Energy Savings Through Effective Interstage Pipe Design of Centrifugal Compressor Stages

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Background

Customer requirements involve complex custom piping

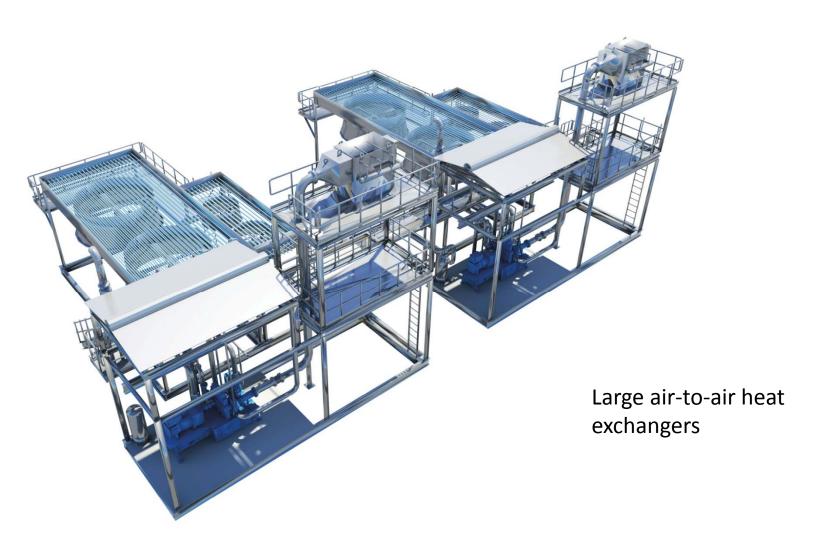




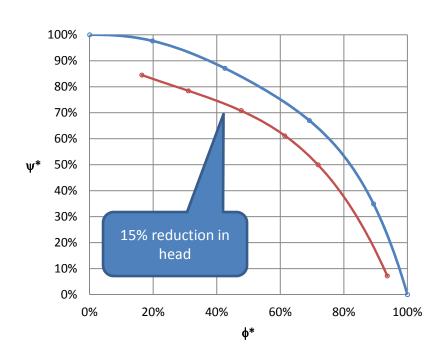
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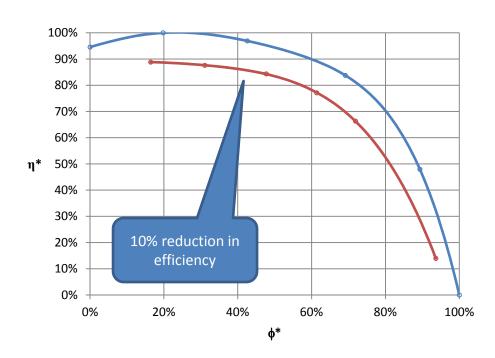


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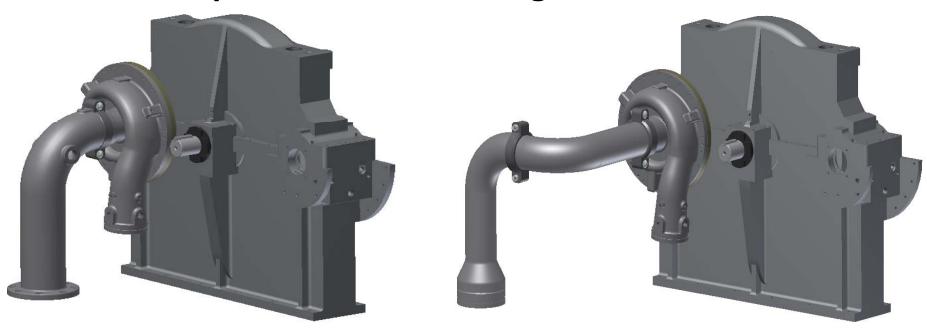


 One unit, using an existing aero design had radical drop in performance in the as-built form

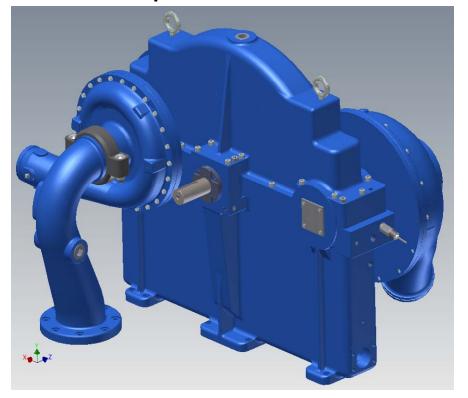




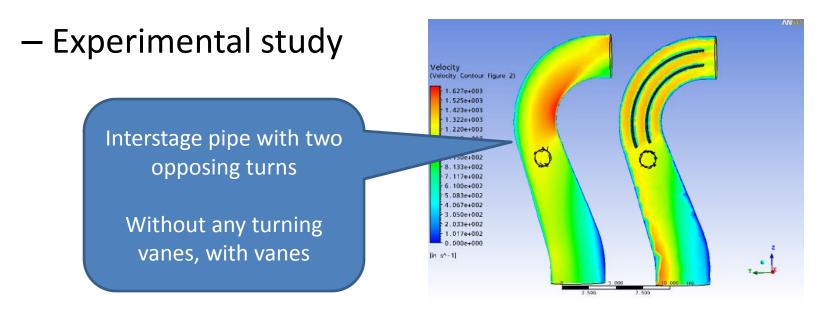
- The variable in the two units is the interstage piping
 - Pipe leading up to stage has multiple bends
 - Potential for non-uniform flow
 - Same impeller, diffuser, casing, and instrumentation



