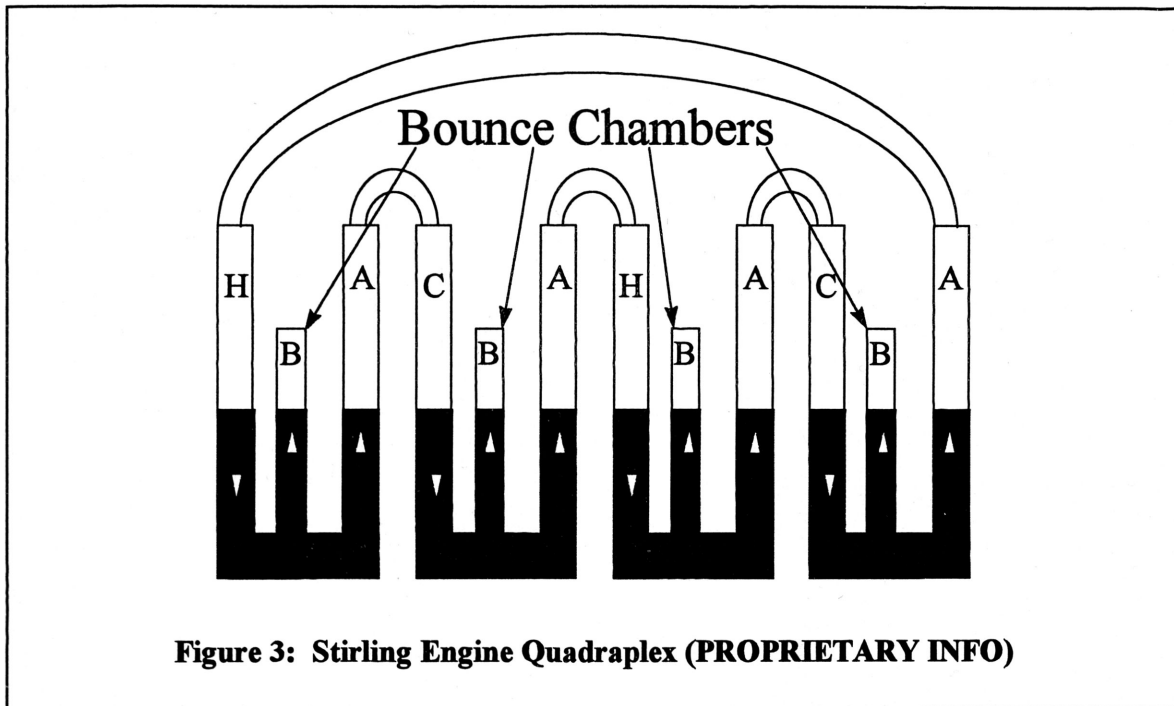
In principle, heat pumps offer the prospect of efficiencies that cannot be matched by any other means. In fact, the Stirling cycle is equivalent to a Carnot cycle in thermodynamic efficiency. However, the perceived advantages of the new designs have not yet been impressive enough to overcome the large capital investments required for mass production.

## PROJECT HISTORY

Dr. Holtzapple first began working with Stirling engines in the mid 1980's while in the U.S. Army. There, he worked on developing a portable cooling unit to be used by infantry. Over the years, he has developed new theories and has built a few functional Stirling engines.

Recently, experiments with a four U-tube design of the Stirling heat pump were performed by Martini. His design exhibited poor performance because the heat pump and the engine were  $180^\circ$  out of phase. This meant the paths of compression and expansion traced the same curve on a P-V diagram. Thus, little or no work was produced by the engine. At low operating pressures, he determined that a slight chilling effect was obtainable; however, because the pressure was low, a negligible amount of work was produced (Nivarthi, 1993).

Holtzapple built an engine according to Martini's design, but it would not run. Later, he modified Martini's design by adding bounce chambers to the engine (see Figure 3).



**Figure 3: Stirling Engine Quadraplex (PROPRIETARY INFO)**

With the addition of bounce chambers, the engine ran, but did not exhibit cooling.

Experiments showed that the expected improvements in engine performance were not obtained because the heat pump and engine were still out of phase. Before more capital was spent on equipment modifications, a FORTRAN computer model was written to optimize engine parameters. Although the computer model of the heat pump with bounce chambers was written, optimal tuning parameters were not found. The difficulty of finding the values lies in the immense number of combinations that can be considered. As a result, the search for optimal tuning parameters is comparable to finding the proverbial needle in the haystack.

# THEORY

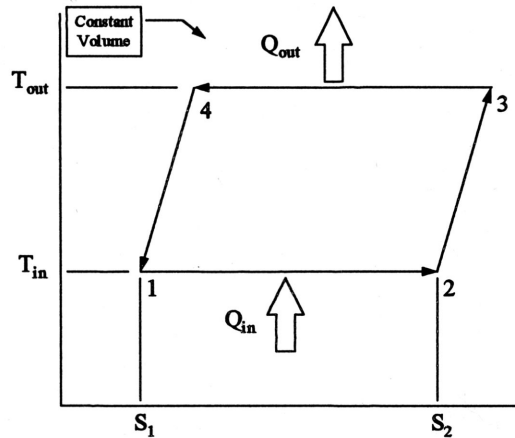
## STIRLING CYCLES & ENGINES

Most engineers do not understand the design of equipment based on Stirling cycles and the related Ericsson and Vuilleumier thermodynamic cycles because these cycles have not been in the mainstream of practical applications. The basic principle of the Stirling engine is simple. When a gas is heated, it tends to expand or, if confined in a closed vessel, to rise in pressure (West, 1983). This pressure, along with the force of gravity, cause the liquid columns to oscillate in the U-tubes (see Figure 3).

The following figure shows the temperature-entropy diagram for the Stirling heat pump cycle. The cycle consists of the following sequence of steps:

- 1 to 2            Isothermal expansion at low source temperature  $T_{in}$ , with heat input  $Q_{in}$
- 2 to 3            Isochoric (constant-volume) compression, with heat input  $Q_r$  from the regenerator
- 3 to 4            Isothermal compression at high sink temperature  $T_{out}$ , with heat output  $Q_{out}$
- 4 to 1            Isochoric expansion, with heat output  $Q_r$  stored in the regenerator

The net result is a cooling effect in the cold liquid piston. Reversing this process results in a Stirling engine cycle.

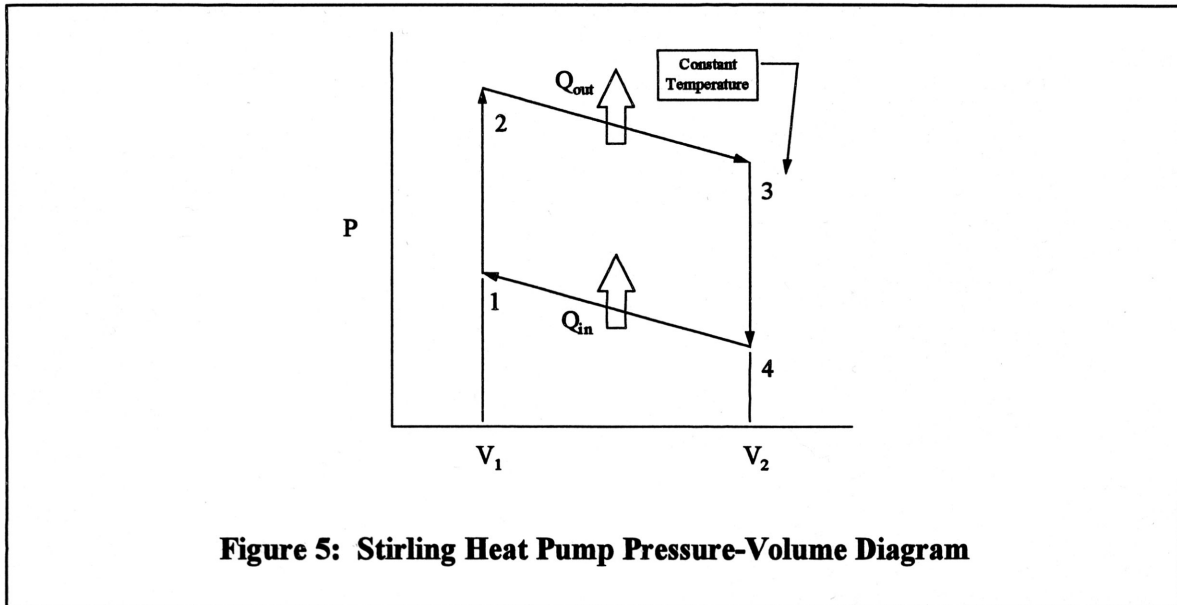


**Figure 4: Stirling Heat Pump Temperature-Entropy Diagram**  
(Wurm, 1990)

The next figure shows a pressure-volume diagram for a Stirling engine cycle. This cycle consists of the following sequence of steps:

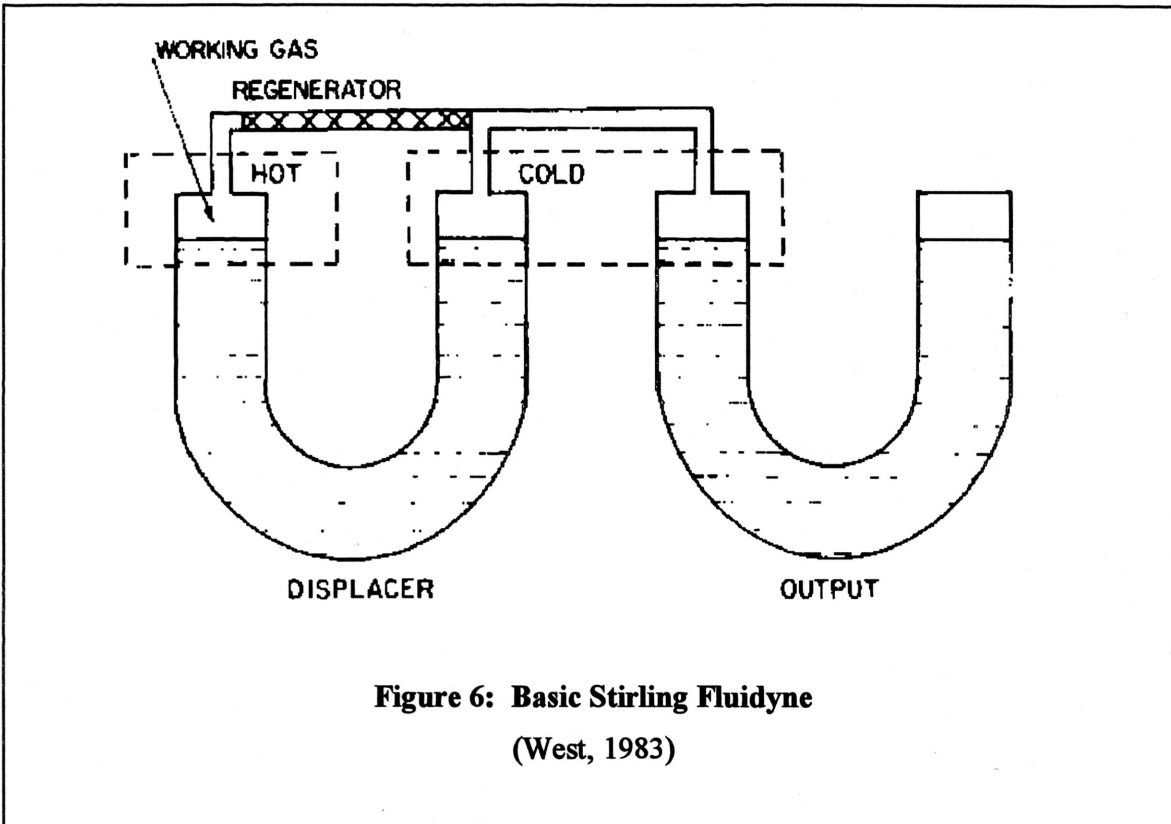
- 1 to 2        Isochoric (constant-volume) expansion, with heat input  $Q_r$  from the regenerator
- 2 to 3        Isothermal expansion at high sink temperature, with heat output  $Q_{out}$
- 3 to 4        Isochoric compression, with heat output  $Q_r$  stored in the regenerator
- 4 to 1        Isothermal compression at low source temperature, with heat input  $Q_{in}$

The amount of work produced by the engine is calculated by integrating the area inside this P-V curve.



**Figure 5: Stirling Heat Pump Pressure-Volume Diagram**

A basic Stirling fluidyne unit is presented in the next figure. As the displacer liquid column oscillates in its U tube, the gas above the liquid surface is transferred back and forth between hot and cold spaces. The resulting pressure variations act upon the liquid in the output column, causing it to move (West, 1983).



**Figure 6: Basic Stirling Fluidyne**  
(West, 1983)

## STIRLING ENGINE COMPONENTS

A schematic of a liquid piston Stirling engine with Holtzapfle's modifications is presented in the next figure. Each riser and bounce chamber is partially filled with water. The volume between the water and the top of the riser is occupied by helium, a high thermoconductive gas (Nivarthi, 1993).

A gas burner is attached to the hot leg of the engine. When ignited, the burner heats the gas and causes the gas to expand. This expansion temporarily forces water out the hot leg and into the bounce chamber. A fraction also fills the ambient leg in the adjoining heat pump. The gas in the heat pump is compressed and does work. Gravity then reverses the direction of the water flow. The expanding gas in the heat pump chills

the column as the water returns to the engine. This completes one cycle of the Stirling engine.

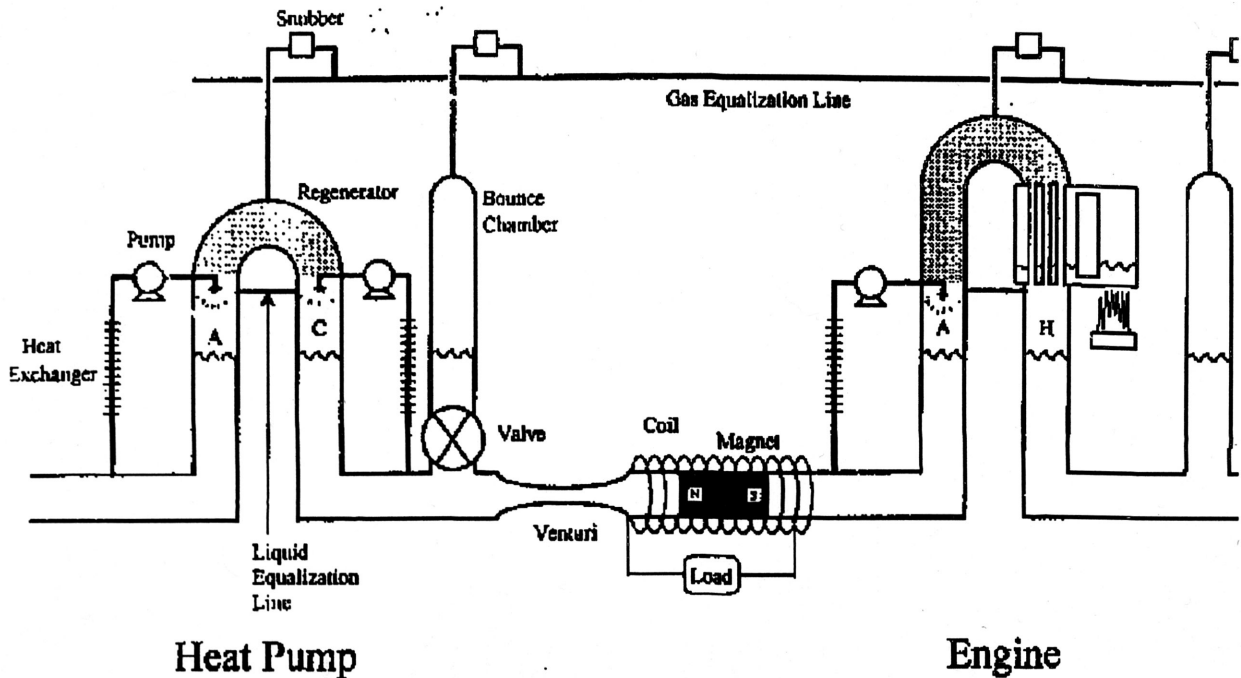


Figure 7: Stirling Engine Diagram (PROPRIETARY INFO)

### *BOUNCE CHAMBER*

The purpose of the bounce chamber is to help tune the engine. This “tuning” is similar to timing an automobile engine to fire so many degrees off top dead center. A poorly tuned engine will not produce much work. The bounce chamber is typically placed closer to the hot or cold leg of the engine or heat pump, respectively. This allows the hot or cold piston to have greater mobility than the ambient piston. This modification increases the engine’s potential power output.

## *REGENERATOR*

The heat pump and engine are composed of two risers connected by a regenerator elbow at the top. The regenerator is filled with metal shavings or wire and maintains the same pressure in both risers (Nivarthi, 1993).

The function of the regenerator may best be explained by first considering what would happen in its absence. As the displacer piston is moved from right to left, hot gas would flow through the connecting tube and into the cold end of the cylinder; when it arrived there, it would be cooled down and the heat extracted from it during this cooling process would have to be carried away by the cooling water or air which was being used to keep the right-hand end of the displacer cylinder at a low temperature. This heat would therefore be wasted - and, of course, wasting heat reduces the efficiency of the engine.

With the regenerator present, however, there is a steady fall in temperature along the regenerator, from left to right, as the gas gives up heat to the regenerator material. By the time the gas emerges into the cold end of the cylinder, therefore, it has already been cooled and no extra heat has to be carried away by the coolant.

When the cold gas flows back to the hot cylinder, its temperature gradually increases as it picks up the heat left in the regenerator during its journey to the cold end. This heat is thus not wasted; the regenerator operates as a kind of heat store, and the efficiency is therefore increased (West, 1983).



## *SNUBBER*

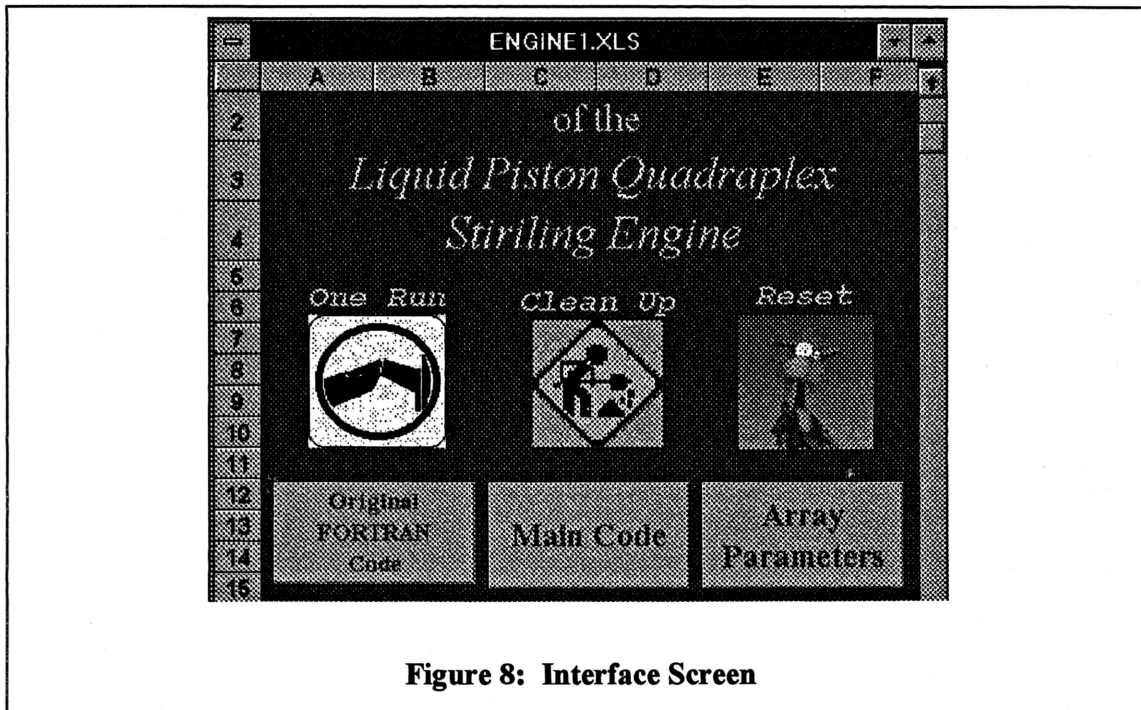
The snubber is simply a valve that connects each heat pump, engine, and bounce chamber to a gas equalization line. It maintains the same mean gas pressure in each riser over time (Holtzapple, 1993).

# DEVELOPMENT OF A LIQUID PISTON STIRLING ENGINE MODEL

The development of a computer program to model a liquid piston quadruplex Stirling engine began by converting an earlier program developed by previous students from FORTRAN to Microsoft Visual Basic. Visual Basic is a programming language embedded within Microsoft Excel. Essentially, Visual Basic is a programming language which can be used to write Windows applications.

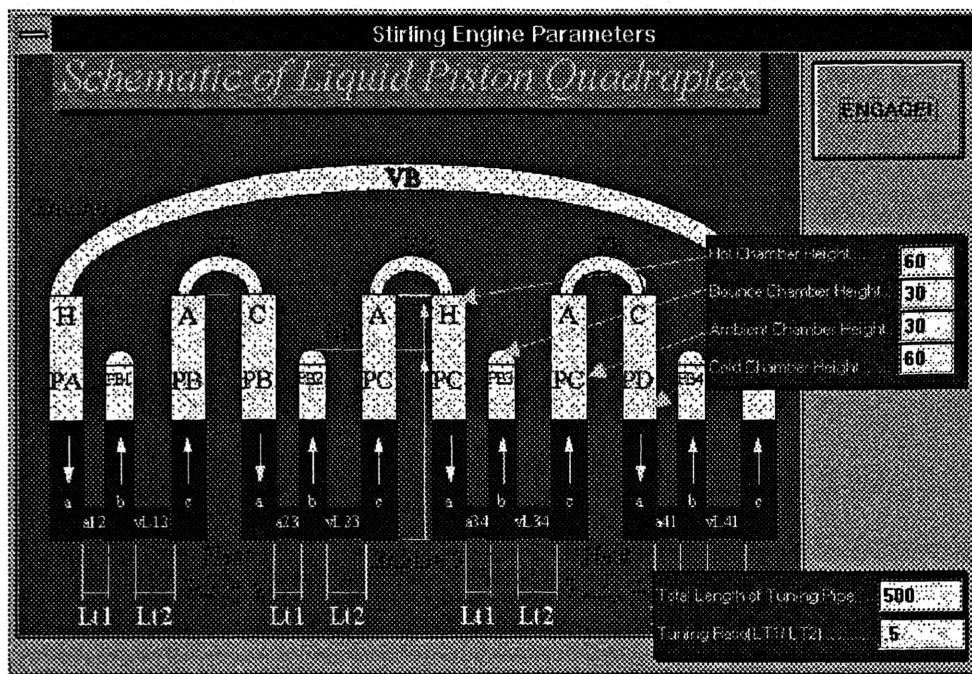
Excel Visual Basic offers several advantages over other programming languages. It is easy to learn and is very user friendly. This in turn helps to create a friendly application for the end user. Raw data generated by a Visual Basic program is readily convertible into graphical formats that are much easier to interpret and analyze. Real time parameter modifications can also be made while the program is running.

To show just how friendly Visual Basic model is, a brief overview of how to use it is presented here. When the file is opened from Excel, the program automatically takes the user to an interface screen, shown in Figure 8 below, where the user has several choices. To initiate a new run, the user clicks on the "One Run" button. This kicks the program off and asks the user a few questions about saving the generated data before continuing on to the next screen.



