

A PROCESS FOR PRODUCING  
REFINED GUAR SPLITS

A Thesis

by

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## ABSTRACT

Guar (*Cyamopsis tetragonoloba*) is a warm-season, annual, leguminous crop that was introduced to the United States in 1903. Guar is harvested with a combine at which time seed pods and leaves are removed. Seeds are processed after harvesting to obtain refined guar splits. A primary use for guar is the production of guar (galactomannon) gum from the refined splits. Guar seed processing equipment primarily originates in India, where the crop has been grown for many years. The purpose of this research is to develop a scalable system for producing refined guar splits that will reach a minimum viscosity of 6500 cP at a 0.92% solids concentration and a white color. Two pilot scale process streams including heating, milling, sieving, and polishing were developed to produce refined splits.

The target viscosity of 6500 cP was achieved under certain conditions for both processes. A white color was not achieved, however predictive models were developed to determine the effects of experimental factors on color and viscosity response variables. Impurities in refined split samples greatly decrease viscosity of the final solution. Thoroughly cleaning and polishing splits is critical to achieving a consistently high viscosity.

Quality metrics vary by end user and affect process parameters. Increasing polishing time increased viscosity but with lower yields of polished splits. Increasing heating temperature had some desirable effects on viscosity and color, but extra costs will be associated with higher energy demands. Raw bean color appeared to affect the

color of the refined splits. Darker splits are not as desired by end users and are often purchased from processors at discounted rates. Gum content is not affected by darkening of the seed coat. However, darker color is not as desired by industries where aesthetics is a concern, such as food and pharmaceuticals. Darkening of seed coats can be reduced during the growing and reproducing of the crop. In addition, alternative polishing technologies can be considered to improve yield and efficiency.

## DEDICATION

I would like to dedicate this paper to the family of Dr. William Brock Faulkner. Throughout my time at Texas A&M, Dr. Faulkner was my greatest mentor. Without his guidance and support, I would not have the professional experience that I do today.. I received my first internship under Dr. Faulkner's recommendation. At the time, I was his student and he made a strong recommendation to the company on my behalf.. I spent the summer in Seguin, TX working for a machine design company where I was able to apply much of the knowledge that I gained while in school.

I later went on to work for Dr. Faulkner as a student worker. I worked on a variety of research projects ranging from air quality to material processing. As graduation neared, I was still unsure of what path I wanted to pursue in full time employment. I continued work with agricultural material processing into graduate school under Dr. Faulkner's guidance. Through this, I found my passion in process and design engineering.

Dr. Faulkner was a dedicated Christian who loved helping others and loved teaching. He was one of strongest and hard working men I have ever met. I am honored to have been given the chance to work under his leadership for so many years. As I move on to a professional career, I will strive to be a role model to young professionals as Dr. Faulkner was to me.

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I have had many great mentors, advisors, and friends throughout my life and college career. My family has always worked to instill good character and an unstoppable work ethic in me. While it was not a smooth road, they always stood behind me and pushed me to succeed. All of those long days in show barn and late nights working on Ag mechanics projects taught me how hard work pays off and that ribbons don't always make the award.

The Biological and Agricultural Engineering family has been important to me during my time at Texas A&M University. I would like to thank my committee chair, Dr. Faulkner, for believing in me and giving me the opportunity to pursue graduate school. I am forever grateful for the experience I gained through these many projects. Many of the opportunities I have been given are largely thanks to you and your desire to help students. From the first day in BAEN 365 to now, you have always been a great mentor and role model to me and many other students. I would also like to thank Dr. Castell-Perez, Dr. Riaz, Chris Mack, and the staff at the Food Protein Research and Development Center for their guidance and support throughout my thesis research.

In addition to my committee members, I would like to thank Ashlea Schroeder, Stormy Kretschmar, Dr. Lacey, Dr. Searcy, Richard Epting, Russel McGee, and Paulo Fortez Da Silva for their support and guidance throughout the various adventures during my college career and for always keeping me on the straight-and-narrow. Many of the life skills I have learned, particularly in time and project management, are in large thanks to these individuals. When I arrived to Texas A&M in the Fall of 2010, I never

imagined I would have the privilege to serve as the President of two student organizations. I certainly would not have been successful in these leadership roles without these advisors and mentors. To my classmates, friends, and colleagues, thank you for the continued support and for always keeping things interesting. From tractors to Mexico, I certainly could not have made it through this without your help!

And to my parents, without a good foundation, none of this would matter. Thank you for teaching me the importance of hard work, respecting others, and of course for your never ending support. I know I have a tendency to overload my plate, but you have always supported me and encouraged me to keep pushing forward. I know those long days in the show barn weren't always the most pleasant, but I think they have certainly paid off.