- A smaller, more cost-effective unit was chosen as a test subject for the study
 - Suspected candidate based on the visible geometry
 - Smaller, easier to work with components
 - Less expensive testing



- Embarked on an extensive study of the effect of vanes in elbows
 - CFD Analysis of pipe with and without turning vanes



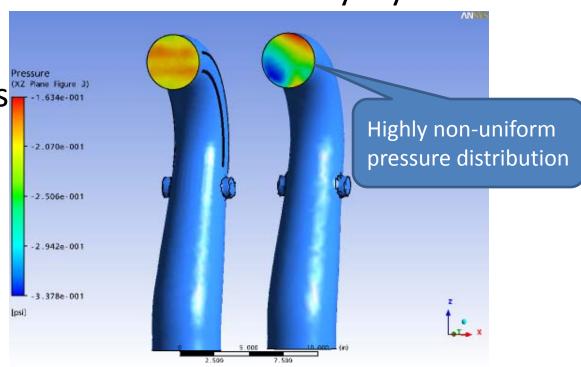
Results - Computational

CFD Analysis

Tetrahedral mesh with inflated boundary layers

- CFX version 14.0

- 100,000 elements



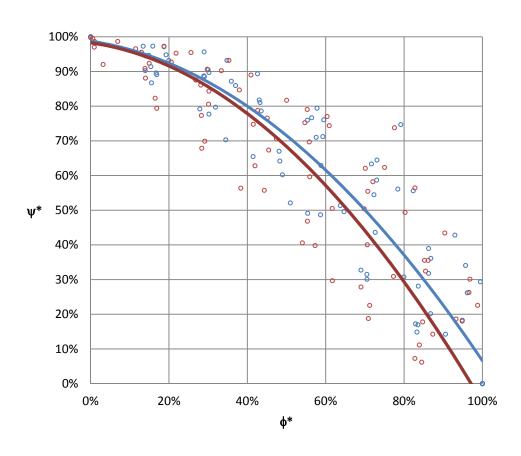
Results – Computational

 CFD Analysis 1.445e+003 1.083e+003 7.223e+002 3.611e+002 Corresponding non-uniform velocity Velocity (Vector 1 Figure 6) distribution 1.678e+003 Significant swirl [in s^-1]

Results - Experimental

- CFD results show directionally what to expect, but do not provide specifics
 - How much head recovery and efficiency improvement can we gain?
 - Experiments used a 700 (nominal) cfm stage,
 4 different profiles, 5 different impeller diameters

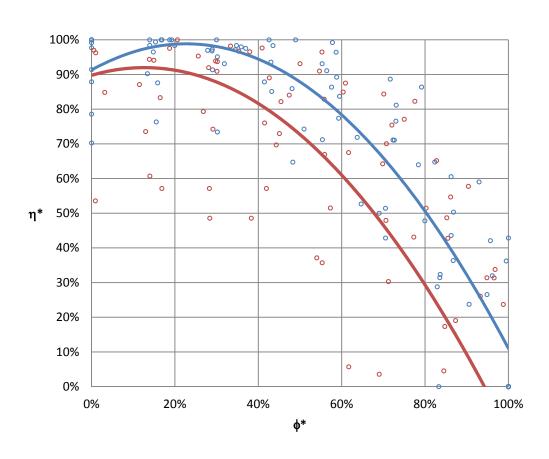
Results – Experimental



Head recovery with vaned pipe is a few points:

About 2-5% near typical design point

Results – Experimental



Efficiency recovery with vaned pipe significant:

5-10% better efficiency near typical design point

- Bigger effect at higher flow
 - To be expected
- Greater effect on efficiency vs. head
 - Indicates prevailing effect is poor pressure distribution (uneven density entering impeller)
 - Swirl is not so prevalent Euler: Head = △C,,U
 - Able to recover some performance losses from convoluted piping

- What does this mean to the manufacturer and customer?
 - It is increasingly more common for a power penalty to be added to submitted proposals in some markets
 - Anywhere from \$1,000 to \$5,000 per kW depending on the application, capacity, motor size, discharge pressure, etc.

- What does this mean to the manufacturer and customer (cont'd.)?
 - Look at a 3,500 scfm compressor with a 5% difference in adiabatic efficiency for two stages of a three stage compressor
 - Compressor #1 \$175,000 price
 - 850 HP (634 kW)
 - Compressor #2 \$200,000 price
 - 826 HP (616 kW)

- Using \$2,000/kW power penalty,
 Compressor #1 becomes \$211,000!
 - \$175,000 + (634 kW 616 kW) * \$2,000/kW

 The cheapest upfront cost is not necessarily the most economical solution in the long run