**Figure 8: Interface Screen**

Next, the user enters the engine parameters into the appropriate boxes on the schematic screen shown in Figure 9. Other less often modified engine parameters can be changed on the parameters screen (see Figure 10). This screen contains all the engine dimensions in addition to operating specifications and other constants. When the "Engage" button is pressed on the engine schematic screen the main program starts running. At any time before the engine reaches steady state, the user can quit and cancel the program or change views by pressing ESC. If the user wants the change views, the view changer screen shown in Figure 11 is pulled up. This screen offers a selection of views and options to change the speed of the oscillating model. One of the views available is presented in Figure 12. This screen displays the liquid piston heights for all the chambers and the current P-V diagram. With a little effort and patience, one can grasp how key design parameters of a Stirling engine effect its performance.



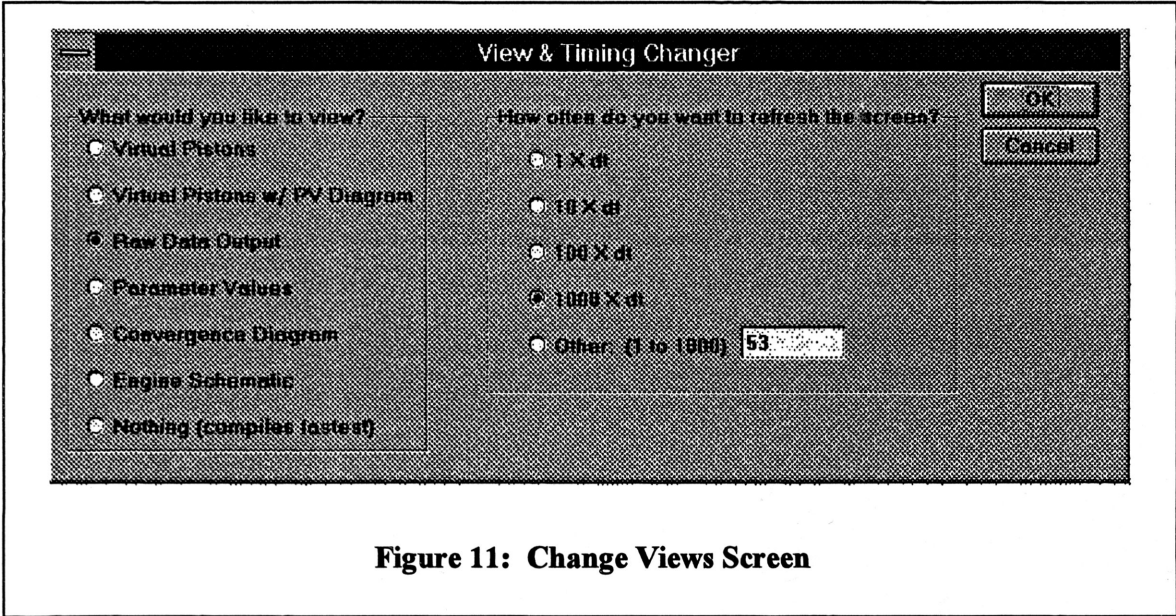
**Figure 9: Schematic Screen (PROPRIETARY INFO)**

ENGINE1.XLS

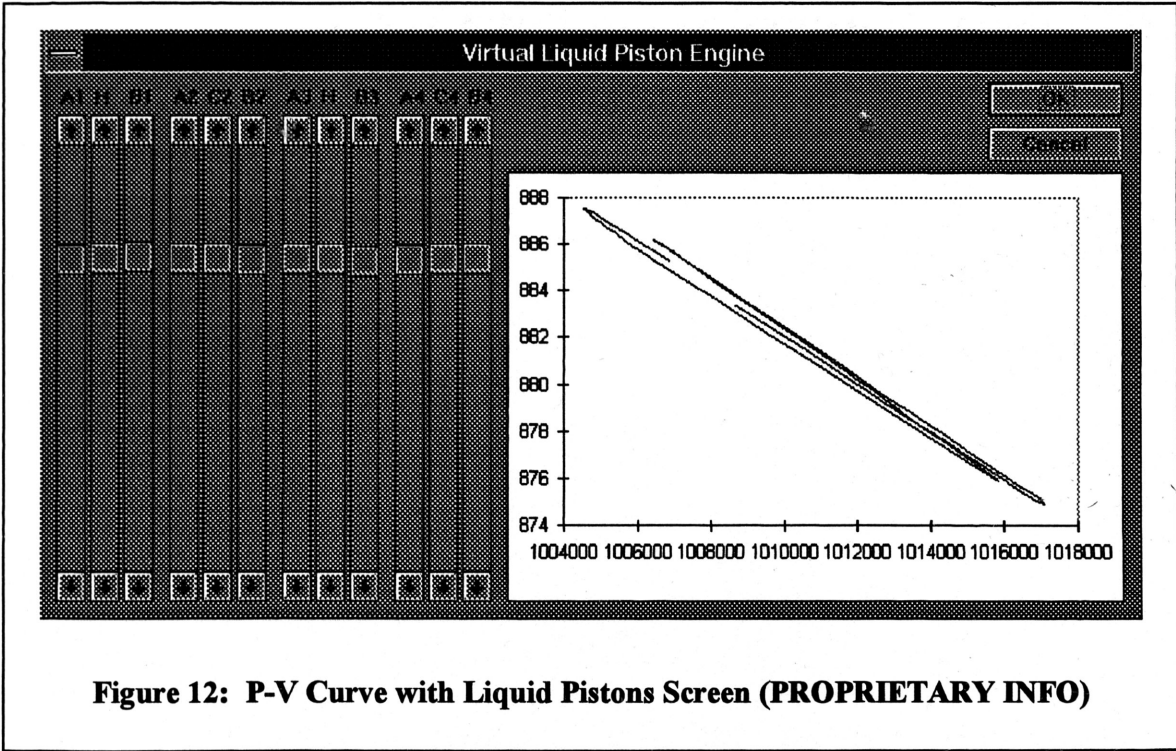
<i>Engine Parameter Values</i>					
<i>Time Parameters</i>			<i>Current</i>		
Time Interval or dt (sec)	0.001	0.001	Regenerator Volume(cm <sup>3</sup> )	98.1748	98.17
Update Interval	10	%	<i>Other Parameters</i>		
<i>Diameters(cm):</i>			Liquid Density(g/cm <sup>3</sup> )	1	1
Engine & Heat Pump	5.0	5.0	Gravitational Acceleration (cm/s <sup>2</sup> )	981	981
Bounce Chamber	4.5	4.5	Fanning Friction	0.03	0.03
<i>Chamber Heights(cm):</i>			Gas Constant (g/cm/s <sup>2</sup> *mol*K)	8.3E+07	8.3E+07
Hot Column	60.0	60.0	Mean Gas Pressure (dyne/cm <sup>2</sup> )	1010000	1010000
Cold Column	60.0	60.0	Mean Vol. Damping Factor	0.5	0.5
Ambient Column	30.0	30.0	<i>Starting Liquid Height (cm):</i>		
Bounce Column	30.0	30.0	Engine, Heat Pump, & B.C.	15.0	15.0
% Full	75%	80%	<i>Tuning Parameters</i>		
<i>Tuning Parameters</i>			<i>Temperatures(K)</i>		
Tuning Ratio L2	0.500	0.5000	Hot Column	537.78	537.78
Total Tuning Length	500.00	500.00	Cold Column	286	286
Length of tuning column 1	80.00	80.00	Ambient Column	316	316
Length of tuning column 2	100.00	100.00	Bounce Column	298	298

Parameter Values

**Figure 10: Engine Parameters Screen**



**Figure 11: Change Views Screen**



**Figure 12: P-V Curve with Liquid Pistons Screen (PROPRIETARY INFO)**

# DEVELOPMENT OF OPTIMIZATION CODE

With all of the errors worked out of the computer model, engine parameter optimization could begin. To simplify this overwhelming task, only eight key engine parameters were selected for optimization. They are as follows:

1. Tuning ratio - T1/T2
2. Total length of the tuning pipe
3. Height of the hot chamber
4. Height of the cold chamber
5. Height of the ambient chamber
6. Height of the bounce chamber
7. Dead volume in the regenerator
8. Water level in the shortest chamber (%)

Initial optimization efforts involved trying random values for each parameter by hand. It quickly became apparent that a structured optimization approach would be required to obtain good results. A brute force array, varying each parameter over a reasonable operating range, was then considered. However, since the optimal value of one parameter could possibly be influenced by a change in any other, a large array would be required. In fact, if there are no independent variables, testing twenty values for each of the eight key variables would call for an array with over 25 billion elements.

Autonomous optimization programs based on numerical methods were considered next. One attempt involved the development of a master-slave Visual Basic program. The master computer could evaluate results and delegate new tasks to several slave

computers over a network drive. This enabled a large number a computers to work in parallel toward a common solution.

Another, approach for optimizing the parameters involved using a “canned” FORTRAN routine based on numerical methods. A routine called Simann was selected from an internet library for this task. Even though this program was limited to serial operation, it had several significant advantages. Since it was FORTRAN based, the program ran faster. A single trial with the Visual Basic code takes approximately twenty minutes to half an hour. The FORTRAN version takes only five minutes. A FORTRAN program could also be run a larger computer, such as workstations and the University’s VAX clusters. Use of the Cray super computer is currently being looked into as well.

## SIMANN

Simann (“simulated annealing”) is a global optimization method that distinguishes between different local optima. Simann, SA, tries to find the global optimum, minimum or maximum, of an N-dimensional function. It moves both up and downhill and as the optimization process proceeds, it focuses on the most promising area. To start, it randomly chooses a trial point within the step length VM (a vector of length N) of the user selected starting point. The function is evaluated at this trial point and its value is compared to its value at the initial point.

In a maximization problem, all uphill moves are accepted and the algorithm continues from that trial point. Downhill moves may be accepted; the decision is made by the Metropolis criteria. It uses TC (temperature) and the size of the downhill move in a probabilistic manner. The smaller T and the size of the downhill move are, the more likely

that move will be accepted. If the trial is accepted, the algorithm moves on from that point. If it is rejected, another point is chosen instead for a trial evaluation. Each element of VM periodically adjusted so that half of all function evaluations in that direction are accepted.

A fall in  $T$  is imposed upon the system with the  $RT$  variable by  $T(i+1) = RT * T(i)$  where  $i$  is the  $i$ th iteration. Thus, as  $T$  declines, downhill moves are less likely to be accepted and the percentage of rejections rise. Given the scheme for the selection for VM, VM falls. Thus, as  $T$  declines, VM falls and SA focuses upon the most promising area for optimization.

Since the algorithm makes very few assumptions regarding the function to be optimized, it is quite robust with respect to non-quadratic surfaces. In fact, the degree of robustness can be adjusted by the user. Consult the appendix for further explanation concerning how to use the program efficiently.

## RESULTS AND DISCUSSION

As mentioned earlier, a rigorous analysis of the generated results and their implications will not be discussed in detail. Rather, a brief overview of the progress made to date will be presented along with future expectations.

In the following figures, an old and poorly tuned engine is compared to a design with new parameters from the SA optimization routine. The old design typically produced 10-15 watts of power per engine, while the new design produces 95-100 watts ( $P_{ave} = 1$  atm, Dia. of pipes = 5cm).

The following figure shows the liquid level in the three chambers of an engine. This data was collected for 2 seconds while the engine was oscillating at a steady state. Note that the new design's oscillations have a larger amplitude. This results in the production of more work.

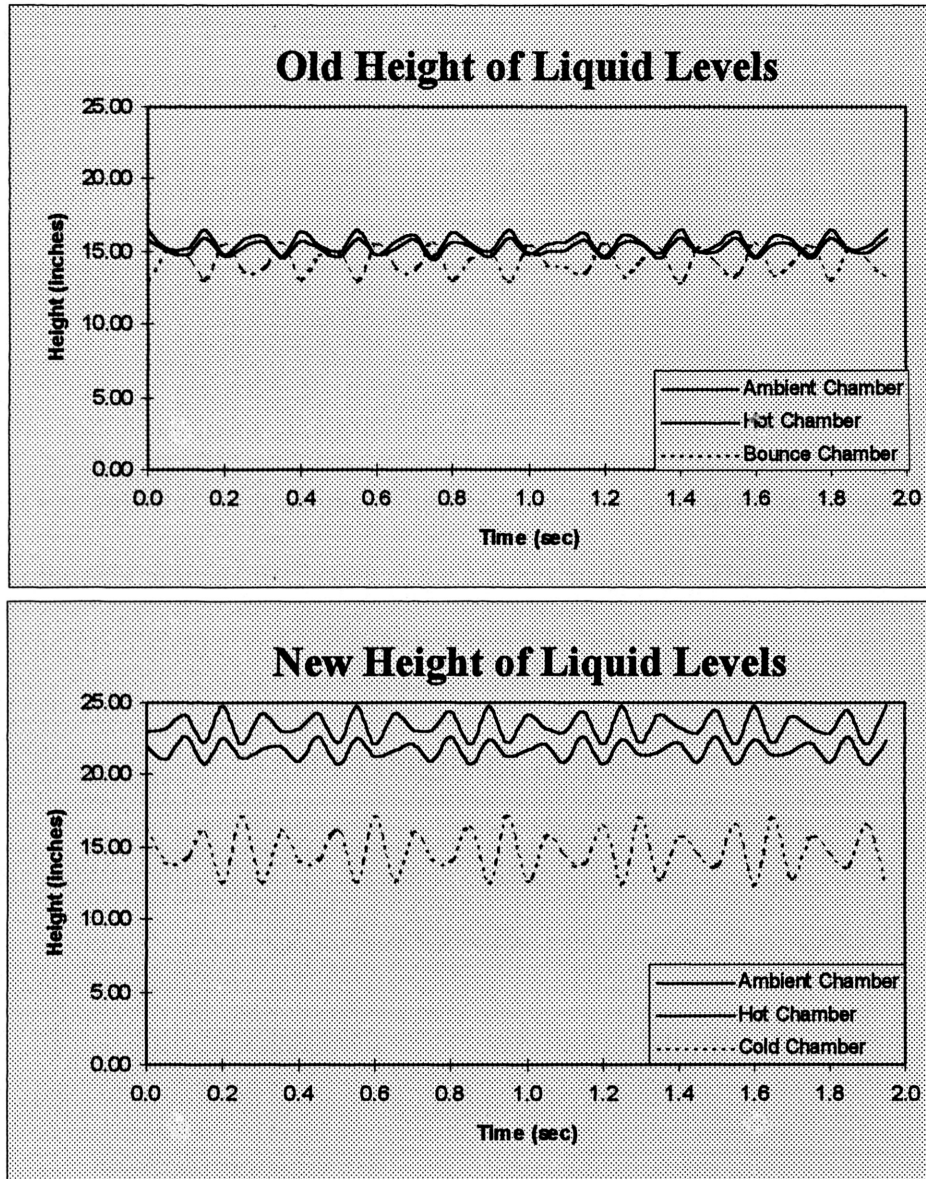
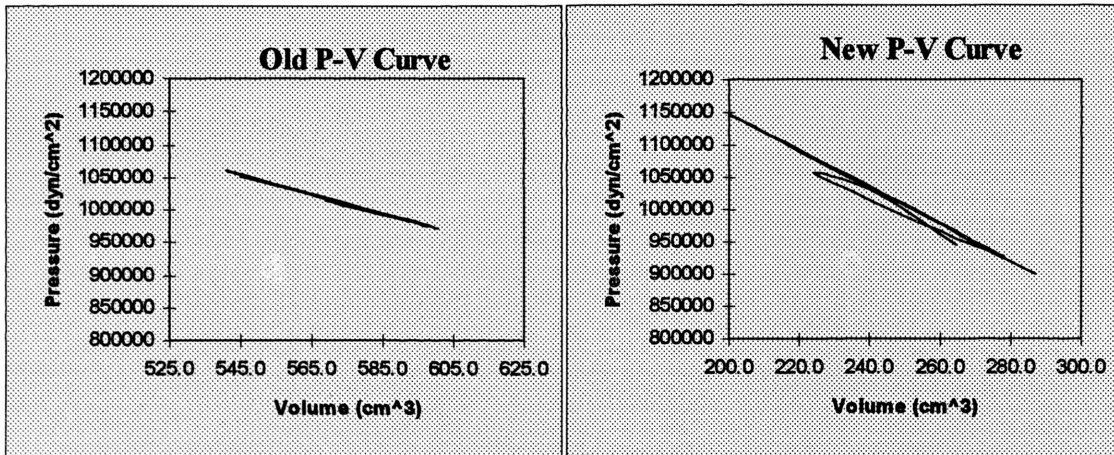


Figure 13: Optimal Liquid Level Comparison

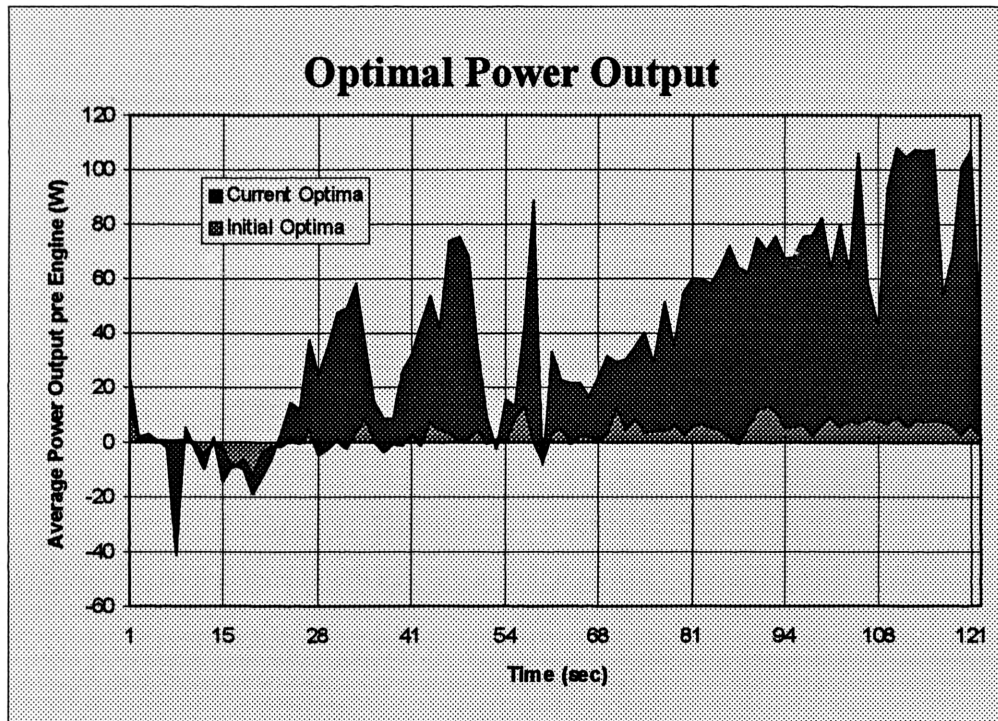


The next figure compares the P-V curves from each design. The larger area within the oval indicates that more work was produced by the new design parameters.



**Figure 14: Optimal P-V Curve Comparison**

Lastly, a comparison is made between the average power output for each engine design over time.



**Figure 15: Optimal Power Output Comparison**

## CONCLUSIONS

Just over three thousand combinations have been tried to date. The initial results are quite encouraging. The engine's power output has as increased nine fold since the optimization process began. Future plans include further optimization trials. Thousands of more are still required to develop accurate trends and correlations relating optimal engine performance to key parameter values. With the parameters optimized, modifications to existing hardware will them be implemented. Experiments with the modified engine will hopefully show that its performance has increased significantly.

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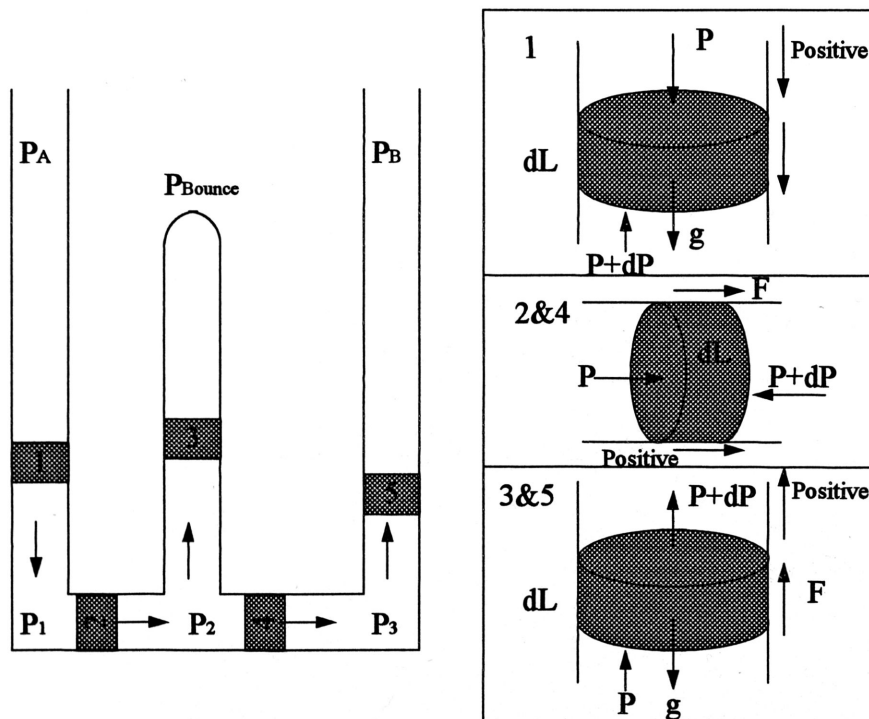
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# APPENDIX A: COMPUTER MODEL DEVELOPMENT

## SAMPLE CALCULATIONS

Presented here is one example (part of pages and pages) calculation that went into the development of this computer model.



**Figure 1A: Differential Fluid Element Diagram**

Proprietary Information !

The derivation of  $P_2$  is fairly complex. A system is first defined at the intersection of fluid elements 2, 3, and 4 shown in the above figure. By performing a mass balance on that system, an equation relating individual fluid element accelerations is obtained.

$$\dot{m}_1 = \dot{m}_3 + \dot{m}_5$$

$$\text{Equation 1: } (\rho A v_l)_1 = (\rho A_{BC} v_l)_3 + (\rho A v_l)_5$$

Subscript  $l$  refers to a liquid velocity. Since the fluid is assumed to be incompressible, the density variable in Equation 1 falls out.

$$\text{Equation 2: } (A v_l)_1 = (A_{BC} v_l)_3 + (A v_l)_5$$

Equation 2 is then differentiated with respect to time,

$$\left( A \frac{dv_l}{dt} \right)_1 = \left( A_{BC} \frac{dv_l}{dt} \right)_3 + \left( A \frac{dv_l}{dt} \right)_5$$

resulting in

$$(Aa)_1 = (A_{BC}a)_3 + (Aa)_5$$

By assuming  $A_1=A_5=A$ ,

$$\text{Equation 3: } a_1 = \frac{A_{BC}}{A} a_3 + a_5$$

### *DERIVATION OF THE LIQUID ACCELERATION EQUATIONS*

A force balance around volume element 1 is first defined.

$$\text{Equation 4: } F = (dm)a_1 = (dm)g + PA - (P + dP)A + i_1 \frac{1}{2} f \rho \pi D (dL) v_n^2$$

where,

$dm$  = mass of the differential volume element

$dL$  = length of the differential volume element

and

$i_1 = -1$  if element 1 has a positive velocity vector

$i_1 = 1$  if element 1 has a negative velocity vector

The first term in Equation 4 corresponds to the force due to gravity. The second is the force due to the pressure difference across the volume element. The last term accounts for the frictional force, which is always acting against the element's velocity vector. The mass of the differential volume element is equivalent to

$$dm = \rho A dL$$

Substituting this into Equation 4 and solving for  $dP$  yields

$$(\rho A dL) a_1 = (\rho A dL) g - A dP + i_1 \frac{1}{2} f \rho \pi D (dL) v_{11}^2$$

$$(\rho dL) a_1 = (\rho dL) g - dP + i_1 \frac{1}{2A} f \rho \pi D (dL) v_{11}^2$$

$$\text{Equation 5: } dP = \left( \rho g + i_1 \frac{1}{2A} f \rho \pi D v_{11}^2 - \rho a_1 \right) dL$$

By integrating Equation 5 from gas pressure  $P_A$  to liquid pressure  $P_1$ , or from the top to the bottom of the column, an equation representing the entire column is formulated.

$$\int_{P_A}^{P_1} dP = \left( \rho g + i_1 \frac{1}{2A} f \rho \pi D v_{11}^2 - \rho a_1 \right) \int_0^{L_1} dL$$

$$P_1 - P_A = \left( \rho g + i_1 \frac{1}{2A} f \rho \pi D v_{11}^2 - \rho a_1 \right) L_1$$

An expression for the liquid acceleration in the column is obtained by solving for  $a_1$ .

$$\rho g L_1 + \frac{i_1 2 f \rho v_{11}^2 L_1}{D} - \rho a_1 L_1 = P_1 - P_A$$

$$\text{Equation 6: } a_1 = \frac{P_A - P_1}{\rho L_1} + g + i_1 \frac{2 f v_{11}^2}{D}$$

In a similar manner, the liquid acceleration for volume element 2 is derived:

$$F = (dm)a_2 = PA - (P + dP)A + i_1 \frac{1}{2} f \rho \pi D (dL) v_{11}^2$$

where,

$dm$  = mass of the differential volume element

$dL$  = length of the differential volume element

and

$i_1 = -1$  if element 1 has a positive velocity vector

$i_1 = 1$  if element 1 has a negative velocity vector

$$(\rho A dL)a_2 = -A dP + i_1 \frac{1}{2} f \rho \pi D (dL) v_{11}^2$$

$$(\rho dL)a_2 = -dP + i_1 \frac{1}{2A} f \rho \pi D (dL) v_{11}^2$$

$$dP = \left( i_1 \frac{1}{2A} f \rho \pi D v_{11}^2 - \rho a_2 \right) dL$$

$$\int_{P_1}^{P_2} dP = \left( i_1 \frac{1}{2A} f \rho \pi D v_{11}^2 - \rho a_2 \right) \int_0^{L_2} dL$$

$$P_2 - P_1 = \left( i_1 \frac{1}{2A} f \rho \pi D v_{11}^2 - \rho a_2 \right) L_2$$

$$\frac{i_1 2 f \rho v_{11}^2 L_2}{D} - \rho a_2 L_2 = P_2 - P_1$$

$$\text{Equation 7: } a_2 = \frac{P_1 - P_2}{\rho L_2} + i_1 \frac{2 f v_{11}^2}{D}$$

The derivation of the liquid acceleration for volume element 3 is nearly identical to that of volume element 1. However, in accordance with the previously defined sign convention for positive motion, elements 1 and 3 are moving in opposite directions. Also,

the diameter of the bounce chamber is not assumed to be the same as the diameter of the heat pump and engine.

$$F = (dm)a_3 = -(dm)g + PA_{BC} - (P + dP)A_{BC} + i_3 \frac{1}{2} f \rho \pi D_{BC} (dL) v_{13}^2$$

where,

$dm$  = mass of the differential volume element

$dL$  = length of the differential volume element

and

$i_3 = -1$  if element 1 has a positive velocity vector

$i_3 = 1$  if element 1 has a negative velocity vector

$$(\rho AdL)a_3 = -(\rho AdL)g - AdP + i_3 \frac{1}{2} f \rho \pi D_{BC} (dL) v_{13}^2$$

$$(\rho dL)a_3 = -(\rho dL)g - dP + i_3 \frac{1}{2A} f \rho \pi D_{BC} (dL) v_{13}^2$$

$$dP = \left( -\rho g + i_3 \frac{1}{2A} f \rho \pi D_{BC} v_{13}^2 - \rho a_3 \right) dL$$

$$\int_{P_2}^{P_{Bounce}} dP = \left( -\rho g + i_3 \frac{1}{2A} f \rho \pi D_{BC} v_{13}^2 - \rho a_3 \right) \int_0^{L_3} dL$$

$$P_{Bounce} - P_2 = \left( -\rho g + i_3 \frac{1}{2A} f \rho \pi D_{BC} v_{13}^2 - \rho a_3 \right) L_3$$

$$-\rho g L_3 + \frac{i_3 2 f \rho v_{13}^2 L_3}{D_{BC}} - \rho a_3 L_3 = P_{Bounce} - P_2$$

$$\text{Equation 8: } a_3 = \frac{P_2 - P_{Bounce}}{\rho L_3} - g + i_3 \frac{2 f v_{13}^2}{D_{BC}}$$



The derivations for the acceleration of elements 4 and 5 are similar to the derivations of 1 and 2 respectively. Consequently, only the equations for the accelerations are presented here.

$$\text{Equation 9: } a_4 = \frac{P_2 - P_3}{\rho L_4} + i_5 \frac{2fv_{15}^2}{D}$$

$$\text{Equation 10: } a_5 = \frac{P_3 - P_B}{\rho L_5} - g + i_5 \frac{2fv_{15}^2}{D}$$

### *DERIVATION OF THE LIQUID PRESSURE EQUATIONS*

The derivation of liquid pressure  $P_1$  begins by equating Equation 6 and Equation 7.

$$a_1 = a_2$$

$$\frac{P_A - P_1}{\rho L_1} + g + i_1 \frac{2fv_{11}^2}{D} = \frac{P_1 - P_2}{\rho L_2} + i_1 \frac{2fv_{11}^2}{D}$$

$$\frac{P_A - P_1}{\rho L_1} + g = \frac{P_1 - P_2}{\rho L_2}$$

$$\frac{P_A}{\rho L_1} - \frac{P_1}{\rho L_1} + g = \frac{P_1}{\rho L_2} - \frac{P_2}{\rho L_2}$$

$$\frac{P_A}{\rho L_1} + g + \frac{P_1}{\rho L_2} = \frac{P_1}{\rho} \left( \frac{1}{L_2} + \frac{1}{L_1} \right)$$

$$\frac{P_A L_2 + g \rho L_1 L_2 + P_2 L_1}{\rho L_1 L_2} = P_1 \left( \frac{L_1 + L_2}{\rho L_1 L_2} \right)$$

$$\text{Equation 11: } P_1 = \frac{P_A L_2 + g \rho L_1 L_2 + P_2 L_1}{L_1 + L_2}$$

The derivation of  $P_3$  is similar to that of  $P_1$ . Equation 9 and Equation 10 are equated, and  $P_3$  is isolated.

$$\text{Equation 12: } P_3 = \frac{P_B L_4 + g \rho L_4 L_5 + P_2 L_5}{L_4 + L_5}$$

The derivation of the equation for  $P_2$  is more difficult. Equation 6, Equation 8, and Equation 9 are substituted into Equation 3 and  $P_2$  is isolated.

$$\alpha_1 = \frac{A_{BC}}{A} \alpha_3 + \alpha_5$$

$$\frac{P_A - P_1}{\rho L_1} + g + i_1 \frac{2f v_{11}^2}{D} = \frac{D_{BC}^2}{D^2} \left( \frac{P_2 - P_{Bounce}}{\rho L_3} - g + i_3 \frac{2f v_{13}^2}{D_{BC}} \right) + \frac{P_3 - P_B}{\rho L_5} - g + i_5 \frac{2f v_{15}^2}{D}$$

$$\frac{P_A - P_1}{\rho L_1} + g + i_1 \frac{2f v_{11}^2}{D} = \frac{D_{BC}^2}{D^2} \left( \frac{P_2 - P_{Bounce}}{\rho L_3} \right) - g \frac{D_{BC}^2}{D^2} + i_3 \frac{2f D_{BC} v_{13}^2}{D^2} + \frac{P_3 - P_B}{\rho L_5} - g + i_5 \frac{2f v_{15}^2}{D}$$

$$\frac{D_{BC}^2}{D^2} \left( \frac{P_2 - P_{Bounce}}{\rho L_3} \right) = \frac{P_A - P_1}{\rho L_1} + g + i_1 \frac{2f v_{11}^2}{D} + g \frac{D_{BC}^2}{D^2} - i_3 \frac{2f D_{BC} v_{13}^2}{D^2} - \frac{P_3 - P_B}{\rho L_5} + g - i_5 \frac{2f v_{15}^2}{D}$$

$$P_2 - P_{Bounce} = \frac{D^2 L_3}{D_{BC}^2 L_1} (P_A - P_1) + g \frac{D^2 \rho L_3}{D_{BC}^2} + i_1 \frac{2 \rho L_3 f D v_{11}^2}{D_{BC}^2} + g \rho L_3 - i_3 \frac{2 \rho L_3 f v_{13}^2}{D_{BC}} - (P_3 - P_B) \frac{L_3 D^2}{L_5 D_{BC}^2} + g \frac{D^2 \rho L_3}{D_{BC}^2} - i_5 \frac{2 \rho L_3 f D v_{15}^2}{D_{BC}^2}$$

$$P_2 = P_{Bounce} + \rho g L_3 \left( 2 \frac{D^2}{D_{BC}^2} + 1 \right) + 2 \rho L_3 f \left( i_1 \frac{D v_{11}^2}{D_{BC}^2} - i_3 \frac{v_{13}^2}{D_{BC}} - i_5 \frac{D v_{15}^2}{D_{BC}^2} \right) + P_A \left( \frac{L_3}{L_1} \right) \left( \frac{D^2}{D_{BC}^2} \right) +$$

$$P_B \left( \frac{L_3}{L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right) - P_1 \left( \frac{L_3}{L_1} \right) \left( \frac{D^2}{D_{BC}^2} \right) - P_3 \left( \frac{L_3}{L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right)$$

Substitutions for  $P_1$  and  $P_3$  in terms of  $P_2$  are then made using Equation 11 and Equation

12.

$$P_2 = P_{Bounce} + \rho g L_3 \left( 2 \frac{D^2}{D_{BC}^2} + 1 \right) + 2 \rho L_3 f \left( i_1 \frac{D v_{11}^2}{D_{BC}^2} - i_3 \frac{v_{13}^2}{D_{BC}} - i_5 \frac{D v_{15}^2}{D_{BC}^2} \right) + P_A \left( \frac{L_3}{L_1} \right) \left( \frac{D^2}{D_{BC}^2} \right) +$$

$$P_B \left( \frac{L_3}{L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right) - \left( \frac{P_A L_2 + g \rho L_1 L_2 + P_2 L_1}{L_1 + L_2} \right) \left( \frac{L_3}{L_1} \right) \left( \frac{D^2}{D_{BC}^2} \right) - \left( \frac{P_B L_4 + g \rho L_4 L_5 + P_2 L_5}{L_4 + L_5} \right) \left( \frac{L_3}{L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right)$$

$$P_2 \left( 1 + \left( \frac{L_B}{L_1 + L_2} \right) \left( \frac{D^2}{D_{BC}^2} \right) + \left( \frac{L_B}{L_4 + L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right) \right) = P_{Bounce} + \rho g L_3 \left( 2 \frac{D^2}{D_{BC}^2} + 1 \right) + 2 \rho L_3 f \left( i_1 \frac{Dv_{11}^2}{D_{BC}^2} - i_3 \frac{v_{13}^2}{D_{BC}} - i_5 \frac{Dv_{15}^2}{D_{BC}^2} \right) +$$

$$P_A \left( \frac{L_3}{L_1} \right) \left( \frac{D^2}{D_{BC}^2} \right) \left( 1 - \left( \frac{L_2}{L_1 + L_2} \right) \right) + P_B \left( \frac{L_3}{L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right) \left( 1 - \left( \frac{L_4}{L_4 + L_5} \right) \right) - \rho g L_B \left( \left( \frac{L_2}{L_1 + L_2} \right) + \left( \frac{L_4}{L_4 + L_5} \right) \right) \left( \frac{D^2}{D_{BC}^2} \right)$$

$$P_3 = \frac{P_{Bounce} + \rho g L_3 \left( 2 \frac{D^2}{D_{BC}^2} + 1 \right) + 2 \rho L_3 f \left( i_1 \frac{Dv_{11}^2}{D_{BC}^2} - i_3 \frac{v_{13}^2}{D_{BC}} - i_5 \frac{Dv_{15}^2}{D_{BC}^2} \right) + P_A \left( \frac{L_3}{L_1} \right) \left( \frac{D^2}{D_{BC}^2} \right) \left( 1 - \left( \frac{L_2}{L_1 + L_2} \right) \right) + P_B \left( \frac{L_3}{L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right) \left( 1 - \left( \frac{L_4}{L_4 + L_5} \right) \right) - \rho g L_B \left( \left( \frac{L_2}{L_1 + L_2} \right) + \left( \frac{L_4}{L_4 + L_5} \right) \right) \left( \frac{D^2}{D_{BC}^2} \right)}{\left( 1 + \left( \frac{L_2}{L_1 + L_2} \right) \left( \frac{D^2}{D_{BC}^2} \right) + \left( \frac{L_4}{L_4 + L_5} \right) \left( \frac{D^2}{D_{BC}^2} \right) \right)}$$

## APPENDIX B: VISUAL BASIC MODEL

```
Option Base 1
Option Explicit
'
'   Type Piston
'   Declares the variable type "Piston" used in calculating the mean
volume
    Counter(1 To 12) As Integer
    A1(0 To 20) As Single 'index '0' is reserved for the average
    A2(0 To 20) As Single 'index '0' is reserved for the average
    A3(0 To 20) As Single 'index '0' is reserved for the average
    A4(0 To 20) As Single 'index '0' is reserved for the average
    H1(0 To 20) As Single 'index '0' is reserved for the average
    C2(0 To 20) As Single 'index '0' is reserved for the average
    H3(0 To 20) As Single 'index '0' is reserved for the average
    C4(0 To 20) As Single 'index '0' is reserved for the average
    B1(0 To 20) As Single 'index '0' is reserved for the average
    B2(0 To 20) As Single 'index '0' is reserved for the average
    B3(0 To 20) As Single 'index '0' is reserved for the average
    B4(0 To 20) As Single 'index '0' is reserved for the average
End Type

Function Engine(Parameters() As Single, Results() As Single) As Integer
'*****Start Error Handler*****
    On Error GoTo ChangeViews
    Application.EnableCancelKey = xlErrorHandler

'*****
'*****      DECLARATION OF VARIABLES      *****
'*****      All units are expressed in CGS system      *****
'*****
'   Pi      -   Pi (any questions?)
Dim Pi As Single

'   g      -   gravitaional acceleration constant
Dim g As Single

'   f      -   Fanning friction factor
Dim f As Single

'   d      -   density of the working fluid (water)
Dim d As Single

'   R      -   gas constant
Dim R As Single

'   Dia***  -   Diameters for the following pipes:
'               -   Tuning pipes, Ambient, hot, and cold columns
```

```

'      Dia_BC - Bounce Chamber columns
Dim Dia, Dia_BC As Single

'      Area*** - Cross-sectional area for the following pipes:
'              - Tuning pipes, Ambient, hot, and cold columns
'      Area_BC - Bounce Chamber columns
Dim Area, Area_BC As Single

'      Dt      - time interval between iterations
Dim Dt As Single

'      L       - height of the bounce, ambient, hot, or cold columns
Dim LB, LA, LH, LC As Single

'      LL      - initial height of the water in all of the columns
Dim LL As Single

'      T*      - temperature of the following columns:
'              H - hot
'              A - ambient
'              C - cold
'              B - bounce
Dim TH, TA, TB, TC As Single

'      Pmean   - mean gas pressure in the gas equalization line
Dim Pmean As Single

'      VB      - volume of the regenerator between the ambient and
hot/cold columns
Dim VB As Single

'      Damp    - damping factor for mean gas volume calculations
Dim Damp As Single

'      L**     - height of liquid in the ambient, hot, cold, or bounce
chamber
Dim LA1, LH1, LB1, LA2, LC2, LB2, LA3, LH3, LB3, LA4, LC4, LB4 As Single

'      vl***   - liquid velocities in the columns. see figure 5 p. 15
Dim vl12a, vl12b, vl12c, vl23a, vl23b, vl23c As Single
Dim vl34a, vl34b, vl34c, vl41a, vl41b, vl41c As Single

'      Vo**    - volume of gas in each column
Dim VoH1, VoH3, VoC2, VoC4, VoB1, VoB2 As Single
Dim VoB3, VoB4, VoA1, VoA2, VoA3, VoA4 As Single

'      Vo**o   - initial volume of gas in each column
Dim VoH1o, VoH3o, VoC2o, VoC4o, VoB1o, VoB2o As Single
Dim VoB3o, VoB4o, VoA1o, VoA2o, VoA3o, VoA4o As Single

'      P**     - pressure of gas in each column
Dim PA, PB, PC, PD, PB1, PB2, PB3, PB4 As Single

'      P**o    - initial pressure of gas in each column
Dim PAo, PBo, PCo, PDo, PB1o, PB2o, PB3o, PB4o As Single

'      j       - mean gas volume counter
Dim j As Integer

'      MeanVol - set of variables used in the calculation of the mean
volume
'              of gas present in each chamber
Dim MeanVol As Piston

```

```

' t - time in seconds
Dim t As Single

' TimeInterval - determines how often the view is updated
Dim TimeInterval As Single

' m,n,u,v - counters used for the calculation of the area
'           inside the PV curve
Dim m, n, u, v As Integer

' p,w - counters used for the calculation of power output
'       from engines 1 & 3
Dim p, w As Integer

' Tick1,Tick3,TickPV - counters used for printing out the power
'                    generated from engines 1 & 3
Dim Tick1, Tick3, TickPV As Integer

' Number_of_cycles - counter used to average the power from x
cycles
Dim Number_of_cycles As Integer

' PP* - intermediate variables used in the calculation of
PA,PB,PC,PD
Dim PP1, PP2, PP3, PP4 As Single

' P1_,P2_,P3_ - pressure of liquid in column
Dim P1A, P1B, P1C, P1D As Single
Dim P2A, P2B, P2C, P2D As Single
Dim P3A, P3B, P3C, P3D As Single

' i_1,i_3,i_5 - direction of liquid in column
Dim i_1, i_3, i_5 As Single

' X*** - intermediate variables used in the calculation of
P1_,P2_,P3_
Dim X11, X12, X13, X14, X15, X21 As Single
Dim X16, X17, X18, X19, X110, X22 As Single
Dim X111, X112, X113, X114, X115, X23 As Single
Dim X116, X117, X118, X119, X120, X24 As Single

' Lt1,Lt2 - lengths of the tuning pipes
Dim Lt1, Lt2 As Single

' a*** - liquid acceleration terms for each column of water
Dim a12a, a23a, a34a, a41a As Single
Dim a12b, a23b, a34b, a41b As Single
Dim a12c, a23c, a34c, a41c As Single

' vl***o - liquid velocity buffer
Dim vl12ao, vl23ao, vl34ao, vl41ao As Single
Dim vl12bo, vl23bo, vl34bo, vl41bo As Single
Dim vl12co, vl23co, vl34co, vl41co As Single

' Chamber,Up,Down - counters used in the calculation of the mean gas
volume
Dim Chamber As Integer
Dim Up(12), Down(12) As Integer
Dim SumVol(12), sum As Single

' - Variables used to calculate the power output from
engines 1 & 3
Dim PosArea, NegArea, AvePower1 As Single
Dim PosArea3, NegArea3, AvePower3 As Single

```

```

Dim PosCurve(1 To 2, 0 To 10000), NegCurve(1 To 2, 0 To 10000), Power(1
To 1000)
Dim PosCurve3(1 To 2, 0 To 10000), NegCurve3(1 To 2, 0 To 10000),
Power3(1 To 1000)
Dim Initial_t1, Initial_t3 As Single
Dim i, ii As Integer

'   neg, sup   -   counters used to check if blowout or negative height
has occurred
Dim neg, sup As Integer

'   PrintRow   -   counter used for printing the output file
Dim PrintRow, PrintRow2 As Integer

'   PrintBuffer -   the number of seconds raw data prints out after
convergence
Dim PrintBuffer As Single

'   View       -   string of the sreen viewed while the program is running
Dim View As String

'   Answer     -   variable used in message boxes
Dim Answer

'               -   variables used to determine convergence
Dim Converged As Boolean
Dim Check1, Check2, Check3, Finished As Single
Dim CycleNumber, CycleNumber_Max As Integer

'               -   variables used to calculate engine period
Dim Hertz, t_initial As Single
Dim CycleNumber_o As Integer

'   Full      -   Shortest column is x% full
Dim Full As Single

'*****
'*****
'   Unloading Parameter Data from Passed Array
'*****
'*****

Lt1 = Parameters(1) 'Tuning Length 1
Lt2 = Parameters(2) 'Tuning Length 2
LH = Parameters(3) 'Hot Chamber Height
LC = Parameters(4) 'Cold Chamber Height
LA = Parameters(5) 'Ambient Chamber Height
LB = Parameters(6) 'Bounce Chamber Height

'*****
'   Reading Parameter Data from Spreadsheet "Initial Conditions"
'*****

Pi = 3.1415927

g = Worksheets("Parameter Values").Range("F8").Value
f = Worksheets("Parameter Values").Range("F9").Value
d = Worksheets("Parameter Values").Range("F7").Value
R = Worksheets("Parameter Values").Range("F11").Value
Dia = Worksheets("Parameter Values").Range("B8").Value
Dia_BC = Worksheets("Parameter Values").Range("B9").Value
Dt = Worksheets("Parameter Values").Range("B4").Value
TH = Worksheets("Parameter Values").Range("F19").Value

```

```

TA = Worksheets("Parameter Values").Range("F21").Value
TC = Worksheets("Parameter Values").Range("F20").Value
TB = Worksheets("Parameter Values").Range("F22").Value
Pmean = Worksheets("Parameter Values").Range("F11").Value
VB = Worksheets("Parameter Values").Range("F4").Value
Damp = Worksheets("Parameter Values").Range("F12").Value
Full = Worksheets("Parameter Values").Range("B16").Value

```

```

'*****
'   Cross-sectional Area Calculations
'*****

```

```

Area = Pi * Dia ^ 2 / 4
Area_BC = Pi * Dia_BC ^ 2 / 4

```

```

'*****
'   Initializing of liquid heights
'*****

```

```

If LH <= LA And LH <= LC And LH <= LB Then LL = LH * Full
If LA <= LH And LA <= LC And LA <= LB Then LL = LA * Full
If LC <= LA And LC <= LH And LC <= LB Then LL = LC * Full
If LB <= LA And LB <= LH And LB <= LC Then LL = LB * Full

```

```

    LA1 = LL
    LH1 = LL
    LB1 = LL + 0.2 ' Infinitesimal offset to start engine oscillation
    LA2 = LL
    LC2 = LL
    LB2 = LL
    LA3 = LL
    LH3 = LL
    LB3 = LL - 0.2 ' Infinitesimal offset to start engine oscillation
    LA4 = LL
    LC4 = LL
    LB4 = LL

```

```

'*****
'   Initializing of liquid velocities in each column
'*****

```

```

    vl12a = 0
    vl12b = 0
    vl12c = 0
    vl23a = 0
    vl23b = 0
    vl23c = 0
    vl34a = 0
    vl34b = 0
    vl34c = 0
    vl41a = 0
    vl41b = 0
    vl41c = 0

```

```

'*****
'   Initializing of gas volumes in each column
'*****

```

```

    VoA1 = Area * (LA - LA1)
    VoH1 = Area * (LH - LH1)
    VoB1 = Area_BC * (LB - LB1)
    VoA2 = Area * (LA - LA2)
    VoC2 = Area * (LC - LC2)

```



```

VoB2 = Area_BC * (LB - LB2)
VoA3 = Area * (LA - LA3)
VoH3 = Area * (LH - LH3)
VoB3 = Area_BC * (LB - LB3)
VoA4 = Area * (LA - LA4)
VoC4 = Area * (LC - LC4)
VoB4 = Area_BC * (LB - LB4)

'*****
'   Initializing of gas pressures in each column
'*****

PA = Pmean
PB = Pmean
PC = Pmean
PD = Pmean
PB1 = Pmean
PB2 = Pmean
PB3 = Pmean
PB4 = Pmean

'*****
'   INITIALIZATION OF TIME AND OTHER COUNTERS
'*****

For j = 1 To 12
    MeanVol.Counter(j) = 1
Next j

For j = 0 To 20
    MeanVol.A1(j) = Area * (LA - LL)
    MeanVol.A2(j) = Area * (LA - LL)
    MeanVol.A3(j) = Area * (LA - LL)
    MeanVol.A4(j) = Area * (LA - LL)
    MeanVol.H1(j) = Area * (LH - LL)
    MeanVol.C2(j) = Area * (LC - LL)
    MeanVol.H3(j) = Area * (LH - LL)
    MeanVol.C4(j) = Area * (LC - LL)
    MeanVol.B1(j) = Area_BC * (LB - LL)
    MeanVol.B2(j) = Area_BC * (LB - LL)
    MeanVol.B3(j) = Area_BC * (LB - LL)
    MeanVol.B4(j) = Area_BC * (LB - LL)
Next j

t = 0
m = 0
n = 0
p = 1
u = 0
v = 0
w = 1
Tick1 = 0
Tick3 = 0
TickPV = 0
Number_of_cycles = Worksheets("Parameter Values").Range("F25").Value
PrintBuffer = Worksheets("Parameter Values").Range("F28").Value
PrintRow = 3
PrintRow2 = 2
Converged = False
Finished = 1000
Engine = 0
CycleNumber = 0
CycleNumber_o = 0
CycleNumber_Max = Worksheets("Parameter Values").Range("F29").Value

```

```

'*****
'   SELECT DEFAULT SHEET VIEWED WHILE RUNNING PROGRAM
'*****

Sheets("Interface").Select
'Sheets("Virtual Pistons").Select
'Sheets("Power Data").Select
'Sheets("Raw Data").Select

'*****
'   BEGINNING OF MAIN LOOP
'*****

Do Until t >= (Finished + PrintBuffer)

    TimeInterval = Worksheets("Parameter Values").Range("B5").Value
    View = Worksheets("Parameter Values").Range("A25").Value
'*****
'   INITIALIZATION OF GAS VOLUMES
'*****

    VoH1o = VoH1
    VoA1o = VoA1
    VoC2o = VoC2
    VoH3o = VoH3
    VoA3o = VoA3
    VoC4o = VoC4
    VoA2o = VoA2
    VoA4o = VoA4
    VoB1o = VoB1
    VoB2o = VoB2
    VoB3o = VoB3
    VoB4o = VoB4

'*****
'   INITIALIZATION OF GAS PRESSURES
'*****

    PAo = PA
    PBo = PB
    PCo = PC
    PDo = PD
    PB1o = PB1
    PB2o = PB2
    PB3o = PB3
    PB4o = PB4

'*****
'   CALCULATION OF GAS VOLUMES
'*****

    VoA1 = Area * (LA - LA1)
    VoH1 = Area * (LH - LH1)
    VoB1 = Area_BC * (LB - LB1)
    VoA2 = Area * (LA - LA2)
    VoC2 = Area * (LC - LC2)
    VoB2 = Area_BC * (LB - LB2)
    VoA3 = Area * (LA - LA3)
    VoH3 = Area * (LH - LH3)
    VoB3 = Area_BC * (LB - LB3)
    VoA4 = Area * (LA - LA4)
    VoC4 = Area * (LC - LC4)
    VoB4 = Area_BC * (LB - LB4)

```

```

'*****
'  CALCULATION OF GAS PRESSURES VIA THE IDEAL GAS LAW
'*****

```

```

PP1 = Pmean * (MeanVol.H1(0) / TH + 2 * VB / (TH + TA) +
MeanVol.A1(0) / TA)
PP3 = Pmean * (MeanVol.H3(0) / TH + 2 * VB / (TH + TA) +
MeanVol.A3(0) / TA)
PA = PP1 / (VoH1 / TH + 2 * VB / (TH + TA) + VoA1 / TA)
PC = PP3 / (VoH3 / TH + 2 * VB / (TH + TA) + VoA3 / TA)
PP2 = Pmean * (MeanVol.A2(0) / TA + 2 * VB / (TA + TC) +
MeanVol.C2(0) / TC)
PP4 = Pmean * (MeanVol.A4(0) / TA + 2 * VB / (TA + TC) +
MeanVol.C4(0) / TC)
PB = PP2 / (VoA2 / TA + 2 * VB / (TA + TC) + VoC2 / TC)
PD = PP4 / (VoA4 / TA + 2 * VB / (TA + TC) + VoC4 / TC)
PB1 = Pmean * MeanVol.B1(0) / VoB1
PB2 = Pmean * MeanVol.B2(0) / VoB2
PB3 = Pmean * MeanVol.B3(0) / VoB3
PB4 = Pmean * MeanVol.B4(0) / VoB4

```

```

'*****
'  CALCULATION OF LIQUID PRESSURES
'*****

```

```

' P2A
i_1 = Sgn(vl12a)
i_3 = Sgn(vl12b)
i_5 = Sgn(vl12c)

X11 = PB1 + d * g * LB1 * (2 * (Dia / Dia_BC) * (Dia / Dia_BC) + 1)
X12 = (PA - PA * Lt1 / (LH1 + Lt1)) * (LB1 / LH1) * (Dia / Dia_BC) *
(Dia / Dia_BC)
X13 = (PB - PB * Lt2 / (LA2 + Lt2)) * (LB1 / LA2) * (Dia / Dia_BC) *
(Dia / Dia_BC)
X14 = (d * g * LB1 * Lt1 / (LH1 + Lt1) + d * g * LB1 * Lt2 / (LA2 +
Lt2)) * (Dia / Dia_BC) * (Dia / Dia_BC)
X15 = 1 + LB1 / (LH1 + Lt1) * (Dia / Dia_BC) * (Dia / Dia_BC) + LB1
/ (LA2 + Lt2) * (Dia / Dia_BC) * (Dia / Dia_BC)
X21 = 2 * f * d * LB1 * (-i_3 * vl12b ^ 2 / Dia_BC - i_5 * Dia *
vl12c ^ 2 / (Dia_BC ^ 2) + i_1 * Dia * vl12a ^ 2 / (Dia_BC ^ 2))
P2A = (X11 + X12 + X13 - X14 + X21) / X15

```

```

' P2B
i_1 = Sgn(vl23a)
i_3 = Sgn(vl23b)
i_5 = Sgn(vl23c)

X16 = PB2 + d * g * LB2 * (2 * (Dia / Dia_BC) * (Dia / Dia_BC) + 1)
X17 = (PB - PB * Lt1 / (LC2 + Lt1)) * (LB2 / LC2) * (Dia / Dia_BC) *
(Dia / Dia_BC)
X18 = (PC - PC * Lt2 / (LA3 + Lt2)) * (LB2 / LA3) * (Dia / Dia_BC) *
(Dia / Dia_BC)
X19 = (d * g * LB2 * Lt1 / (LC2 + Lt1) + d * g * LB2 * Lt2 / (LA3 +
Lt2)) * (Dia / Dia_BC) * (Dia / Dia_BC)
X110 = 1 + LB2 / (LC2 + Lt1) * (Dia / Dia_BC) * (Dia / Dia_BC) + LB2
/ (LA3 + Lt2) * (Dia / Dia_BC) * (Dia / Dia_BC)
X22 = 2 * f * d * LB2 * (-i_3 * vl23b ^ 2 / Dia_BC - i_5 * Dia *
vl23c ^ 2 / (Dia_BC ^ 2) + i_1 * Dia * vl23a ^ 2 / (Dia_BC ^ 2))
P2B = (X16 + X17 + X18 - X19 + X22) / X110

```

```

' P2C
i_1 = Sgn(vl34a)
i_3 = Sgn(vl34b)
i_5 = Sgn(vl34c)

```

```

X111 = PB3 + d * g * LB3 * (2 * (Dia / Dia_BC) * (Dia / Dia_BC) + 1)
X112 = (PC - PC * Lt1 / (LH3 + Lt1)) * (LB3 / LH3) * (Dia / Dia_BC)
* (Dia / Dia_BC)
X113 = (PD - PD * Lt2 / (LA4 + Lt2)) * (LB3 / LA4) * (Dia / Dia_BC)
* (Dia / Dia_BC)
X114 = (d * g * LB3 * Lt1 / (LH3 + Lt1) + d * g * LB3 * Lt2 / (LA4 +
Lt2)) * (Dia / Dia_BC) * (Dia / Dia_BC)
X115 = 1 + LB3 / (LH3 + Lt1) * (Dia / Dia_BC) * (Dia / Dia_BC) + LB3
/ (LA4 + Lt2) * (Dia / Dia_BC) * (Dia / Dia_BC)
X23 = 2 * f * d * LB3 * (-i_3 * vl34b ^ 2 / Dia_BC - i_5 * Dia *
vl34c ^ 2 / (Dia_BC ^ 2) + i_1 * Dia * vl34a ^ 2 / (Dia_BC ^ 2))
P2C = (X111 + X112 + X113 - X114 + X23) / X115
' P2D
i_1 = Sgn(vl41a)
i_3 = Sgn(vl41b)
i_5 = Sgn(vl41c)

X116 = PB4 + d * g * LB4 * (2 * (Dia / Dia_BC) * (Dia / Dia_BC) + 1)
X117 = (PD - PD * Lt1 / (LC4 + Lt1)) * (LB4 / LC4) * (Dia / Dia_BC)
* (Dia / Dia_BC)
X118 = (PA - PA * Lt2 / (LA1 + Lt2)) * (LB4 / LA1) * (Dia / Dia_BC)
* (Dia / Dia_BC)
X119 = (d * g * LB4 * Lt1 / (LC4 + Lt1) + d * g * LB4 * Lt2 / (LA1 +
Lt2)) * (Dia / Dia_BC) * (Dia / Dia_BC)
X120 = 1 + LB4 / (LC4 + Lt1) * (Dia / Dia_BC) * (Dia / Dia_BC) + LB4
/ (LA1 + Lt2) * (Dia / Dia_BC) * (Dia / Dia_BC)
X24 = 2 * f * d * LB4 * (-i_3 * vl41b ^ 2 / Dia_BC - i_5 * Dia *
vl41c ^ 2 / (Dia_BC ^ 2) + i_1 * Dia * vl41a ^ 2 / (Dia_BC ^ 2))
P2D = (X116 + X117 + X118 - X119 + X24) / X120

P1A = (PA * Lt1 + g * d * LH1 * Lt1 + P2A * LH1) / (LH1 + Lt1)
P1B = (PB * Lt1 + g * d * LC2 * Lt1 + P2B * LC2) / (LC2 + Lt1)
P1C = (PC * Lt1 + g * d * LH3 * Lt1 + P2C * LH3) / (LH3 + Lt1)
P1D = (PD * Lt1 + g * d * LC4 * Lt1 + P2D * LC4) / (LC4 + Lt1)

' P3A = (g * d * Lt2 * LA2 + PB * Lt2 + P2A * LA2) / (Lt2 + LA2)
' P3B = (g * d * Lt2 * LA3 + PC * Lt2 + P2B * LA3) / (Lt2 + LA3)
' P3C = (g * d * Lt2 * LA4 + PD * Lt2 + P2C * LA4) / (Lt2 + LA4)
' P3D = (g * d * Lt2 * LA1 + PA * Lt2 + P2D * LA1) / (Lt2 + LA1)

```

```

'*****
' CALCULATION OF LIQUID ACCELERATIONS
'*****

```

```

If (vl12a <= 0) Then a12a = (PA - P1A) / (d * LH1) + g + 2 * f *
vl12a * vl12a / Dia
If (vl12a > 0) Then a12a = (PA - P1A) / (d * LH1) + g - 2 * f *
vl12a * vl12a / Dia
If (vl23a <= 0) Then a23a = (PB - P1B) / (d * LC2) + g + 2 * f *
vl23a * vl23a / Dia
If (vl23a > 0) Then a23a = (PB - P1B) / (d * LC2) + g - 2 * f *
vl23a * vl23a / Dia
If (vl34a <= 0) Then a34a = (PC - P1C) / (d * LH3) + g + 2 * f *
vl34a * vl34a / Dia
If (vl34a > 0) Then a34a = (PC - P1C) / (d * LH3) + g - 2 * f *
vl34a * vl34a / Dia
If (vl41a <= 0) Then a41a = (PD - P1D) / (d * LC4) + g + 2 * f *
vl41a * vl41a / Dia
If (vl41a > 0) Then a41a = (PD - P1D) / (d * LC4) + g - 2 * f *
vl41a * vl41a / Dia
If (vl12b <= 0) Then a12b = (P2A - PB1) / (d * LB1) - g + 2 * f *
vl12b * vl12b / Dia_BC

```

```

      If (vl12b > 0) Then a12b = (P2A - PB1) / (d * LB1) - g - 2 * f *
vl12b * vl12b / Dia_BC
      If (vl23b <= 0) Then a23b = (P2B - PB2) / (d * LB2) - g + 2 * f *
vl23b * vl23b / Dia_BC
      If (vl23b > 0) Then a23b = (P2B - PB2) / (d * LB2) - g - 2 * f *
vl23b * vl23b / Dia_BC
      If (vl34b <= 0) Then a34b = (P2C - PB3) / (d * LB3) - g + 2 * f *
vl34b * vl34b / Dia_BC
      If (vl34b > 0) Then a34b = (P2C - PB3) / (d * LB3) - g - 2 * f *
vl34b * vl34b / Dia_BC
      If (vl41b <= 0) Then a41b = (P2D - PB4) / (d * LB4) - g + 2 * f *
vl41b * vl41b / Dia_BC
      If (vl41b > 0) Then a41b = (P2D - PB4) / (d * LB4) - g - 2 * f *
vl41b * vl41b / Dia_BC

```

```

a12c = a12a - (Dia_BC / Dia) * (Dia_BC / Dia) * a12b
a23c = a23a - (Dia_BC / Dia) * (Dia_BC / Dia) * a23b
a34c = a34a - (Dia_BC / Dia) * (Dia_BC / Dia) * a34b
a41c = a41a - (Dia_BC / Dia) * (Dia_BC / Dia) * a41b

```

```
t = t + Dt
```

```

'*****
'  CALCULATION OF VELOCITY BUFFER
'*****

```

```

vl12ao = vl12a
vl12bo = vl12b
vl12co = vl12c
vl23ao = vl23a
vl23bo = vl23b
vl23co = vl23c
vl34ao = vl34a
vl34bo = vl34b
vl34co = vl34c
vl41ao = vl41a
vl41bo = vl41b
vl41co = vl41c

```

```

'*****
'  CALCULATION OF LIQUID VELOCITIES
'*****

```

```

vl12a = vl12ao + a12a * Dt
vl12b = vl12bo + a12b * Dt
vl12c = vl12co + a12c * Dt
vl23a = vl23ao + a23a * Dt
vl23b = vl23bo + a23b * Dt
vl23c = vl23co + a23c * Dt
vl34a = vl34ao + a34a * Dt
vl34b = vl34bo + a34b * Dt
vl34c = vl34co + a34c * Dt
vl41a = vl41ao + a41a * Dt
vl41b = vl41bo + a41b * Dt
vl41c = vl41co + a41c * Dt

```

```

'*****
'  CALCULATION OF LIQUID POSITIONS IN EACH COLUMN
'*****

```

```

LH1 = LH1 - vl12ao * Dt - 0.5 * a12a * Dt * Dt
LB1 = LB1 + vl12bo * Dt + 0.5 * a12b * Dt * Dt
LA2 = LA2 + vl12co * Dt + 0.5 * a12c * Dt * Dt
LC2 = LC2 - vl23ao * Dt - 0.5 * a23a * Dt * Dt

```

```

LB2 = LB2 + v123bo * Dt + 0.5 * a23b * Dt * Dt
LA3 = LA3 + v123co * Dt + 0.5 * a23c * Dt * Dt
LH3 = LH3 - v134ao * Dt - 0.5 * a34a * Dt * Dt
LB3 = LB3 + v134bo * Dt + 0.5 * a34b * Dt * Dt
LA4 = LA4 + v134co * Dt + 0.5 * a34c * Dt * Dt
LC4 = LC4 - v141ao * Dt - 0.5 * a41a * Dt * Dt
LB4 = LB4 + v141bo * Dt + 0.5 * a41b * Dt * Dt
LA1 = LA1 + v141co * Dt + 0.5 * a41c * Dt * Dt

'*****
'  CALCULATION OF MEAN GAS VOLUME IN EACH CHAMBER
'*****

'*****          Ambient Chamber 1          *****

Chamber = 1

  If VoA1 > VoA1o Then          '  Down Stroke
    If (Up(Chamber) > 0) Then  '  One cycle complete
      MeanVol.A1(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
      (Up(Chamber) + Down(Chamber))
      sum = 0
      For j = 1 To 20
        sum = MeanVol.A1(j) / 20 + sum
      Next
      MeanVol.A1(0) = (sum - MeanVol.A1(0)) * Damp + sum
      MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
      If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0
      End If
      Down(Chamber) = Down(Chamber) + 1
      SumVol(Chamber) = SumVol(Chamber) + VoA1
    Else          '  Up Stroke
      SumVol(Chamber) = SumVol(Chamber) + VoA1
      Up(Chamber) = Up(Chamber) + 1
    End If

'*****          Hot Chamber 1          *****

Chamber = 2

  If VoH1 > VoH1o Then          '  Down Stroke
    If (Up(Chamber) > 0) Then  '  One cycle complete

      '  Calculate frequency of engine
      If CycleNumber = CycleNumber_o + 9 Then
        Hertz = 1 / ((t - t_initial) / 10)
        CycleNumber_o = CycleNumber
        t_initial = t
        Worksheets("Power Data").Range("C7").Value = Hertz
        Worksheets("Parameter Values").Range("B28").Value =
Hertz

      End If
      CycleNumber = CycleNumber + 1
      Worksheets("Convergence").Range("K3").Value = CycleNumber
      Worksheets("Power Data").Range("C9").Value = CycleNumber
      Worksheets("Parameter Values").Range("B29").Value =
CycleNumber

      MeanVol.H1(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
      (Up(Chamber) + Down(Chamber))

```

```

sum = 0
For j = 1 To 20
sum = MeanVol.H1(j) / 20 + sum
Next
MeanVol.H1(0) = (sum - MeanVol.H1(0)) * Damp + sum
MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
Up(Chamber) = 0
Down(Chamber) = 0
SumVol(Chamber) = 0
End If
Down(Chamber) = Down(Chamber) + 1
SumVol(Chamber) = SumVol(Chamber) + VoH1
Else
' Up Stroke
SumVol(Chamber) = SumVol(Chamber) + VoH1
Up(Chamber) = Up(Chamber) + 1
End If

```

\*\*\*\*\* Bounce Chamber 1 \*\*\*\*\*

Chamber = 3

```

If VoB1 > VoB1o Then
' Down Stroke
If (Up(Chamber) > 0) Then ' One cycle complete
MeanVol.B1(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
sum = 0
For j = 1 To 20
sum = MeanVol.B1(j) / 20 + sum
Next
MeanVol.B1(0) = (sum - MeanVol.B1(0)) * Damp + sum
MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
Up(Chamber) = 0
Down(Chamber) = 0
SumVol(Chamber) = 0
End If
Down(Chamber) = Down(Chamber) + 1
SumVol(Chamber) = SumVol(Chamber) + VoB1
Else
' Up Stroke
SumVol(Chamber) = SumVol(Chamber) + VoB1
Up(Chamber) = Up(Chamber) + 1
End If

```

\*\*\*\*\* Ambient Chamber 2 \*\*\*\*\*

Chamber = 4

```

If VoA2 > VoA2o Then
' Down Stroke
If (Up(Chamber) > 0) Then ' One cycle complete
MeanVol.A2(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
sum = 0
For j = 1 To 20
sum = MeanVol.A2(j) / 20 + sum
Next
MeanVol.A2(0) = (sum - MeanVol.A2(0)) * Damp + sum
MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
Up(Chamber) = 0
Down(Chamber) = 0

```

```

        SumVol(Chamber) = 0
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoA2
Else
    ' Up Stroke
    SumVol(Chamber) = SumVol(Chamber) + VoA2
    Up(Chamber) = Up(Chamber) + 1
End If

'***** Cold Chamber 2 *****

Chamber = 5

    If VoC2 > VoC2o Then
        ' Down Stroke
        If (Up(Chamber) > 0) Then ' One cycle complete
            MeanVol.C2(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
            (Up(Chamber) + Down(Chamber))
            sum = 0
            For j = 1 To 20
                sum = MeanVol.C2(j) / 20 + sum
            Next
            MeanVol.C2(0) = (sum - MeanVol.C2(0)) * Damp + sum
            MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
            If MeanVol.Counter(Chamber) = 21 Then
                MeanVol.Counter(Chamber) = 1
                Up(Chamber) = 0
                Down(Chamber) = 0
                SumVol(Chamber) = 0
            End If
            Down(Chamber) = Down(Chamber) + 1
            SumVol(Chamber) = SumVol(Chamber) + VoC2
        Else
            ' Up Stroke
            SumVol(Chamber) = SumVol(Chamber) + VoC2
            Up(Chamber) = Up(Chamber) + 1
        End If

'***** Bounce Chamber 2 *****

Chamber = 6

    If VoB2 > VoB2o Then
        ' Down Stroke
        If (Up(Chamber) > 0) Then ' One cycle complete
            MeanVol.B2(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
            (Up(Chamber) + Down(Chamber))
            sum = 0
            For j = 1 To 20
                sum = MeanVol.B2(j) / 20 + sum
            Next
            MeanVol.B2(0) = (sum - MeanVol.B2(0)) * Damp + sum
            MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
            If MeanVol.Counter(Chamber) = 21 Then
                MeanVol.Counter(Chamber) = 1
                Up(Chamber) = 0
                Down(Chamber) = 0
                SumVol(Chamber) = 0
            End If
            Down(Chamber) = Down(Chamber) + 1
            SumVol(Chamber) = SumVol(Chamber) + VoB2
        Else
            ' Up Stroke
            SumVol(Chamber) = SumVol(Chamber) + VoB2
            Up(Chamber) = Up(Chamber) + 1
        End If

'***** Ambient Chamber 3 *****

```



Chamber = 7

```
      If VoA3 > VoA3o Then          '      Down Stroke
        If (Up(Chamber) > 0) Then ' One cycle complete
          MeanVol.A3(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
          sum = 0
          For j = 1 To 20
            sum = MeanVol.A3(j) / 20 + sum
          Next
          MeanVol.A3(0) = (sum - MeanVol.A3(0)) * Damp + sum
          MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
          If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
          Up(Chamber) = 0
          Down(Chamber) = 0
          SumVol(Chamber) = 0
          End If
          Down(Chamber) = Down(Chamber) + 1
          SumVol(Chamber) = SumVol(Chamber) + VoA3
        Else                          '      Up Stroke
          SumVol(Chamber) = SumVol(Chamber) + VoA3
          Up(Chamber) = Up(Chamber) + 1
        End If
```

'\*\*\*\*\* Hot Chamber 3 \*\*\*\*\*

Chamber = 8

```
      If VoH3 > VoH3o Then          '      Down Stroke
        If (Up(Chamber) > 0) Then ' One cycle complete
          MeanVol.H3(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
          sum = 0
          For j = 1 To 20
            sum = MeanVol.H3(j) / 20 + sum
          Next
          MeanVol.H3(0) = (sum - MeanVol.H3(0)) * Damp + sum
          MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
          If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
          Up(Chamber) = 0
          Down(Chamber) = 0
          SumVol(Chamber) = 0
          End If
          Down(Chamber) = Down(Chamber) + 1
          SumVol(Chamber) = SumVol(Chamber) + VoH3
        Else                          '      Up Stroke
          SumVol(Chamber) = SumVol(Chamber) + VoH3
          Up(Chamber) = Up(Chamber) + 1
        End If
```

'\*\*\*\*\* Bounce Chamber 3 \*\*\*\*\*

Chamber = 9

```
      If VoB3 > VoB3o Then          '      Down Stroke
        If (Up(Chamber) > 0) Then ' One cycle complete
          MeanVol.B3(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
          sum = 0
          For j = 1 To 20
            sum = MeanVol.B3(j) / 20 + sum
```

```

Next
MeanVol.B3(0) = (sum - MeanVol.B3(0)) * Damp + sum
MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
Up(Chamber) = 0
Down(Chamber) = 0
SumVol(Chamber) = 0
End If
Down(Chamber) = Down(Chamber) + 1
SumVol(Chamber) = SumVol(Chamber) + VoB3
Else
' Up Stroke
SumVol(Chamber) = SumVol(Chamber) + VoB3
Up(Chamber) = Up(Chamber) + 1
End If

```

\*\*\*\*\* Ambient Chamber 4 \*\*\*\*\*

Chamber = 10

```

If VoA4 > VoA4o Then ' Down Stroke
If (Up(Chamber) > 0) Then ' One cycle complete
MeanVol.A4(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
sum = 0
For j = 1 To 20
sum = MeanVol.A4(j) / 20 + sum
Next
MeanVol.A4(0) = (sum - MeanVol.A4(0)) * Damp + sum
MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
Up(Chamber) = 0
Down(Chamber) = 0
SumVol(Chamber) = 0
End If
Down(Chamber) = Down(Chamber) + 1
SumVol(Chamber) = SumVol(Chamber) + VoA4
Else
' Up Stroke
SumVol(Chamber) = SumVol(Chamber) + VoA4
Up(Chamber) = Up(Chamber) + 1
End If

```

\*\*\*\*\* Cold Chamber 4 \*\*\*\*\*

Chamber = 11

```

If VoC4 > VoC4o Then ' Down Stroke
If (Up(Chamber) > 0) Then ' One cycle complete
MeanVol.C4(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
(Up(Chamber) + Down(Chamber))
sum = 0
For j = 1 To 20
sum = MeanVol.C4(j) / 20 + sum
Next
MeanVol.C4(0) = (sum - MeanVol.C4(0)) * Damp + sum
MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
Up(Chamber) = 0
Down(Chamber) = 0
SumVol(Chamber) = 0
End If
Down(Chamber) = Down(Chamber) + 1

```

```

    SumVol(Chamber) = SumVol(Chamber) + VoC4
Else
    SumVol(Chamber) = SumVol(Chamber) + VoC4
    Up(Chamber) = Up(Chamber) + 1
End If

'***** Bounce Chamber 4 *****

Chamber = 12

    If VoB4 > VoB4o Then
        ' Down Stroke
        If (Up(Chamber) > 0) Then ' One cycle complete
            MeanVol.B4(MeanVol.Counter(Chamber)) = SumVol(Chamber) /
            (Up(Chamber) + Down(Chamber))
            sum = 0
            For j = 1 To 20
                sum = MeanVol.B4(j) / 20 + sum
            Next
            MeanVol.B4(0) = (sum - MeanVol.B4(0)) * Damp + sum
            MeanVol.Counter(Chamber) = MeanVol.Counter(Chamber) + 1
            If MeanVol.Counter(Chamber) = 21 Then
MeanVol.Counter(Chamber) = 1
                Up(Chamber) = 0
                Down(Chamber) = 0
                SumVol(Chamber) = 0
            End If
            Down(Chamber) = Down(Chamber) + 1
            SumVol(Chamber) = SumVol(Chamber) + VoB4
        Else
            ' Up Stroke
            SumVol(Chamber) = SumVol(Chamber) + VoB4
            Up(Chamber) = Up(Chamber) + 1
        End If
'*****

'*****
' CALCULATION OF POWER PER CYCLE
'*****

    If ((VoH1 + VoA1) > (VoH1o + VoA1o)) Then
        ' Positive Curve
        If (n > 0) Then
            PosArea = PV_Area(PosCurve, m)
            NegArea = PV_Area(NegCurve, n)
            Power(p) = (NegArea - PosArea) / (t - Initial_t1) _
                / 10000000#
            Initial_t1 = t
            m = 0
            n = 0
            p = p + 1
            If p = Number_of_cycles + 1 Then
                AvePower1 = 0
                For ii = 1 To Number_of_cycles
                    AvePower1 = Power(ii) / Number_of_cycles + AvePower1
                Next ii
                'POWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWER
                DialogSheets("Virtual Pistons").EditBoxes("Edit Box 53")

                .Text = AvePower1
                Worksheets("Power Data").Cells(6, 8).Value = AvePower1
                Worksheets("Power Data").Cells(Tick1 + 7, 8).Value = AvePower1
            AvePower1

            Worksheets("Power Data").Cells(Tick1 + 7, 7).Value = t
            Tick1 = Tick1 + 1
            'POWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWER
            p = 1
        End If
    End If

```

```

        End If
    End If
    PosCurve(1, m) = PA
    PosCurve(2, m) = VoH1 + VoA1
    m = m + 1
End If
If ((VoH1 + VoA1) < (VoH1o + VoA1o)) Then      ' Negative Curve
    NegCurve(1, n) = PA
    NegCurve(2, n) = VoH1o + VoA1o
    n = n + 1
End If

' Engine 3 Power

If ((VoH3 + VoA3) > (VoH3o + VoA3o)) Then      ' Positvie
Curve
    If (u > 0) Then
        PosArea3 = PV_Area(PosCurve3, v)
        NegArea3 = PV_Area(NegCurve3, u)
        Power3(w) = (NegArea3 - PosArea3) / (t - Initial_t3) _
            / 100000000#
        Initial_t3 = t
        v = 0
        u = 0
        w = w + 1
        If w = Number_of_cycles + 1 Then
            AvePower3 = 0
            For ii = 1 To Number_of_cycles
                AvePower3 = Power3(ii) / Number_of_cycles +
AvePower3
            Next ii
            'POWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWER
            DialogSheets("Virtual Pistons").EditBoxes("Edit Box 54")
            .Text = AvePower3
            Worksheets("Power Data").Cells(6, 10).Value = AvePower3
            Worksheets("Power Data").Cells(Tick3 + 7, 10).Value =
AvePower3
            Worksheets("Power Data").Cells(Tick3 + 7, 9).Value = t
            Tick3 = Tick3 + 1
            'POWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWERPOWER
            w = 1
        End If
    End If
    PosCurve3(1, v) = PC
    PosCurve3(2, v) = VoH3 + VoA3
    v = v + 1
End If
If ((VoH3 + VoA3) < (VoH3o + VoA3o)) Then      ' Negative
Curve
    NegCurve3(1, u) = PC
    NegCurve3(2, u) = VoH3o + VoA3o
    u = u + 1
End If

'*****
' NEGATIVE HEIGHT CHECK
'*****

If (LH1 < 0) Then neg = neg + 1
If (LB1 < 0) Then neg = neg + 1
If (LA2 < 0) Then neg = neg + 1
If (LC2 < 0) Then neg = neg + 1

```

```

If (LB2 < 0) Then neg = neg + 1
If (LA3 < 0) Then neg = neg + 1
If (LH3 < 0) Then neg = neg + 1
If (LB3 < 0) Then neg = neg + 1
If (LA4 < 0) Then neg = neg + 1
If (LC4 < 0) Then neg = neg + 1
If (LB4 < 0) Then neg = neg + 1
If (LA1 < 0) Then neg = neg + 1
If (neg >= 1) Then
    Engine = -1
    Exit Do
End If

'*****
' BLOWOUT CHECK
'*****

If (LH1 > LH) Then sup = sup + 1
If (LB1 > LB) Then sup = sup + 1
If (LA2 > LA) Then sup = sup + 1
If (LC2 > LC) Then sup = sup + 1
If (LB2 > LB) Then sup = sup + 1
If (LA3 > LA) Then sup = sup + 1
If (LH3 > LH) Then sup = sup + 1
If (LB3 > LB) Then sup = sup + 1
If (LA4 > LA) Then sup = sup + 1
If (LC4 > LC) Then sup = sup + 1
If (LB4 > LB) Then sup = sup + 1
If (LA1 > LA) Then sup = sup + 1
If (sup >= 1) Then
    Engine = 1
    Exit Do
End If

'*****
' UPDATE CURRENT VIEW
'*****

If (t * 1000 Mod TimeInterval = 0) Then

    If View = "Power Data" Or View = "Virtual Pistons" Or View =
"Virtual Pistons II" Then
        Worksheets("Power Data").Cells(3, 1).Value = LA1
        Worksheets("Power Data").Cells(3, 2).Value = LH1
        Worksheets("Power Data").Cells(3, 3).Value = LB1
        Worksheets("Power Data").Cells(3, 4).Value = LA2
        Worksheets("Power Data").Cells(3, 5).Value = LC2
        Worksheets("Power Data").Cells(3, 6).Value = LB2
        Worksheets("Power Data").Cells(3, 7).Value = LA3
        Worksheets("Power Data").Cells(3, 8).Value = LH3
        Worksheets("Power Data").Cells(3, 9).Value = LB3
        Worksheets("Power Data").Cells(3, 10).Value = LA4
        Worksheets("Power Data").Cells(3, 11).Value = LC4
        Worksheets("Power Data").Cells(3, 12).Value = LB4
        Worksheets("Power Data").Cells(5, 3).Value = t
        Worksheets("Power Data").Cells(TickPV + 8, 1).Value = PA
        Worksheets("Power Data").Cells(TickPV + 8, 2).Value = VoH1 + VoA1
        TickPV = TickPV + 1
        If TickPV > 30 Then TickPV = 0
    End If

    If View = "Virtual Pistons" Then
        DialogSheets("Virtual Pistons").EditBoxes("Edit Box 19").Text = t
    End If

```

End If

```
' *****  
' PRINT OUT RESULTS  
' *****
```

i = 50

If Converged And (t \* 1000 Mod i = 0) Then

```
PrintRow = PrintRow + 1  
Worksheets("Raw Data").Cells(PrintRow, 1).Value = t  
Worksheets("Raw Data").Cells(PrintRow, 2).Value = LA1  
Worksheets("Raw Data").Cells(PrintRow, 3).Value = LH1  
Worksheets("Raw Data").Cells(PrintRow, 4).Value = LB1  
Worksheets("Raw Data").Cells(PrintRow, 5).Value = LA2  
Worksheets("Raw Data").Cells(PrintRow, 6).Value = LC2  
Worksheets("Raw Data").Cells(PrintRow, 7).Value = LB2  
Worksheets("Raw Data").Cells(PrintRow, 8).Value = LA3  
Worksheets("Raw Data").Cells(PrintRow, 9).Value = LH3  
Worksheets("Raw Data").Cells(PrintRow, 10).Value = LB3  
Worksheets("Raw Data").Cells(PrintRow, 11).Value = LA4  
Worksheets("Raw Data").Cells(PrintRow, 12).Value = LC4  
Worksheets("Raw Data").Cells(PrintRow, 13).Value = LB4  
Worksheets("Raw Data").Cells(PrintRow, 14).Value = MeanVol.A1(0)  
Worksheets("Raw Data").Cells(PrintRow, 15).Value = MeanVol.H1(0)  
Worksheets("Raw Data").Cells(PrintRow, 16).Value = MeanVol.B1(0)  
Worksheets("Raw Data").Cells(PrintRow, 17).Value = MeanVol.A2(0)  
Worksheets("Raw Data").Cells(PrintRow, 18).Value = MeanVol.C2(0)  
Worksheets("Raw Data").Cells(PrintRow, 19).Value = MeanVol.B2(0)  
Worksheets("Raw Data").Cells(PrintRow, 20).Value = MeanVol.A3(0)  
Worksheets("Raw Data").Cells(PrintRow, 21).Value = MeanVol.H3(0)  
Worksheets("Raw Data").Cells(PrintRow, 22).Value = MeanVol.B3(0)  
Worksheets("Raw Data").Cells(PrintRow, 23).Value = MeanVol.A4(0)  
Worksheets("Raw Data").Cells(PrintRow, 24).Value = MeanVol.C4(0)  
Worksheets("Raw Data").Cells(PrintRow, 25).Value = MeanVol.B4(0)  
  
Worksheets("Raw Data").Cells(PrintRow, 26).Value = PA  
Worksheets("Raw Data").Cells(PrintRow, 27).Value = VoA1 + VoH1  
Worksheets("Raw Data").Cells(PrintRow, 28).Value = PB  
Worksheets("Raw Data").Cells(PrintRow, 29).Value = VoA2 + VoC2  
Worksheets("Raw Data").Cells(PrintRow, 30).Value = PA  
Worksheets("Raw Data").Cells(PrintRow, 31).Value = VoA3 + VoH3  
Worksheets("Raw Data").Cells(PrintRow, 32).Value = PB  
Worksheets("Raw Data").Cells(PrintRow, 33).Value = VoA4 + VoC4  
  
Worksheets("Raw Data").Cells(PrintRow, 34).Value = Power(p)  
Worksheets("Raw Data").Cells(PrintRow, 35).Value = Power3(w)
```

End If

```
' *****  
' CONVERGENCE CHECK  
' *****
```

i = 100

```

'
'
'   If (t * 1000 Mod i = 0) And Converged = False Then
'   PrintRow2 = PrintRow2 + 1
'   Worksheets("Convergence").Cells(PrintRow2, 1).Value = t
'   Worksheets("Convergence").Cells(PrintRow2, 2).Value = MeanVol.A1(0)
'   Worksheets("Convergence").Cells(PrintRow2, 3).Value = MeanVol.H1(0)
'   Worksheets("Convergence").Cells(PrintRow2, 4).Value = MeanVol.B1(0)
'   If PrintRow2 >= 202 Then PrintRow2 = 2
'   Check1 = Worksheets("Convergence").Cells(3, 8).Value
'   Check2 = Worksheets("Convergence").Cells(3, 9).Value
'   Check3 = Worksheets("Convergence").Cells(3, 10).Value
'   If CycleNumber > 200 And Check1 < 25 And Check2 < 25 And Check3
< 25 Or t > Finished Then
'       Converged = True
'       Finished = t
'       Beep
'       Beep
'       Beep
'       Sheets("Raw Data").Select
'   End If
' End If

'   If CycleNumber > 1000 Then
'       Converged = True
'       Finished = t
'       Sheets("Raw Data").Select
'   End If

'*****
' REPEAT LOOP
'*****

Loop

'*****
'   Quit computation and return results
'*****

'   If Engine = 0 Then

'   Results(1) = Finished

'   For i = 4 To PrintBuffer * 10 + 4
'       Results(2) = Worksheets("Raw Data").Cells(i, 46).Value _
'                   / (PrintBuffer * 10) + Results(2)
'       Results(3) = Worksheets("Raw Data").Cells(i, 47).Value _
'                   / (PrintBuffer * 10) + Results(3)
'   Next i

'   End If

Exit Function

ChangeViews:
'   If Err = 18 Then
'       Answer = MsgBox("Would you like to view a different screen or
change refresh rate?", vbYesNoCancel)
'       If Answer = vbCancel Then 'Continue at the point of
interruption
'           Resume
'       ElseIf Answer = vbNo Then 'End Program

```

```

        Exit Function
    Else 'Enable dialog box to change to view
        ViewChanger
        Resume
    End If
Else 'Handle other errors
    MsgBox Error(Err)
    Exit Function
End If

```

```
End Function
```

```
Function PV_Area(Curve, num)
```

```

    Dim j As Integer

    For j = 1 To num
        PV_Area = PV_Area + Abs(((Curve(1, j - 1) + Curve(1, j)) / 2) * _
            (Curve(2, j - 1) - Curve(2, j)))
    Next j
End Function

```

```
Sub ViewChanger()
```

```

    DialogSheets("View Changer").Show

    If DialogSheets("View Changer").OptionButtons(1).Value = xlOn
Then
        Sheets("Virtual Pistons").Select
        Worksheets("Parameter Values").Range("A25").Value = "Virtual
Pistons"

        ElseIf DialogSheets("View Changer").OptionButtons(2).Value =
xlOn Then
            Sheets("Virtual Pistons II").Select
            Worksheets("Parameter Values").Range("A25").Value = "Virtual
Pistons II"

            ElseIf DialogSheets("View Changer").OptionButtons(3).Value =
xlOn Then
                Sheets("Power Data").Select
                Worksheets("Parameter Values").Range("A25").Value = "Power
Data"

                ElseIf DialogSheets("View Changer").OptionButtons(4).Value =
xlOn Then
                    Sheets("Parameter Values").Select
                    Worksheets("Parameter Values").Range("A25").Value =
"Parameter Values"

                    ElseIf DialogSheets("View Changer").OptionButtons(5).Value =
xlOn Then
                        Sheets("Convergence").Select
                        Worksheets("Parameter Values").Range("A25").Value =
"Convergence"

```



```

        ElseIf DialogSheets("View Changer").OptionButtons(6).Value =
xlOn Then
            Sheets("Parameters").Select
            Worksheets("Parameter Values").Range("A25").Value =
"Parameters"

            ElseIf DialogSheets("View Changer").OptionButtons(7).Value =
xlOn Then
                Sheets("Interface").Select
                Worksheets("Parameter Values").Range("A25").Value =
"Interface"

                End If

            If DialogSheets("View Changer").OptionButtons(8).Value = xlOn
Then
                Worksheets("Parameter Values").Range("B5").Value = 1

                ElseIf DialogSheets("View Changer").OptionButtons(9).Value =
xlOn Then
                    Worksheets("Parameter Values").Range("B5").Value = 10

                    ElseIf DialogSheets("View Changer").OptionButtons(10).Value =
xlOn Then
                        Worksheets("Parameter Values").Range("B5").Value = 100

                        ElseIf DialogSheets("View Changer").OptionButtons(11).Value =
xlOn Then
                            Worksheets("Parameter Values").Range("B5").Value = 1000

                            ElseIf DialogSheets("View Changer").OptionButtons(12).Value =
xlOn Then
                                Worksheets("Parameter Values").Range("B5").Value =
DialogSheets("View Changer").EditBoxes("Edit Box 21").Text

                                End If

            End Sub

```

# APPENDIX C: FORTRAN OPTIMIZATION CODE

```
C ABSTRACT:
C Simulated annealing is a global optimization method that
distinguishes
C between different local optima. Starting from an initial point, the
C algorithm takes a step and the function is evaluated. When
minimizing a
C function, any downhill step is accepted and the process repeats from
this
C new point. An uphill step may be accepted. Thus, it can escape from
local
C optima. This uphill decision is made by the Metropolis criteria. As
the
C optimization process proceeds, the length of the steps decline and
the
C algorithm closes in on the global optimum. Since the algorithm makes
very
C few assumptions regarding the function to be optimized, it is quite
C robust with respect to non-quadratic surfaces. The degree of
robustness
C can be adjusted by the user. In fact, simulated annealing can be
used as
C a local optimizer for difficult functions.
C
C This implementation of simulated annealing was used in "Global
Optimization
C of Statistical Functions with Simulated Annealing," Goffe, Ferrier
and
C Rogers, Journal of Econometrics, vol. 60, no. 1/2, Jan./Feb. 1994,
pp.
C 65-100. Briefly, we found it competitive, if not superior, to
multiple
C restarts of conventional optimization routines for difficult
optimization
C problems.
C
C For more information on this routine, contact its author:
C Bill Goffe, bgoffe@whale.st.usm.edu
C
PROGRAM SIMANN
C This file is an example of the Corana et al. simulated annealing
C algorithm for multimodal and robust optimization as implemented
C and modified by Goffe, Ferrier and Rogers. Counting the above line
C ABSTRACT as 1, the routine itself (SA), with its supplementary
C routines, is on lines 232-990. A multimodal example from Judge et al.
C (FCN) is on lines 150-231. The rest of this file (lines 1-149) is a
C driver routine with values appropriate for the Judge example. Thus,
this
C example is ready to run.
C
C To understand the algorithm, the documentation for SA on lines 236-
C 484 should be read along with the parts of the paper that describe
C simulated annealing. Then the following lines will then aid the user
C in becoming proficient with this implementation of simulated
C annealing.
C
C Learning to use SA:
C Use the sample function from Judge with the following suggestions
```

C to get a feel for how SA works. When you've done this, you should be  
C ready to use it on most any function with a fair amount of expertise.  
C 1. Run the program as is to make sure it runs okay. Take a look at  
C the intermediate output and see how it optimizes as temperature  
C (T) falls. Notice how the optimal point is reached and how  
C falling T reduces VM.  
C 2. Look through the documentation to SA so the following makes a  
C bit of sense. In line with the paper, it shouldn't be that hard  
C to figure out. The core of the algorithm is described on pp. 68-  
70  
C and on pp. 94-95. Also see Corana et al. pp. 264-9.  
C 3. To see how it selects points and makes decisions about uphill  
C and downhill moves, set IPRINT = 3 (very detailed intermediate  
C output) and MAXEVL = 100 (only 100 function evaluations to limit  
C output).  
C 4. To see the importance of different temperatures, try starting  
C with a very low one (say T = 10E-5). You'll see (i) it never  
C escapes from the local optima (in annealing terminology, it  
C quenches) & (ii) the step length (VM) will be quite small. This  
C is a key part of the algorithm: as temperature (T) falls, step  
C length does too. In a minor point here, note how VM is quickly  
C reset from its initial value. Thus, the input VM is not very  
C important. This is all the more reason to examine VM once the  
C algorithm is underway.  
C 5. To see the effect of different parameters and their effect on  
C the speed of the algorithm, try RT = .95 & RT = .1. Notice the  
C vastly different speed for optimization. Also try NT = 20. Note  
C that this sample function is quite easy to optimize, so it will  
C tolerate big changes in these parameters. RT and NT are the  
C parameters one should adjust to modify the runtime of the  
C algorithm and its robustness.  
C 6. Try constraining the algorithm with either LB or UB.

PARAMETER (N = 8, NEPS = 4)

DOUBLE PRECISION LB(N), UB(N), X(N), XOPT(N), C(N), VM(N),  
1 FSTAR(NEPS), XP(N), T, EPS, RT, FOPT

INTEGER NACP(N), NS, NT, NFCNEV, IER, ISEED1, ISEED2,  
1 MAXEVL, IPRINT, NACC, NOBDS

LOGICAL MAX

EXTERNAL FCN

C Set underflows to zero on IBM mainframes.

C CALL XUFLOW(0)

OPEN (7, FILE='SIMDAT.DAT', STATUS='UNKNOWN')

C Set input parameters.

MAX = .TRUE.

EPS = 1.0D-6

RT = .85

ISEED1 = 1

ISEED2 = 2

NS = 20

NT = 5

MAXEVL = 50

IPRINT = 3

LB(1) = .1

```

UB(1) = 10.
LB(2) = 10.
UB(2) = 1000.
DO I= 3 , 6
    LB(I)=15.
    UB(I)=200.
End Do
LB(7) = 10.
UB(7) = 500.
LB(8) = .5
UB(8) = .95
Do I= 1, N
    C(I) = 2.0
End Do

```

C Note start at local, but not global, optima of the Judge function.

```

X(1) = .5
X(2) = 100.
X(3) = 30.
X(4) = 30.
X(5) = 30.
X(6) = 30.
X(7) = 100.
X(8) = .5

```

C Set input values of the input/output parameters.

```

T = 5.0
DO 20, I = 1, N
    VM(I) = 1.0
20 CONTINUE

```

```

WRITE(7,1000) N, MAX, T, RT, EPS, NS, NT, NEPS, MAXEVL, IPRINT,
1 ISEED1, ISEED2

```

```

CALL PRTVEC(X,N,'STARTING VALUES')
CALL PRTVEC(VM,N,'INITIAL STEP LENGTH')
CALL PRTVEC(LB,N,'LOWER BOUND')
CALL PRTVEC(UB,N,'UPPER BOUND')
CALL PRTVEC(C,N,'C VECTOR')

```

```

WRITE(7,'(/,' ' **** END OF DRIVER ROUTINE OUTPUT ****'
1 /,' ' **** BEFORE CALL TO SA. ****')')

```

```

CALL SA(N,X,MAX,RT,EPS,NS,NT,NEPS,MAXEVL,LB,UB,C,IPRINT,ISEED1,
1 ISEED2,T,VM,XOPT,FOPT,NACC,NFCNEV,NOBDS,IER,
2 FSTAR,XP,NACP)

```

```

WRITE(7,'(/,' ' **** RESULTS AFTER SA **** ')')
CALL PRTVEC(XOPT,N,'SOLUTION')
CALL PRTVEC(VM,N,'FINAL STEP LENGTH')
WRITE(7,1001) FOPT, NFCNEV, NACC, NOBDS, T, IER

```

```

1000 FORMAT(/,' SIMULATED ANNEALING EXAMPLE',/,
1 /,' NUMBER OF PARAMETERS: ',I3,' MAXIMAZATION: ',L5,
2 /,' INITIAL TEMP: ',G8.2,' RT: ',G8.2,' EPS: ',G8.2,
3 /,' NS: ',I3,' NT: ',I2,' NEPS: ',I2,
4 /,' MAXEVL: ',I10,' IPRINT: ',I1,' ISEED1: ',I4,
5 ' ISEED2: ',I4)
1001 FORMAT(/,' OPTIMAL FUNCTION VALUE: ',G20.13
1 /,' NUMBER OF FUNCTION EVALUATIONS: ',I10,
2 /,' NUMBER OF ACCEPTED EVALUATIONS: ',I10,
3 /,' NUMBER OF OUT OF BOUND EVALUATIONS: ',I10,
4 /,' FINAL TEMP: ',G20.13,' IER: ',I3)

```

STOP

```

      END
C *****
C *****

      SUBROUTINE FCN(Var, X, Engine)

      Double Precision X(8),engine
      Integer Var

C*****
C*****      DECLARATION OF VARIABLES      *****
C*****      All units are expressed in CGS system      *****
C*****

C   Pi      -   Pi (any questions?)
      Real Pi

C   g      -   gravitaional acceleration constant
      Real g

C   f      -   Fanning friction factor
      Real f

C   d      -   density of the working fluid (water)
      Real d

C   R      -   gas constant
      Real R

C   Dia*** -   Diameters for the following pipes:
C             -   Tuning pipes, Ambient, hot, and cold columns
C   _BC    -   Bounce Chamber columns
      Real Dia, DiaBC

C   Area*** -   Cross-sectional area for the following pipes:
C             -   Tuning pipes, Ambient, hot, and cold columns
C   _BC    -   Bounce Chamber columns
      Real Area, AreaBC

C   Dt     -   time interval between iterations
      Real Dt

C   L      -   height of the bounce, ambient, hot, or cold columns
      Real LB, LA, LH, LC

C   LL     -   initial height of the water in all of the columns
      Real LL
      Real Full

C   T*     -   temperature of the following columns:
C   H      -   hot
C   A      -   ambient
C   C      -   cold
C   B      -   bounce
      Real TH, TA, TB, TC

C   Pmean  -   mean gas pressure in the gas equalization line
      Real Pmean

C   VB     -   volume of the regenerator between the ambient and
C             hot/cold columns
      Real VB

C   Damp   -   damping factor for mean gas volume calculations

```

Real Damp

C L\*\* - height of liquid in the ambient, hot, cold, or bounce  
C chamber  
Real LA1, LH1, LB1, LA2, LC2, LB2, LA3, LH3, LB3, LA4, LC4, LB4

C vl\*\*\* - liquid velocities in the columns. see figure 5 p. 15  
Real vl12a, vl12b, vl12c, vl23a, vl23b, vl23c  
Real vl34a, vl34b, vl34c, vl41a, vl41b, vl41c

C Vo\*\* - volume of gas in each column  
Real VoH1, VoH3, VoC2, VoC4, VoB1, VoB2  
Real VoB3, VoB4, VoA1, VoA2, VoA3, VoA4

C Vo\*\*o - initial volume of gas in each column  
Real VoH1o, VoH3o, VoC2o, VoC4o, VoB1o, VoB2o  
Real VoB3o, VoB4o, VoA1o, VoA2o, VoA3o, VoA4o

C P\*\* - pressure of gas in each column  
Real PA, PB, PC, PD, PB1, PB2, PB3, PB4

C P\*\*o - initial pressure of gas in each column  
Real PAo, PBo, PCo, PDo, PB1o, PB2o, PB3o, PB4o

C j - mean gas volume counter  
Integer j

C MeanVol - set of variables used in the calculation of the mean  
volume  
C of gas present in each chamber

Integer MVCount(12)  
Real MVA1(21)  
Real MVA2(21)  
Real MVA3(21)  
Real MVA4(21)  
Real MVH1(21)  
Real MVC2(21)  
Real MVH3(21)  
Real MVC4(21)  
Real MVB1(21)  
Real MVB2(21)  
Real MVB3(21)  
Real MVB4(21)

C t - time in seconds  
Real t

C m,n,u,v - counters used for the calculation of the area  
C inside the PV curve  
Integer m, n, u, v

C p,w - counters used for the calculation of Power1 output  
C from engines 1 & 3  
Integer p, w

C Powcycle - counter used to average the Power1 from x cycles  
Integer Powcycle

C PP\* - intermediate variables used in the calculation of  
PA,PB,PC,PD  
Real PP1, PP2, PP3, PP4

C P1\_,P2\_,P3\_ - pressure of liquid in column

```

Real P1A, P1B, P1C, P1D
Real P2A, P2B, P2C, P2D
Real P3A, P3B, P3C, P3D

C i1,i3,i5 - direction of liquid in column
Real I1, I3, I5

C X***-intermediate variables used in the calculation of P1_,P2_,P3_
Real X11, X12, X13, X14, X15, X21
Real X16, X17, X18, X19, X110, X22
Real X111, X112, X113, X114, X115, X23
Real X116, X117, X118, X119, X120, X24

C Lt1,Lt2 - lengths of the tuning pipes
Real Lt1, Lt2

C a*** - liquid acceleration terms for each column of water
Real a12a, a23a, a34a, a41a
Real a12b, a23b, a34b, a41b
Real a12c, a23c, a34c, a41c

C vl***o - liquid velocity buffer
Real vl12ao, vl23ao, vl34ao, vl41ao
Real vl12bo, vl23bo, vl34bo, vl41bo
Real vl12co, vl23co, vl34co, vl41co

C Chamber,Up,Down - counters used in the calculation of the mean gas
volume
Integer Chamber
Integer Up(12), Down(12)
Real SumVol(12), sum

C-Variables used to calculate the Power1 output from engines 1 & 3
Real PosArea, NegArea, AvePow1
Real PosArea3, NegArea3, AvePow3
Real PosCur1(2, 10000), NegCur1(2, 10000), Power1(1000)
Real PosCur3(2, 10000), NegCur3(2, 10000), Power3(1000)
Real Initial1, Initial3
Integer ii

C neg, sup - counters used to check if blowout or negative height
C has occurred
Integer neg, sup

C - variables used to determine convergance
Integer CycleNum

C*****
C*****
C Unloading Parameter Data from Passed Array
C*****
C*****

Lt2 = X(2) / (1. + X(1))
Lt1 = X(2) - Lt2
LH = X(3)
LC = X(4)
LA = X(5)
LB = X(6)
VB = X(7)
Full=X(8)

```

```
C*****
C Reading Parameter Data from Spreadsheet "Initial Conditions"
C*****
```

```
Pi = 3.1415927
g = 981.
f = 0.03
d = 1.
R = 82880600.
Dia = 5.
DiaBC = 4.5
Dt = 0.001
TH = 537.78
TA = 316.
TC = 286.
TB = 289.
Pmean = 1010000.
Damp = 0.5
```

```
C*****
C Cross-sectional Area Calculations
C*****
```

```
Area = Pi * Dia ** 2. / 4.
AreaBC = Pi * DiaBC ** 2. / 4.
```

```
C*****
C Initializing of liquid heights
C*****
```

```
If (LH .LE. LA) Then
  If (LH .LE. LC) Then
    IF (LH .LE. LB) Then
      LL = LH * Full
    End If
  End If
End IF
```

```
If (LA .LE. LH) Then
  If (LA .LE. LC) Then
    IF (LA .LE. LB) Then
      LL = LA * Full
    End If
  End If
End IF
```

```
If (LC .LE. LA) Then
  If (LC .LE. LH) Then
    IF (LC .LE. LB) Then
      LL = LC * Full
    End If
  End If
End IF
```

```
If (LB .LE. LA) Then
  If (LB .LE. LC) Then
    IF (LB .LE. LH) Then
      LL = LB * Full
    End If
  End If
End IF
```

```
LA1 = LL
```



LH1 = LL  
LB1 = LL + 0.2  
LA2 = LL  
LC2 = LL  
LB2 = LL  
LA3 = LL  
LH3 = LL  
LB3 = LL - 0.2  
LA4 = LL  
LC4 = LL  
LB4 = LL

C\*\*\*\*\*  
C Initializing of liquid velocities in each column  
C\*\*\*\*\*

vl12a = 0.  
vl12b = 0.  
vl12c = 0.  
vl23a = 0.  
vl23b = 0.  
vl23c = 0.  
vl34a = 0.  
vl34b = 0.  
vl34c = 0.  
vl41a = 0.  
vl41b = 0.  
vl41c = 0.

C\*\*\*\*\*  
C Initializing of gas volumes in each column  
C\*\*\*\*\*

VoA1 = Area \* (LA - LA1)  
VoH1 = Area \* (LH - LH1)  
VoB1 = AreaBC \* (LB - LB1)  
VoA2 = Area \* (LA - LA2)  
VoC2 = Area \* (LC - LC2)  
VoB2 = AreaBC \* (LB - LB2)  
VoA3 = Area \* (LA - LA3)  
VoH3 = Area \* (LH - LH3)  
VoB3 = AreaBC \* (LB - LB3)  
VoA4 = Area \* (LA - LA4)  
VoC4 = Area \* (LC - LC4)  
VoB4 = AreaBC \* (LB - LB4)

C\*\*\*\*\*  
C Initializing of gas pressures in each column  
C\*\*\*\*\*

PA = Pmean  
PB = Pmean  
PC = Pmean  
PD = Pmean  
PB1 = Pmean  
PB2 = Pmean  
PB3 = Pmean  
PB4 = Pmean

C\*\*\*\*\*  
C INITIALIZATION OF TIME AND OTHER COUNTERS  
C\*\*\*\*\*

Do j = 1, 12

```

MVCCount(j) = 1
Up(j) = 0
Down(j) = 0
SumVol(j) = 0.
End Do

Do j = 1, 21
MVA1(j) = Area * (LA - LL)
MVA2(j) = Area * (LA - LL)
MVA3(j) = Area * (LA - LL)
MVA4(j) = Area * (LA - LL)
MVH1(j) = Area * (LH - LL)
MVC2(j) = Area * (LC - LL)
MVH3(j) = Area * (LH - LL)
MVC4(j) = Area * (LC - LL)
MVB1(j) = AreaBC * (LB - LL)
MVB2(j) = AreaBC * (LB - LL)
MVB3(j) = AreaBC * (LB - LL)
MVB4(j) = AreaBC * (LB - LL)
End Do

```

```

t = 0.
m = 1
n = 1
p = 1
u = 1
v = 1
w = 1
Powcycle = 99
Engine = 0.
CycleNum = 0
sum=0.
PosArea=0.
NegArea=0.
AvePow1=0.
AvePow3=0.
Initial1=0.
Initial3=0.
neg=0
sup=0

```

```

C*****
C BEGINNING OF MAIN LOOP
C*****

```

```

1005 If (CycleNum.EQ. 1000) then
      GOTO 1009
End IF

```

```

C*****
C INITIALIZATION OF GAS VOLUMES
C*****

```

```

VoH1o = VoH1
VoA1o = VoA1
VoC2o = VoC2
VoH3o = VoH3
VoA3o = VoA3
VoC4o = VoC4
VoA2o = VoA2
VoA4o = VoA4
VoB1o = VoB1
VoB2o = VoB2
VoB3o = VoB3

```

VoB4o = VoB4

C\*\*\*\*\*  
C   INITIALIZATION OF GAS PRESSURES  
C\*\*\*\*\*

PAo = PA  
PBo = PB  
PCo = PC  
PDo = PD  
PB1o = PB1  
PB2o = PB2  
PB3o = PB3  
PB4o = PB4

C\*\*\*\*\*  
C   CALCULATION OF GAS VOLUMES  
C\*\*\*\*\*

VoA1 = Area \* (LA - LA1)  
VoH1 = Area \* (LH - LH1)  
VoB1 = AreaBC \* (LB - LB1)  
VoA2 = Area \* (LA - LA2)  
VoC2 = Area \* (LC - LC2)  
VoB2 = AreaBC \* (LB - LB2)  
VoA3 = Area \* (LA - LA3)  
VoH3 = Area \* (LH - LH3)  
VoB3 = AreaBC \* (LB - LB3)  
VoA4 = Area \* (LA - LA4)  
VoC4 = Area \* (LC - LC4)  
VoB4 = AreaBC \* (LB - LB4)

C\*\*\*\*\*  
C   CALCULATION OF GAS PRESSURES VIA THE IDEAL GAS LAW  
C\*\*\*\*\*

PP1 = Pmean\*(MVH1(21)/TH + 2. \* VB / (TH + TA) + MVA1(21) / TA)  
PP3 = Pmean\*(MVH3(21)/TH + 2. \* VB / (TH + TA) + MVA3(21) / TA)  
PA = PP1/(VoH1 / TH + 2. \* VB / (TH + TA) + VoA1 / TA)  
PC = PP3/(VoH3 / TH + 2. \* VB / (TH + TA) + VoA3 / TA)  
PP2 = Pmean\*(MVA2(21)/TA + 2. \* VB / (TA + TC) + MVC2(21) / TC)  
PP4 = Pmean\*(MVA4(21)/TA + 2. \* VB / (TA + TC) + MVC4(21) / TC)  
PB = PP2/(VoA2 / TA + 2. \* VB / (TA + TC) + VoC2 / TC)  
PD = PP4/(VoA4 / TA + 2. \* VB / (TA + TC) + VoC4 / TC)  
PB1 = Pmean\*MVB1(21) / VoB1  
PB2 = Pmean\*MVB2(21) / VoB2  
PB3 = Pmean\*MVB3(21) / VoB3  
PB4 = Pmean\*MVB4(21) / VoB4

C\*\*\*\*\*  
C   CALCULATION OF LIQUID PRESSURES  
C\*\*\*\*\*

C P2A  
  IF (vl12a.gt.0.) then  
    I1 = 1  
  Else  
    I1 = -1  
  End If  
  
  IF (vl12b.gt.0.) then  
    I3 = 1  
  Else  
    I3 = -1

```

End If

IF (vl12c.gt.0.) then
    I5 = 1
Else
    I5 = -1
End If

X11 = PB1 + d * g * LB1 * (2. * (Dia/DiaBC)**2. + 1.)
X12 = (PA - PA * Lt1 / (LH1 + Lt1)) * (LB1 / LH1) *
(Dia/DiaBC)**2.
X13 = (PB - PB * Lt2 / (LA2 + Lt2)) * (LB1 / LA2) *
(Dia/DiaBC)**2.
X14 = (d * g * LB1 * Lt1 / (LH1 + Lt1) + d * g * LB1 * Lt2 /
1 (LA2 + Lt2)) * (Dia/DiaBC)**2.
X15 = 1. + LB1 / (LH1 + Lt1) * (Dia/DiaBC)**2. + LB1 /
1 (LA2 + Lt2) * (Dia/DiaBC)**2.
X21 = 2. * f * d * LB1 * (-I3 * vl12b**2. / DiaBC - I5 *
1Dia * vl12c**2. / (DiaBC * DiaBC) + I1 * Dia * vl12a *
2vl12a / (DiaBC * DiaBC))
P2A = (X11 + X12 + X13 - X14 + X21) / X15

```

C P2B

```

IF (vl23a.gt.0.) then
    I1 = 1
Else
    I1 = -1
End If

```

```

IF (vl23b.gt.0.) then
    I3 = 1
Else
    I3 = -1
End If

```

```

IF (vl23c.gt.0.) then
    I5 = 1
Else
    I5 = -1
End If

```

```

X16 = PB2 + d * g * LB2 * (2. * (Dia/DiaBC)**2. + 1.)
X17 = (PB - PB * Lt1 / (LC2 + Lt1)) * (LB2 / LC2) *
(Dia/DiaBC)**2.
X18 = (PC - PC * Lt2 / (LA3 + Lt2)) * (LB2 / LA3) *
(Dia/DiaBC)**2.
X19 = (d * g * LB2 * Lt1 / (LC2 + Lt1) + d * g * LB2 * Lt2 /
1 (LA3 + Lt2)) * (Dia/DiaBC)**2.
X110 = 1. + LB2 / (LC2+Lt1) * (Dia/DiaBC)**2. + LB2 /
1 (LA3 + Lt2) * (Dia/DiaBC)**2.
X22 = 2. * f * d * LB2 * (-I3 * vl23b**2. / DiaBC - I5 *
1Dia * vl23c ** 2. / (DiaBC * DiaBC) + I1 * Dia * vl23a *
2vl23a / (DiaBC * DiaBC))
P2B = (X16 + X17 + X18 - X19 + X22) / X110

```

C P2C

```

IF (vl34a.gt.0.) then
    I1 = 1
Else
    I1 = -1
End If

```

```

IF (vl34b.gt.0.) then
    I3 = 1

```

```

Else
    I3 = -1
End If

IF (vl34c.gt.0.) then
    I5 = 1
Else
    I5 = -1
End If

X111 = PB3 + d * g * LB3 * (2. * (Dia/DiaBC)**2. + 1.)
X112 = (PC - PC * Lt1 / (LH3 + Lt1)) * (LB3 / LH3) *
1 (Dia/DiaBC)**2.
X113 = (PD - PD * Lt2 / (LA4 + Lt2)) * (LB3 / LA4) *
1 (Dia/DiaBC)**2.
X114 = (d * g * LB3 * Lt1 / (LH3 + Lt1) + d * g * LB3 * Lt2 /
1 (LA4 + Lt2)) * (Dia/DiaBC)**2.
X115 = 1. + LB3 / (LH3 + Lt1) * (Dia/DiaBC)**2. + LB3 /
1 (LA4 + Lt2) * (Dia/DiaBC)**2.
X23 = 2. * f * d * LB3 * (-I3 * vl34b**2. / DiaBC - I5 *
1 Dia * vl34c**2. / (DiaBC * DiaBC) + I1 * Dia *
2 vl34a * vl34a / (DiaBC * DiaBC))
P2C = (X111 + X112 + X113 - X114 + X23) / X115

```

C P2D

```

IF (vl41a.gt.0.) then
    I1 = 1
Else
    I1 = -1
End If

IF (vl41b.gt.0.) then
    I3 = 1
Else
    I3 = -1
End If

IF (vl41c.gt.0.) then
    I5 = 1
Else
    I5 = -1
End If

X116 = PB4 + d * g * LB4 * (2. * (Dia/DiaBC)**2. + 1.)
X117 = (PD - PD * Lt1 / (LC4 + Lt1)) * (LB4 / LC4) *
1 (Dia/DiaBC)**2.
X118 = (PA - PA * Lt2 / (LA1 + Lt2)) * (LB4 / LA1) *
1 (Dia/DiaBC)**2.
X119 = (d * g * LB4 * Lt1 / (LC4 + Lt1) + d * g * LB4 * Lt2 /
1 (LA1 + Lt2)) * (Dia/DiaBC)**2.
X120 = 1. + LB4 / (LC4 + Lt1) * (Dia/DiaBC)**2. + LB4 /
1 (LA1 + Lt2) * (Dia/DiaBC)**2.
X24 = 2. * f * d * LB4 * (-I3 * vl41b**2. / DiaBC - I5 *
1 Dia * vl41c**2. / (DiaBC * DiaBC) + I1 * Dia * vl41a *
2 vl41a / (DiaBC * DiaBC))
P2D = (X116 + X117 + X118 - X119 + X24) / X120

P1A = (PA * Lt1 + g * d * LH1 * Lt1 + P2A * LH1) / (LH1 + Lt1)
P1B = (PB * Lt1 + g * d * LC2 * Lt1 + P2B * LC2) / (LC2 + Lt1)
P1C = (PC * Lt1 + g * d * LH3 * Lt1 + P2C * LH3) / (LH3 + Lt1)
P1D = (PD * Lt1 + g * d * LC4 * Lt1 + P2D * LC4) / (LC4 + Lt1)

P3A = (g * d * Lt2 * LA2 + PB * Lt2 + P2A * LA2) / (Lt2 + LA2)
P3B = (g * d * Lt2 * LA3 + PC * Lt2 + P2B * LA3) / (Lt2 + LA3)

```

$$P3C = (g * d * Lt2 * LA4 + PD * Lt2 + P2C * LA4) / (Lt2 + LA4)$$

$$P3D = (g * d * Lt2 * LA1 + PA * Lt2 + P2D * LA1) / (Lt2 + LA1)$$

C\*\*\*\*\*  
 C CALCULATION OF LIQUID ACCELERATIONS  
 C\*\*\*\*\*

```

If (v112a .LE. 0.) Then
a12a = (PA - P1A) / (d * LH1) + g + 2. * f * v112a * v112a / Dia
End If
If (v112a .GT. 0.) Then
a12a = (PA - P1A) / (d * LH1) + g - 2. * f * v112a * v112a / Dia
End If
If (v123a .LE. 0.) Then
a23a = (PB - P1B) / (d * LC2) + g + 2. * f * v123a * v123a / Dia
End If
If (v123a .GT. 0.) Then
a23a = (PB - P1B) / (d * LC2) + g - 2. * f * v123a * v123a / Dia
End If
If (v134a .LE. 0.) Then
a34a = (PC - P1C) / (d * LH3) + g + 2. * f * v134a * v134a / Dia
End If
If (v134a .GT. 0.) Then
a34a = (PC - P1C) / (d * LH3) + g - 2. * f * v134a * v134a / Dia
End If
If (v141a .LE. 0.) Then
a41a = (PD - P1D) / (d * LC4) + g + 2. * f * v141a * v141a / Dia
End If
If (v141a .GT. 0.) Then
a41a = (PD - P1D) / (d * LC4) + g - 2. * f * v141a * v141a / Dia
End If
If (v112b .LE. 0.) Then
a12b = (P2A - PB1) / (d * LB1) - g + 2. * f * v112b **2. / DiaBC
End If
If (v112b .GT. 0.) Then
a12b = (P2A - PB1) / (d * LB1) - g - 2. * f * v112b **2. / DiaBC
End If
If (v123b .LE. 0.) Then
a23b = (P2B - PB2) / (d * LB2) - g + 2. * f * v123b **2. / DiaBC
End If
If (v123b .GT. 0.) Then
a23b = (P2B - PB2) / (d * LB2) - g - 2. * f * v123b **2. / DiaBC
End If
If (v134b .LE. 0.) Then
a34b = (P2C - PB3) / (d * LB3) - g + 2. * f * v134b **2. / DiaBC
End If
If (v134b .GT. 0.) Then
a34b = (P2C - PB3) / (d * LB3) - g - 2. * f * v134b **2. / DiaBC
End If
If (v141b .LE. 0.) Then
a41b = (P2D - PB4) / (d * LB4) - g + 2. * f * v141b **2. / DiaBC
End If
If (v141b .GT. 0.) Then
a41b = (P2D - PB4) / (d * LB4) - g - 2. * f * v141b **2. / DiaBC
End If

a12c = a12a - (DiaBC / Dia) * (DiaBC / Dia) * a12b
a23c = a23a - (DiaBC / Dia) * (DiaBC / Dia) * a23b
a34c = a34a - (DiaBC / Dia) * (DiaBC / Dia) * a34b
a41c = a41a - (DiaBC / Dia) * (DiaBC / Dia) * a41b

t = t + Dt

```

C\*\*\*\*\*

C CALCULATION OF VELOCITY BUFFER

C\*\*\*\*\*

vl12ao = vl12a  
 vl12bo = vl12b  
 vl12co = vl12c  
 vl23ao = vl23a  
 vl23bo = vl23b  
 vl23co = vl23c  
 vl34ao = vl34a  
 vl34bo = vl34b  
 vl34co = vl34c  
 vl41ao = vl41a  
 vl41bo = vl41b  
 vl41co = vl41c

C\*\*\*\*\*

C CALCULATION OF LIQUID VELOCITIES

C\*\*\*\*\*

vl12a = vl12ao + a12a \* Dt  
 vl12b = vl12bo + a12b \* Dt  
 vl12c = vl12co + a12c \* Dt  
 vl23a = vl23ao + a23a \* Dt  
 vl23b = vl23bo + a23b \* Dt  
 vl23c = vl23co + a23c \* Dt  
 vl34a = vl34ao + a34a \* Dt  
 vl34b = vl34bo + a34b \* Dt  
 vl34c = vl34co + a34c \* Dt  
 vl41a = vl41ao + a41a \* Dt  
 vl41b = vl41bo + a41b \* Dt  
 vl41c = vl41co + a41c \* Dt

C\*\*\*\*\*

C CALCULATION OF LIQUID POSITIONS IN EACH COLUMN

C\*\*\*\*\*

LH1 = LH1 - vl12ao \* Dt - 0.5 \* a12a \* Dt \* Dt  
 LB1 = LB1 + vl12bo \* Dt + 0.5 \* a12b \* Dt \* Dt  
 LA2 = LA2 + vl12co \* Dt + 0.5 \* a12c \* Dt \* Dt  
 LC2 = LC2 - vl23ao \* Dt - 0.5 \* a23a \* Dt \* Dt  
 LB2 = LB2 + vl23bo \* Dt + 0.5 \* a23b \* Dt \* Dt  
 LA3 = LA3 + vl23co \* Dt + 0.5 \* a23c \* Dt \* Dt  
 LH3 = LH3 - vl34ao \* Dt - 0.5 \* a34a \* Dt \* Dt  
 LB3 = LB3 + vl34bo \* Dt + 0.5 \* a34b \* Dt \* Dt  
 LA4 = LA4 + vl34co \* Dt + 0.5 \* a34c \* Dt \* Dt  
 LC4 = LC4 - vl41ao \* Dt - 0.5 \* a41a \* Dt \* Dt  
 LB4 = LB4 + vl41bo \* Dt + 0.5 \* a41b \* Dt \* Dt  
 LA1 = LA1 + vl41co \* Dt + 0.5 \* a41c \* Dt \* Dt

C\*\*\*\*\*

C CALCULATION OF MEAN GAS VOLUME IN EACH CHAMBER

C\*\*\*\*\*

C\*\*\*\*\* Ambient Chamber 1 \*\*\*\*\*

Chamber = 1

If (VoA1 .GT. VoA1o) Then  
 If (Up(Chamber) .GT. 0) Then  
 MVA1(MVCount(Chamber)) = SumVol(Chamber) /  
 1 (Up(Chamber) + Down(Chamber))  
 sum = 0.  
 DO j = 1 , 20

```

        sum = MVA1(j) / 20. + sum
    End DO
    MVA1(21) = (sum - MVA1(21)) * Damp + sum
    MVCount(Chamber) = MVCount(Chamber) + 1
    If (MVCount(Chamber) .EQ. 21) Then
        MVCount(Chamber) = 1
    End IF
    Up(Chamber) = 0
    Down(Chamber) = 0
    SumVol(Chamber) = 0.
End If
Down(Chamber) = Down(Chamber) + 1
SumVol(Chamber) = SumVol(Chamber) + VoA1
Else
    SumVol(Chamber) = SumVol(Chamber) + VoA1
    Up(Chamber) = Up(Chamber) + 1
End If

C***** Hot Chamber 1 *****

Chamber = 2

If (VoH1 .GT. VoH1o) Then
    If (Up(Chamber) .GT. 0) Then
        MVH1(MVCount(Chamber)) = SumVol(Chamber) /
1      (Up(Chamber) + Down(Chamber))
        sum = 0.
        Do j = 1 , 20.
            sum = MVH1(j) / 20. + sum
        End Do
        MVH1(21) = (sum - MVH1(21)) * Damp + sum
        MVCount(Chamber) = MVCount(Chamber) + 1
        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoH1
Else
    SumVol(Chamber) = SumVol(Chamber) + VoH1
    Up(Chamber) = Up(Chamber) + 1
End If

C***** Bounce Chamber 1 *****

Chamber = 3

If (VoB1 .GT. VoB1o) Then
    If (Up(Chamber) .GT. 0) Then
        MVB1(MVCount(Chamber)) = SumVol(Chamber) /
1      (Up(Chamber) + Down(Chamber))
        sum = 0.
        Do j = 1 ,20
            sum = MVB1(j) / 20. + sum
        End Do
        MVB1(21) = (sum - MVB1(21)) * Damp + sum
        MVCount(Chamber) = MVCount(Chamber) + 1
        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0

```



```

        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoB1
Else
    SumVol(Chamber) = SumVol(Chamber) + VoB1
    Up(Chamber) = Up(Chamber) + 1
End If

```

C\*\*\*\*\* Ambient Chamber 2 \*\*\*\*\*

```

Chamber = 4

If (VoA2 .GT. VoA2o) Then
    If (Up(Chamber) .GT. 0) Then
        MVA2(MVCount(Chamber)) = SumVol(Chamber) /
1         (Up(Chamber) + Down(Chamber))
        sum = 0.
        Do j = 1 , 20
            sum = MVA2(j) / 20. + sum
        End Do
        MVA2(21) = (sum - MVA2(21)) * Damp + sum
        MVCount(Chamber) = MVCount(Chamber) + 1
        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoA2
Else
    SumVol(Chamber) = SumVol(Chamber) + VoA2
    Up(Chamber) = Up(Chamber) + 1
End If

```

C\*\*\*\*\* Cold Chamber 2 \*\*\*\*\*

```

Chamber = 5

If (VoC2 .GT. VoC2o) Then
    If (Up(Chamber) .GT. 0) Then
        MVC2(MVCount(Chamber)) = SumVol(Chamber) /
1         (Up(Chamber) + Down(Chamber))
        sum = 0.
        Do j = 1 , 20
            sum = MVC2(j) / 20. + sum
        End Do
        MVC2(21) = (sum - MVC2(21)) * Damp + sum
        MVCount(Chamber) = MVCount(Chamber) + 1
        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoC2
Else
    SumVol(Chamber) = SumVol(Chamber) + VoC2
    Up(Chamber) = Up(Chamber) + 1

```

```

End If
C***** Bounce Chamber 2 *****
Chamber = 6
If (VoB2 .GT. VoB2o) Then
  If (Up(Chamber) .GT. 0) Then
    MVB2(MVCount(Chamber)) = SumVol(Chamber) /
1      (Up(Chamber) + Down(Chamber))
    sum = 0.
    Do j = 1 , 20
      sum = MVB2(j) / 20. + sum
    End Do
    MVB2(21) = (sum - MVB2(21)) * Damp + sum
    MVCount(Chamber) = MVCount(Chamber) + 1
    If (MVCount(Chamber) .EQ. 21) Then
      MVCount(Chamber) = 1
    End If
    Up(Chamber) = 0
    Down(Chamber) = 0
    SumVol(Chamber) = 0.
  End If
  Down(Chamber) = Down(Chamber) + 1
  SumVol(Chamber) = SumVol(Chamber) + VoB2
Else
  SumVol(Chamber) = SumVol(Chamber) + VoB2
  Up(Chamber) = Up(Chamber) + 1
End If

```

```

C***** Ambient Chamber 3 *****
Chamber = 7
If (VoA3 .GT. VoA3o) Then
  If (Up(Chamber) .GT. 0) Then
    MVA3(MVCount(Chamber)) = SumVol(Chamber) /
1      (Up(Chamber) + Down(Chamber))
    sum = 0.
    Do j = 1 , 20
      sum = MVA3(j) / 20. + sum
    End Do
    MVA3(21) = (sum - MVA3(21)) * Damp + sum
    MVCount(Chamber) = MVCount(Chamber) + 1
    If (MVCount(Chamber) .EQ. 21) Then
      MVCount(Chamber) = 1
    End If
    Up(Chamber) = 0
    Down(Chamber) = 0
    SumVol(Chamber) = 0.
  End If
  Down(Chamber) = Down(Chamber) + 1
  SumVol(Chamber) = SumVol(Chamber) + VoA3
Else
  SumVol(Chamber) = SumVol(Chamber) + VoA3
  Up(Chamber) = Up(Chamber) + 1
End If

```

```

C***** Hot Chamber 3 *****
Chamber = 8
If (VoH3 .GT. VoH3o) Then
  If (Up(Chamber) .GT. 0) Then

```

```

1      MVH3 (MVCCount (Chamber)) = SumVol (Chamber) /
      (Up (Chamber) + Down (Chamber))
      sum = 0.
      Do j = 1 , 20
      sum = MVH3 (j) / 20. + sum
      End Do
      MVH3 (21) = (sum - MVH3 (21)) * Damp + sum
      MVCCount (Chamber) = MVCCount (Chamber) + 1
      If (MVCCount (Chamber) .EQ. 21) Then
      MVCCount (Chamber) = 1
      End If
      Up (Chamber) = 0
      Down (Chamber) = 0
      SumVol (Chamber) = 0.
      End If
      Down (Chamber) = Down (Chamber) + 1
      SumVol (Chamber) = SumVol (Chamber) + VoH3
Else
      SumVol (Chamber) = SumVol (Chamber) + VoH3
      Up (Chamber) = Up (Chamber) + 1
End If

```

C\*\*\*\*\* Bounce Chamber 3 \*\*\*\*\*

```

Chamber = 9

If (VoB3 .GT. VoB3o) Then
  If (Up (Chamber) .GT. 0) Then
1      MVB3 (MVCCount (Chamber)) = SumVol (Chamber) /
      (Up (Chamber) + Down (Chamber))
      sum = 0.
      Do j = 1 , 20
      sum = MVB3 (j) / 20. + sum
      End Do
      MVB3 (21) = (sum - MVB3 (21)) * Damp + sum
      MVCCount (Chamber) = MVCCount (Chamber) + 1
      If (MVCCount (Chamber) .EQ. 21) Then
      MVCCount (Chamber) = 1
      End If
      Up (Chamber) = 0
      Down (Chamber) = 0
      SumVol (Chamber) = 0.
      End If
      Down (Chamber) = Down (Chamber) + 1
      SumVol (Chamber) = SumVol (Chamber) + VoB3
Else
      SumVol (Chamber) = SumVol (Chamber) + VoB3
      Up (Chamber) = Up (Chamber) + 1
End If

```

C\*\*\*\*\* Ambient Chamber 4 \*\*\*\*\*

```

Chamber = 10

If (VoA4 .GT. VoA4o) Then
  If (Up (Chamber) .GT. 0) Then
1      MVA4 (MVCCount (Chamber)) = SumVol (Chamber) /
      (Up (Chamber) + Down (Chamber))
      sum = 0.
      Do j = 1 , 20
      sum = MVA4 (j) / 20. + sum
      End DO
      MVA4 (21) = (sum - MVA4 (21)) * Damp + sum
      MVCCount (Chamber) = MVCCount (Chamber) + 1

```

```

        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoA4
Else
    SumVol(Chamber) = SumVol(Chamber) + VoA4
    Up(Chamber) = Up(Chamber) + 1
End If

```

C\*\*\*\*\* Cold Chamber 4 \*\*\*\*\*

```

Chamber = 11

If (VoC4 .GT. VoC4o) Then
    If (Up(Chamber) .GT. 0) Then
        MVC4(MVCount(Chamber)) = SumVol(Chamber) /
1         (Up(Chamber) + Down(Chamber))
        sum = 0.
        Do j = 1 , 20
            sum = MVC4(j) / 20. + sum
        End DO
        MVC4(21) = (sum - MVC4(21)) * Damp + sum
        MVCount(Chamber) = MVCount(Chamber) + 1
        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1
    SumVol(Chamber) = SumVol(Chamber) + VoC4
Else
    SumVol(Chamber) = SumVol(Chamber) + VoC4
    Up(Chamber) = Up(Chamber) + 1
End If

```

C\*\*\*\*\* Bounce Chamber 4 \*\*\*\*\*

```

Chamber = 12

If (VoB4 .GT. VoB4o) Then
    If (Up(Chamber) .GT. 0) Then
        MVB4(MVCount(Chamber)) = SumVol(Chamber) /
1         (Up(Chamber) + Down(Chamber))
        sum = 0.
        Do j = 1 , 20
            sum = MVB4(j) / 20. + sum
        End Do
        MVB4(21) = (sum - MVB4(21)) * Damp + sum
        MVCount(Chamber) = MVCount(Chamber) + 1
        If (MVCount(Chamber) .EQ. 21) Then
            MVCount(Chamber) = 1
        End If
        Up(Chamber) = 0
        Down(Chamber) = 0
        SumVol(Chamber) = 0.
    End If
    Down(Chamber) = Down(Chamber) + 1

```

```

SumVol(Chamber) = SumVol(Chamber) + VoB4
Else
SumVol(Chamber) = SumVol(Chamber) + VoB4
Up(Chamber) = Up(Chamber) + 1
End If

```

```

C*****
C  CALCULATION OF Power PER CYCLE
C*****

```

```

If ((VoH1 + VoA1) .GT. (VoH1o + VoA1o)) Then
  If (n .GT. 1) Then
    CycleNum = CycleNum+1
    PosArea = PVArea(PosCurl, m, PosArea)
    NegArea = PVArea(NegCurl, n, NegArea)
    Power1(p) = (NegArea-PosArea)/(t-Initial1)/10000000
    Initial1 = t
    m = 1
    n = 1
    p = p + 1
    If (p .EQ. (Powcycle + 1)) Then
      AvePow1 = 0.
      Do ii = 1 , Powcycle
        AvePow1 = Power1(ii)/Powcycle+AvePow1
      End Do
      p = 1
    End If
  End If
  PosCurl(1, m) = PA
  PosCurl(2, m) = VoH1 + VoA1
  m = m + 1
End If
If ((VoH1 + VoA1) .LT. (VoH1o + VoA1o)) Then
  NegCurl(1, N) = PA
  NegCurl(2, N) = VoH1o + VoA1o
  n = n + 1
End If

```

```

C  Engine 3 Power1

```

```

If ((VoH3 + VoA3) .GT. (VoH3o + VoA3o)) Then
  If (u .GT. 1) Then
    PosArea3 = PVArea(PosCur3, v, PosArea3)
    NegArea3 = PVArea(NegCur3, u, NegArea3)
    Power3(w) = (NegArea3-PosArea3)/(t-Initial3)/10000000
    Initial3 = t
    v = 1
    u = 1
    w = w + 1
    If (w .EQ. (Powcycle + 1)) Then
      AvePow3 = 0.
      Do ii = 1 , Powcycle
        AvePow3=Power3(ii)/Powcycle+AvePow3
      End Do
      w = 1
    End If
  End If
  PosCur3(1, v) = PC
  PosCur3(2, v) = VoH3 + VoA3
  v = v + 1
End If
If ((VoH3 + VoA3) .LT. (VoH3o + VoA3o)) Then
  NegCur3(1, u) = PC
  NegCur3(2, u) = VoH3o + VoA3o

```

```
      u = u + 1
End If
```

```
C*****
C  NEGATIVE HEIGHT CHECK
C*****
```

```
      If (LH1 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LB1 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LA2 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LC2 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LB2 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LA3 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LH3 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LB3 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LA4 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LC4 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LB4 .LT. 0.) Then
        neg = neg + 1
      End If
      If (LA1 .LT. 0.) Then
        neg = neg + 1
      End If
      If (neg .GE. 1) Then
        Engine = -10
        GoTo 1009
      End If
```

```
C*****
C  BLOWOUT CHECK
C*****
```

```
      If (LH1 .GT. LH) Then
        sup = sup + 1
      End If
      If (LB1 .GT. LB) Then
        sup = sup + 1
      End If
      If (LA2 .GT. LA) Then
        sup = sup + 1
      End If
      If (LC2 .GT. LC) Then
        sup = sup + 1
      End If
```

```

If (LB2 .GT. LB) Then
sup = sup + 1
End If
If (LA3 .GT. LA) Then
sup = sup + 1
End If
If (LH3 .GT. LH) Then
sup = sup + 1
End If
If (LB3 .GT. LB) Then
sup = sup + 1
End If
If (LA4 .GT. LA) Then
sup = sup + 1
End If
If (LC4 .GT. LC) Then
sup = sup + 1
End If
If (LB4 .GT. LB) Then
sup = sup + 1
End If
If (LA1 .GT. LA) Then
sup = sup + 1
End If
If (sup .GE. 1) Then
    Engine = -10
    GoTo 1009
End If

```

```

C*****
C REPEAT LOOP
C*****

```

```

GoTo 1005

```

```

C*****
C Quit computation and return results
C*****

```

```

1009 Engine = (AvePow1 + AvePow3) / 2.
VAR=VAR
Return
End

```

```

Function PVArea(Curve, num, Area)
Real Curve(2,*), Area
Integer jj, num

```

```

Area=0.
Do jj = 2 , num
Area = Area + Abs(((Curve(1, jj - 1) +
1 Curve(1, jj)) / 2) * (Curve(2, jj - 1) - Curve(2, jj)))
End Do
PVArea=Area

```

```

Return
End

```

```

C *****
C *****
C *****

```

C \*\*\*\*\*

```
      SUBROUTINE SA(N,X,MAX,RT,EPS,NS,NT,NEPS,MAXEVL,LB,UB,C,IPRINT,  
1         ISEED1,ISEED2,T,VM,XOPT,FOPT,NACC,NFCNEV,NOBDS,IER,  
2         FSTAR,XP,NACP)
```

C Version: 3.2

C Date: 1/22/94.

C Differences compared to Version 2.0:

C 1. If a trial is out of bounds, a point is randomly selected  
C from LB(i) to UB(i). Unlike in version 2.0, this trial is  
C evaluated and is counted in acceptances and rejections.  
C All corresponding documentation was changed as well.

C Differences compared to Version 3.0:

C 1. If  $VM(i) > (UB(i) - LB(i))$ , VM is set to  $UB(i) - LB(i)$ .  
C The idea is that if T is high relative to LB & UB, most  
C points will be accepted, causing VM to rise. But, in this  
C situation, VM has little meaning; particularly if VM is  
C larger than the acceptable region. Setting VM to this size  
C still allows all parts of the allowable region to be selected.

C Differences compared to Version 3.1:

C 1. Test made to see if the initial temperature is positive.  
C 2. WRITE statements prettied up.  
C 3. References to paper updated.

C Synopsis:

C This routine implements the continuous simulated annealing global  
C optimization algorithm described in Corana et al.'s article  
C "Minimizing Multimodal Functions of Continuous Variables with the  
C "Simulated Annealing" Algorithm" in the September 1987 (vol. 13,  
C no. 3, pp. 262-280) issue of the ACM Transactions on Mathematical  
C Software.

C A very quick (perhaps too quick) overview of SA:

C SA tries to find the global optimum of an N dimensional function.  
C It moves both up and downhill and as the optimization process  
C proceeds, it focuses on the most promising area.

C To start, it randomly chooses a trial point within the step length  
C VM (a vector of length N) of the user selected starting point. The  
C function is evaluated at this trial point and its value is compared  
C to its value at the initial point.

C In a maximization problem, all uphill moves are accepted and the  
C algorithm continues from that trial point. Downhill moves may be  
C accepted; the decision is made by the Metropolis criteria. It uses T  
C (temperature) and the size of the downhill move in a probabilistic  
C manner. The smaller T and the size of the downhill move are, the more  
C likely that move will be accepted. If the trial is accepted, the  
C algorithm moves on from that point. If it is rejected, another point  
C is chosen instead for a trial evaluation.

C Each element of VM periodically adjusted so that half of all  
C function evaluations in that direction are accepted.

C A fall in T is imposed upon the system with the RT variable by  
C  $T(i+1) = RT * T(i)$  where i is the ith iteration. Thus, as T declines,  
C downhill moves are less likely to be accepted and the percentage of  
C rejections rise. Given the scheme for the selection for VM, VM falls.  
C Thus, as T declines, VM falls and SA focuses upon the most promising  
C area for optimization.

C The importance of the parameter T:

C The parameter T is crucial in using SA successfully. It influences  
C VM, the step length over which the algorithm searches for optima. For  
C a small initial T, the step length may be too small; thus not enough  
C of the function might be evaluated to find the global optima. The

user



C should carefully examine VM in the intermediate output (set IPRINT =  
C 1) to make sure that VM is appropriate. The relationship between the  
C initial temperature and the resulting step length is function  
C dependent.

C To determine the starting temperature that is consistent with  
C optimizing a function, it is worthwhile to run a trial run first. Set  
C RT = 1.5 and T = 1.0. With RT > 1.0, the temperature increases and VM  
C rises as well. Then select the T that produces a large enough VM.

C For modifications to the algorithm and many details on its use,  
C (particularly for econometric applications) see Goffe, Ferrier  
C and Rogers, "Global Optimization of Statistical Functions with  
C Simulated Annealing," Journal of Econometrics, vol. 60, no. 1/2,  
C Jan./Feb. 1994, pp. 65-100.

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C As far as possible, the parameters here have the same name as in  
C the description of the algorithm on pp. 266-8 of Corana et al.

C In this description, SP is single precision, DP is double precision,  
C INT is integer, L is logical and (N) denotes an array of length n.  
C Thus, DP(N) denotes a double precision array of length n.

C Input Parameters:

C Note: The suggested values generally come from Corana et al. To  
C drastically reduce runtime, see Goffe et al., pp. 90-1 for  
C suggestions on choosing the appropriate RT and NT.  
C N - Number of variables in the function to be optimized. (INT)  
C X - The starting values for the variables of the function to be  
C optimized. (DP(N))  
C MAX - Denotes whether the function should be maximized or  
C minimized. A true value denotes maximization while a false  
C value denotes minimization. Intermediate output (see IPRINT)  
C takes this into account. (L)  
C RT - The temperature reduction factor. The value suggested by  
C Corana et al. is .85. See Goffe et al. for more advice. (DP)  
C EPS - Error tolerance for termination. If the final function  
C values from the last nept temperatures differ from the  
C corresponding value at the current temperature by less than  
C EPS and the final function value at the current temperature  
C differs from the current optimal function value by less than  
C EPS, execution terminates and IER = 0 is returned. (EP)  
C NS - Number of cycles. After NS\*N function evaluations, each  
C element of VM is adjusted so that approximately half of  
C all function evaluations are accepted. The suggested value  
C is 20. (INT)  
C NT - Number of iterations before temperature reduction. After  
C NT\*NS\*N function evaluations, temperature (T) is changed  
C by the factor RT. Value suggested by Corana et al. is  
C MAX(100, 5\*N). See Goffe et al. for further advice. (INT)  
C NEPS - Number of final function values used to decide upon termi-  
C nation. See EPS. Suggested value is 4. (INT)  
C MAXEVL - The maximum number of function evaluations. If it is  
C exceeded, IER = 1. (INT)  
C LB - The lower bound for the allowable solution variables. (DP(N))  
C UB - The upper bound for the allowable solution variables. (DP(N))  
C If the algorithm chooses X(I) .LT. LB(I) or X(I) .GT. UB(I),

C I = 1, N, a point is from inside is randomly selected. This  
 C This focuses the algorithm on the region inside UB and LB.  
 C Unless the user wishes to concentrate the search to a par-  
 C ticular region, UB and LB should be set to very large positive  
 C and negative values, respectively. Note that the starting  
 C vector X should be inside this region. Also note that LB and  
 C UB are fixed in position, while VM is centered on the last  
 C accepted trial set of variables that optimizes the function.  
 C C - Vector that controls the step length adjustment. The suggested  
 C value for all elements is 2.0. (DP(N))  
 C IPRINT - controls printing inside SA. (INT)  
 C Values: 0 - Nothing printed.  
 C 1 - Function value for the starting value and  
 C summary results before each temperature  
 C reduction. This includes the optimal  
 C function value found so far, the total  
 C number of moves (broken up into uphill,  
 C downhill, accepted and rejected), the  
 C number of out of bounds trials, the  
 C number of new optima found at this  
 C temperature, the current optimal X and  
 C the step length VM. Note that there are  
 C N\*NS\*NT function evaluations before each  
 C temperature reduction. Finally, notice is  
 C is also given upon achieving the termination  
 C criteria.  
 C 2 - Each new step length (VM), the current optimal  
 C X (XOPT) and the current trial X (X). This  
 C gives the user some idea about how far X  
 C strays from XOPT as well as how VM is adapting  
 C to the function.  
 C 3 - Each function evaluation, its acceptance or  
 C rejection and new optima. For many problems,  
 C this option will likely require a small tree  
 C if hard copy is used. This option is best  
 C used to learn about the algorithm. A small  
 C value for MAXEVL is thus recommended when  
 C using IPRINT = 3.  
 C Suggested value: 1  
 C Note: For a given value of IPRINT, the lower valued  
 C options (other than 0) are utilized.  
 C ISEED1 - The first seed for the random number generator RANMAR.  
 C 0 .LE. ISEED1 .LE. 31328. (INT)  
 C ISEED2 - The second seed for the random number generator RANMAR.  
 C 0 .LE. ISEED2 .LE. 30081. Different values for ISEED1  
 C and ISEED2 will lead to an entirely different sequence  
 C of trial points and decisions on downhill moves (when  
 C maximizing). See Goffe et al. on how this can be used  
 C to test the results of SA. (INT)  
 C  
 C Input/Output Parameters:  
 C T - On input, the initial temperature. See Goffe et al. for advice.  
 C On output, the final temperature. (DP)  
 C VM - The step length vector. On input it should encompass the  
 C region of interest given the starting value X. For point  
 C X(I), the next trial point is selected is from X(I) - VM(I)  
 C to X(I) + VM(I). Since VM is adjusted so that about half  
 C of all points are accepted, the input value is not very  
 C important (i.e. is the value is off, SA adjusts VM to the  
 C correct value). (DP(N))  
 C  
 C Output Parameters:  
 C XOPT - The variables that optimize the function. (DP(N))  
 C FOPT - The optimal value of the function. (DP)

C NACC - The number of accepted function evaluations. (INT)  
 C NFCNEV - The total number of function evaluations. In a minor  
 C point, note that the first evaluation is not used in the  
 C core of the algorithm; it simply initializes the  
 C algorithm. (INT).  
 C NOBDS - The total number of trial function evaluations that  
 C would have been out of bounds of LB and UB. Note that  
 C a trial point is randomly selected between LB and UB.  
 C (INT)  
 C IER - The error return number. (INT)  
 C Values: 0 - Normal return; termination criteria achieved.  
 C 1 - Number of function evaluations (NFCNEV) is  
 C greater than the maximum number (MAXEVL).  
 C 2 - The starting value (X) is not inside the  
 C bounds (LB and UB).  
 C 3 - The initial temperature is not positive.  
 C 99 - Should not be seen; only used internally.

C Work arrays that must be dimensioned in the calling routine:

```

C   RWK1 (DP(NEPS)) (FSTAR in SA)
C   RWK2 (DP(N))   (XP   "  ")
C   IWK  (INT(N))  (NACP  "  ")

```

C Required Functions (included):

C EXPREP - Replaces the function EXP to avoid under- and overflows.  
 C It may have to be modified for non-IBM-type main-  
 C frames. (DP)  
 C RMARIN - Initializes the random number generator RANMAR.  
 C RANMAR - The actual random number generator. Note that  
 C RMARIN must run first (SA does this). It produces uniform  
 C random numbers on [0,1]. These routines are from  
 C Usenet's comp.lang.fortran. For a reference, see  
 C "Toward a Universal Random Number Generator"  
 C by George Marsaglia and Arif Zaman, Florida State  
 C University Report: FSU-SCRI-87-50 (1987).  
 C It was later modified by F. James and published in  
 C "A Review of Pseudo-random Number Generators." For  
 C further information, contact stuart@ads.com. These  
 C routines are designed to be portable on any machine  
 C with a 24-bit or more mantissa. I have found it produces  
 C identical results on a IBM 3081 and a Cray Y-MP.

C Required Subroutines (included):

```

C PRTVEC - Prints vectors.
C PRT1 ... PRT10 - Prints intermediate output.
C FCN - Function to be optimized. The form is
C   SUBROUTINE FCN(N,X,F)
C   INTEGER N
C   DOUBLE PRECISION X(N), F
C   ...
C   function code with F = F(X)
C   ...
C   RETURN
C   END

```

C Note: This is the same form used in the multivariable  
 C minimization algorithms in the IMSL edition 10 library.

C Machine Specific Features:

- C 1. EXPREP may have to be modified if used on non-IBM type main-frames. Watch for under- and overflows on EXPREP.
- C 2. Some FORMAT statements use G25.18; this may be excessive for some machines.
- C 3. RMARIN and RANMAR are designed to be protable; they should not cause any problems.

```

C Type all external variables.
  DOUBLE PRECISION X(*), LB(*), UB(*), C(*), VM(*), FSTAR(*),
  1      KOPT(*), XP(*), T, EPS, RT, FOPT
  INTEGER NACP(*), N, NS, NT, NEPS, NACC, MAXEVL, IPRINT,
  1      NOBDS, IER, NFCNEV, ISEED1, ISEED2
  LOGICAL MAX

C Type all internal variables.
  DOUBLE PRECISION F, FP, P, PP, RATIO
  INTEGER NUP, NDOWN, NREJ, NNEW, LNOBDS, H, I, J, M
  LOGICAL QUIT

C Type all functions.
  DOUBLE PRECISION EXPREP
  REAL RANMAR

C Initialize the random number generator RANMAR.
  CALL RMARIN( ISEED1, ISEED2)

C Set initial values.
  NACC = 0
  NOBDS = 0
  NFCNEV = 0
  IER = 99

  DO 10, I = 1, N
    KOPT(I) = X(I)
    NACP(I) = 0
10  CONTINUE

  DO 20, I = 1, NEPS
    FSTAR(I) = 1.0D+20
20  CONTINUE

C If the initial temperature is not positive, notify the user and
C return to the calling routine.
  IF (T .LE. 0.0) THEN
    WRITE(7, '(/, ' THE INITIAL TEMPERATURE IS NOT POSITIVE. '
  1      /, ' RESET THE VARIABLE T. ' /)')
    IER = 3
    RETURN
  END IF

C If the initial value is out of bounds, notify the user and return
C to the calling routine.
  DO 30, I = 1, N
    IF ((X(I) .GT. UB(I)) .OR. (X(I) .LT. LB(I))) THEN
      CALL PRT1
      IER = 2
      RETURN
    END IF
30  CONTINUE

C Evaluate the function with input X and return value as F.
  CALL FCN(N,X,F)

C If the function is to be minimized, switch the sign of the function.
C Note that all intermediate and final output switches the sign back
C to eliminate any possible confusion for the user.
  IF(.NOT. MAX) F = -F
  NFCNEV = NFCNEV + 1
  FOPT = F
  FSTAR(1) = F

```

```

        IF(IPRINT .GE. 1) CALL PRT2(MAX,N,X,F)

C Start the main loop. Note that it terminates if (i) the algorithm
C succesfully optimizes the function or (ii) there are too many
C function evaluations (more than MAXEVL).
100  NUP = 0
      NREJ = 0
      NNEW = 0
      NDOWN = 0
      LNOBDS = 0

      DO 400, M = 1, NT
        DO 300, J = 1, NS
          DO 200, H = 1, N

C Generate XP, the trial value of X. Note use of VM to choose XP.
          DO 110, I = 1, N
            IF (I .EQ. H) THEN
              XP(I) = X(I) + (RANMAR()*2.- 1.) * VM(I)
            ELSE
              XP(I) = X(I)
            END IF

C If XP is out of bounds, select a point in bounds for the trial.
            IF((XP(I) .LT. LB(I)) .OR. (XP(I) .GT. UB(I))) THEN
              XP(I) = LB(I) + (UB(I) - LB(I))*RANMAR()
              LNOBDS = LNOBDS + 1
              NOBDS = NOBDS + 1
              IF(IPRINT .GE. 3) CALL PRT3(MAX,N,XP,X,FP,F)
            END IF
110      CONTINUE

C Evaluate the function with the trial point XP and return as FP.
          CALL FCN(N,XP,FP)
          IF(.NOT. MAX) FP = -FP
          NFCNEV = NFCNEV + 1
          IF(IPRINT .GE. 3) CALL PRT4(MAX,N,XP,X,FP,F)

C If too many function evaluations occur, terminate the algorithm.
          IF(NFCNEV .GE. MAXEVL) THEN
            CALL PRT5
            IF (.NOT. MAX) FOPT = -FOPT
            IER = 1
            RETURN
          END IF

C Accept the new point if the function value increases.
          IF(FP .GE. F) THEN
            IF(IPRINT .GE. 3) THEN
              WRITE(7,('( ' POINT ACCEPTED'))')
            END IF
            DO 120, I = 1, N
              X(I) = XP(I)
120      CONTINUE
            F = FP
            NACC = NACC + 1
            NACP(H) = NACP(H) + 1
            NUP = NUP + 1

C If greater than any other point, record as new optimum.
            IF (FP .GT. FOPT) THEN
              IF(IPRINT .GE. 3) THEN
                WRITE(7,('( ' NEW OPTIMUM'))')
              END IF

```

```

DO 130, I = 1, N
  XOPT(I) = XP(I)
130  CONTINUE
     FOPT = FP
     NNEW = NNEW + 1
     END IF

C If the point is lower, use the Metropolis criteria to decide on
C acceptance or rejection.
  ELSE
    P = EXPREP((FP - F)/T)
    PP = RANMAR()
    IF (PP .LT. P) THEN
      IF (IPRINT .GE. 3) CALL PRT6(MAX)
      DO 140, I = 1, N
        X(I) = XP(I)
140    CONTINUE
        F = FP
        NACC = NACC + 1
        NACP(H) = NACP(H) + 1
        NDOWN = NDOWN + 1
      ELSE
        NREJ = NREJ + 1
        IF (IPRINT .GE. 3) CALL PRT7(MAX)
      END IF
    END IF

200  CONTINUE
300  CONTINUE

C Adjust VM so that approximately half of all evaluations are accepted.
  DO 310, I = 1, N
    RATIO = DFLOAT(NACP(I)) /DFLOAT(NS)
    IF (RATIO .GT. .6) THEN
      VM(I) = VM(I)*(1. + C(I)*(RATIO - .6)/.4)
    ELSE IF (RATIO .LT. .4) THEN
      VM(I) = VM(I)/(1. + C(I)*((.4 - RATIO)/.4))
    END IF
    IF (VM(I) .GT. (UB(I)-LB(I))) THEN
      VM(I) = UB(I) - LB(I)
    END IF
310  CONTINUE

    IF (IPRINT .GE. 2) THEN
      CALL PRT8(N,VM,XOPT,X)
    END IF

    DO 320, I = 1, N
      NACP(I) = 0
320  CONTINUE

400  CONTINUE

    IF (IPRINT .GE. 1) THEN
      CALL PRT9(MAX,N,T,XOPT,VM,FOPT,NUP,NDOWN,NREJ,LNOBDS,NNEW)
    END IF

C Check termination criteria.
  QUIT = .FALSE.
  FSTAR(1) = F
  IF ((FOPT - FSTAR(1)) .LE. EPS) QUIT = .TRUE.
  DO 410, I = 1, NEPS
    IF (ABS(F - FSTAR(I)) .GT. EPS) QUIT = .FALSE.
410  CONTINUE

```

```

C Terminate SA if appropriate.
  IF (QUIT) THEN
    DO 420, I = 1, N
      X(I) = XOPT(I)
420  CONTINUE
      IER = 0
      IF (.NOT. MAX) FOPT = -FOPT
      IF(IPRINT .GE. 1) CALL PRT10
      RETURN
    END IF

C If termination criteria is not met, prepare for another loop.
  T = RT*T
  DO 430, I = NEPS, 2, -1
    FSTAR(I) = FSTAR(I-1)
430  CONTINUE
    F = FOPT
    DO 440, I = 1, N
      X(I) = XOPT(I)
440  CONTINUE

C Loop again.
  GO TO 100

  END

  FUNCTION EXPREP(RDUM)
C This function replaces exp to avoid under- and overflows and is
C designed for IBM 370 type machines. It may be necessary to modify
C it for other machines. Note that the maximum and minimum values of
C EXPREP are such that they has no effect on the algorithm.

  DOUBLE PRECISION RDUM, EXPREP

  IF (RDUM .GT. 174.) THEN
    EXPREP = 3.69D+75
  ELSE IF (RDUM .LT. -180.) THEN
    EXPREP = 0.0
  ELSE
    EXPREP = EXP(RDUM)
  END IF

  RETURN
  END

  subroutine RMARIN(IJ,KL)
C This subroutine and the next function generate random numbers. See
C the comments for SA for more information. The only changes from the
C original code is that (1) the test to make sure that RMARIN runs first
C was taken out since SA assures that this is done (this test didn't
C compile under IBM's VS Fortran) and (2) typing ivec as integer was
C taken out since ivec isn't used. With these exceptions, all following
C lines are original.

C This is the initialization routine for the random number generator
C RANMAR()
C NOTE: The seed variables can have values between:    0 <= IJ <= 31328
C                                                    0 <= KL <= 30081
C
  real U(97), C, CD, CM
  integer I97, J97
  common /raset1/ U, C, CD, CM, I97, J97
  if( IJ .lt. 0 .or. IJ .gt. 31328 .or.
*   KL .lt. 0 .or. KL .gt. 30081 ) then

```

```

    print '(A)', ' The first random number seed must have a value
*between 0 and 31328'
    print '(A)', ' The second seed must have a value between 0 and
*30081'

```

```

        stop
    endif
    i = mod(IJ/177, 177) + 2
    j = mod(IJ      , 177) + 2
    k = mod(KL/169, 178) + 1
    l = mod(KL,    169)
    do 2 ii = 1, 97
        s = 0.0
        t = 0.5
        do 3 jj = 1, 24
            m = mod(mod(i*j, 179)*k, 179)
            i = j
            j = k
            k = m
            l = mod(53*l+1, 169)
            if (mod(l*m, 64) .ge. 32) then
                s = s + t
            endif
        enddo
        t = 0.5 * t
    3    continue
    U(ii) = s
2    continue
    C = 362436.0 / 16777216.0
    CD = 7654321.0 / 16777216.0
    CM = 16777213.0 / 16777216.0
    I97 = 97
    J97 = 33
    return
end

```

```

function ranmar()
real U(97), C, CD, CM
integer I97, J97
common /raset1/ U, C, CD, CM, I97, J97
uni = U(I97) - U(J97)
if( uni .lt. 0.0 ) uni = uni + 1.0
U(I97) = uni
I97 = I97 - 1
if(I97 .eq. 0) I97 = 97
J97 = J97 - 1
if(J97 .eq. 0) J97 = 97
C = C - CD
if( C .lt. 0.0 ) C = C + CM
uni = uni - C
if( uni .lt. 0.0 ) uni = uni + 1.0
RANMAR = uni
return
END

```

#### SUBROUTINE PRT1

C This subroutine prints intermediate output, as does PRT2 through  
C PRT10. Note that if SA is minimizing the function, the sign of the  
C function value and the directions (up/down) are reversed in all  
C output to correspond with the actual function optimization. This  
C correction is because SA was written to maximize functions and  
C it minimizes by maximizing the negative a function.

```

    WRITE(7, '(/, '' THE STARTING VALUE (X) IS OUTSIDE THE BOUNDS ''
1      /, '' (LB AND UB). EXECUTION TERMINATED WITHOUT ANY''
2      /, '' OPTIMIZATION. RESPECIFY X, UB OR LB SO THAT ''

```



```
3          /,' ' LB(I) .LT. X(I) .LT. UB(I), I = 1, N. ' /')
```

```
RETURN  
END
```

```
SUBROUTINE PRT2 (MAX,N,X,F)
```

```
DOUBLE PRECISION X(*), F  
INTEGER N  
LOGICAL MAX
```

```
WRITE (7, '( ' ' ' )')  
CALL PRTVEC(X,N, 'INITIAL X')  
IF (MAX) THEN  
  WRITE (7, '( ' INITIAL F: ' ',/, G25.18)') F  
ELSE  
  WRITE (7, '( ' INITIAL F: ' ',/, G25.18)') -F  
END IF
```

```
RETURN  
END
```

```
SUBROUTINE PRT3 (MAX,N,XP,X,FP,F)
```

```
DOUBLE PRECISION XP(*), X(*), FP, F  
INTEGER N  
LOGICAL MAX
```

```
WRITE (7, '( ' ' ' )')  
CALL PRTVEC(X,N, 'CURRENT X')  
IF (MAX) THEN  
  WRITE (7, '( ' CURRENT F: ' ',G25.18)') F  
ELSE  
  WRITE (7, '( ' CURRENT F: ' ',G25.18)') -F  
END IF  
CALL PRTVEC(XP,N, 'TRIAL X')  
WRITE (7, '( ' POINT REJECTED SINCE OUT OF BOUNDS ' )')  
FP=FP  
RETURN  
END
```

```
SUBROUTINE PRT4 (MAX,N,XP,X,FP,F)
```

```
DOUBLE PRECISION XP(*), X(*), FP, F  
INTEGER N  
LOGICAL MAX
```

```
WRITE (7, '( ' ' ' )')  
CALL PRTVEC(X,N, 'CURRENT X')  
IF (MAX) THEN  
  WRITE (7, '( ' CURRENT F: ' ',G25.18)') F  
  WRITE (*, '( ' CURRENT F: ' ',G25.18)') F  
  CALL PRTVEC(XP,N, 'TRIAL X')  
  WRITE (7, '( ' RESULTING F: ' ',G25.18)') FP  
  WRITE (*, '( ' RESULTING F: ' ',G25.18)') FP  
ELSE  
  WRITE (7, '( ' CURRENT F: ' ',G25.18)') -F  
  WRITE (*, '( ' CURRENT F: ' ',G25.18)') -F  
  CALL PRTVEC(XP,N, 'TRIAL X')  
  WRITE (7, '( ' RESULTING F: ' ',G25.18)') -FP  
  WRITE (*, '( ' RESULTING F: ' ',G25.18)') -FP  
END IF
```

```
RETURN
```

```

END

SUBROUTINE PRT5

WRITE(7, '(/, '' TOO MANY FUNCTION EVALUATIONS; CONSIDER ''
1      /, '' INCREASING MAXEVL OR EPS, OR DECREASING ''
2      /, '' NT OR RT. THESE RESULTS ARE LIKELY TO BE ''
3      /, '' POOR.'', /)')

RETURN
END

SUBROUTINE PRT6 (MAX)

LOGICAL MAX

IF (MAX) THEN
  WRITE(7, '( '' THOUGH LOWER, POINT ACCEPTED'' )')
ELSE
  WRITE(7, '( '' THOUGH HIGHER, POINT ACCEPTED'' )')
END IF

RETURN
END

SUBROUTINE PRT7 (MAX)

LOGICAL MAX

IF (MAX) THEN
  WRITE(7, '( '' LOWER POINT REJECTED'' )')
ELSE
  WRITE(7, '( '' HIGHER POINT REJECTED'' )')
END IF

RETURN
END

SUBROUTINE PRT8 (N, VM, XOPT, X)

DOUBLE PRECISION VM(*), XOPT(*), X(*)
INTEGER N

WRITE(7, '(/,
1 '' INTERMEDIATE RESULTS AFTER STEP LENGTH ADJUSTMENT'', /)')
CALL PRTVEC(VM, N, 'NEW STEP LENGTH (VM)')
CALL PRTVEC(XOPT, N, 'CURRENT OPTIMAL X')
CALL PRTVEC(X, N, 'CURRENT X')
WRITE(7, '( '' '' )')

RETURN
END

SUBROUTINE PRT9 (MAX, N, T, XOPT, VM, FOPT, NUP, NDOWN, NREJ, LNOBDS, NNEW)

DOUBLE PRECISION XOPT(*), VM(*), T, FOPT
INTEGER N, NUP, NDOWN, NREJ, LNOBDS, NNEW, TOTMOV
LOGICAL MAX

TOTMOV = NUP + NDOWN + NREJ

WRITE(7, '(/,
1 '' INTERMEDIATE RESULTS BEFORE NEXT TEMPERATURE REDUCTION'', /)')
WRITE(7, '( '' CURRENT TEMPERATURE: '' ,G12.5)') T

```

```

IF (MAX) THEN
WRITE(7, '( ' ' MAX FUNCTION VALUE SO FAR: ' ',G25.18) ') FOPT
WRITE(7, '( ' ' TOTAL MOVES: ' ',I8) ') TOTMOV
WRITE(7, '( ' ' UPHILL: ' ',I8) ') NUP
WRITE(7, '( ' ' ACCEPTED DOWNHILL: ' ',I8) ') NDOWN
WRITE(7, '( ' ' REJECTED DOWNHILL: ' ',I8) ') NREJ
WRITE(7, '( ' ' OUT OF BOUNDS TRIALS: ' ',I8) ') LNOBDS
WRITE(7, '( ' ' NEW MAXIMA THIS TEMPERATURE: ' ',I8) ') NNEW
ELSE
WRITE(7, '( ' ' MIN FUNCTION VALUE SO FAR: ' ',G25.18) ') -FOPT
WRITE(7, '( ' ' TOTAL MOVES: ' ',I8) ') TOTMOV
WRITE(7, '( ' ' DOWNHILL: ' ',I8) ') NUP
WRITE(7, '( ' ' ACCEPTED UPHILL: ' ',I8) ') NDOWN
WRITE(7, '( ' ' REJECTED UPHILL: ' ',I8) ') NREJ
WRITE(7, '( ' ' TRIALS OUT OF BOUNDS: ' ',I8) ') LNOBDS
WRITE(7, '( ' ' NEW MINIMA THIS TEMPERATURE: ' ',I8) ') NNEW
END IF
CALL PRTVEC(XOPT,N,'CURRENT OPTIMAL X')
CALL PRTVEC(VM,N,'STEP LENGTH (VM)')
WRITE(7, '( ' ' ' ' ' ' ')

RETURN
END

SUBROUTINE PRT10

WRITE(7, '( /, ' ' SA ACHIEVED TERMINATION CRITERIA. IER = 0. ' ', /) ')

RETURN
END

```

```

SUBROUTINE PRTVEC(VECTOR,NCOLS,NAME)
C This subroutine prints the double precision vector named VECTOR.
C Elements 1 thru NCOLS will be printed. NAME is a character variable
C that describes VECTOR. Note that if NAME is given in the call to
C PRTVEC, it must be enclosed in quotes. If there are more than 10
C elements in VECTOR, 10 elements will be printed on each line.

```

```

INTEGER NCOLS
DOUBLE PRECISION VECTOR(NCOLS)
CHARACTER *(*) NAME

WRITE(7,1001) NAME

IF (NCOLS .GT. 10) THEN
LINES = INT(NCOLS/10.)

DO 100, I = 1, LINES
LL = 10*(I - 1)
WRITE(7,1000) (VECTOR(J),J = 1+LL, 10+LL)
100 CONTINUE

WRITE(7,1000) (VECTOR(J),J = 11+LL, NCOLS)
ELSE
WRITE(7,1000) (VECTOR(J),J = 1, NCOLS)
END IF

1000 FORMAT( 10(G12.5,1X))
1001 FORMAT(/,25X,A)

RETURN
END

```