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## CHAPTER I

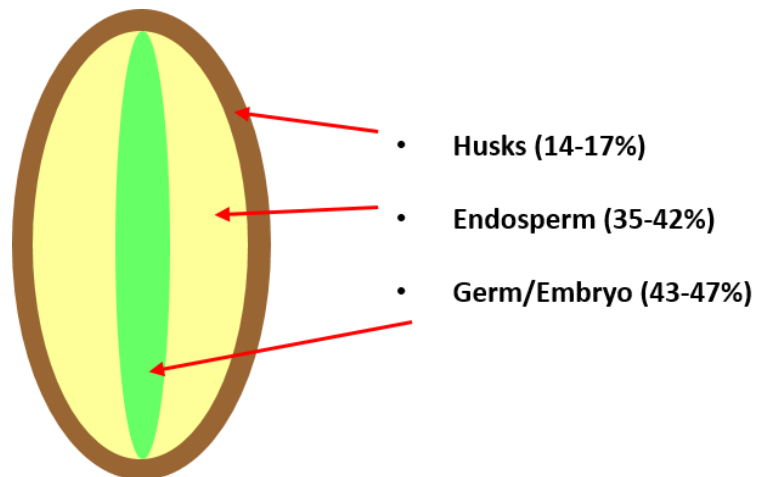
### INTRODUCTION AND LITERATURE REVIEW

Guar (*Cyamopsis tetragonoloba*) is a warm-season, annual, leguminous crop that was introduced to the United States in 1903. Commercial production of guar began in the 1950's and has been concentrated in the Texas panhandle and Oklahoma (Undersander et al., 2015). Guar is known for its drought tolerance, which makes it ideal for arid climates, and as a legume, is excellent in a crop rotation program since it improves soil properties (Undersander et al., 2015).

Guar (Figure 1) is harvested with a combine at which time the seed pods and leaves are removed. Seeds are processed after harvesting to obtain refined guar splits (polished endosperm). Guar seed is composed of three main components: seed coat, endosperm, and embryo (Figure 2). Guar (galactomannan) gum is produced from dehulled endosperm, which accounts for 35-42% of the seed weight (Goldstein et al., 1959).



**Figure 1. Guar seeds and pods.**



**Figure 2. Guar bean composition.**

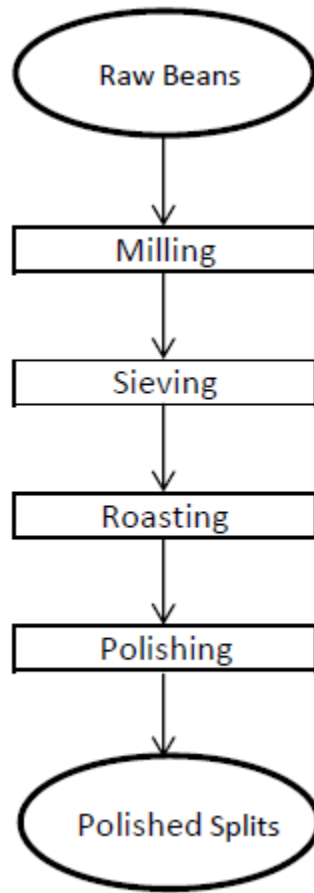
Gum is used in many industries, including food production, pharmaceuticals, and drilling. Chudzikowski (1971) defines gum as all materials that can be dispersed in water to form more or less viscous solutions. It has ability to form hydrogen bonds with

water molecules, which gives it use as a thickener and a stabilizer. Guar gum is used in the production of toothpaste and shaving cream to which the gum imparts slip, or a shear thinning property. The slip allows extrusion from the container with limited force, and in the case of shaving cream, the slip reduces friction during shaving (Chudzikowski, 1971). Bolliger et al. (2000) reported that guar gum is functional at inhibiting recrystallization in ice cream production. Stabilization during temperature fluctuation is enhanced by the thickening of the unfrozen phase of ice cream. The commercial use of guar gum began with the use of hydraulic fracturing fluids. Guar gum serves as a thickening agent for the fracturing fluid which allows the fluid to carry sand into cracks and fractured rock (Mudgil et al., 2014). The shear thinning properties of guar gum reduce the energy needed to pump material into rock formations. When the gum slows down in the fractured rock, it becomes thick to hold the rock formations open. The hydrogen bonding characteristic of guar gum is useful as a water seal in explosives. Gum will seal holes or cracks in the explosives and keep moisture out and has become the primary gum agent in water based explosives (Mudgil et al., 2014).

Darker seeds are believed to be of a lower quality (less gum content), than that of lighter seeds. Higher quantities of extracted endosperm will give higher guar gum yields (Whistler and Hymowitz, 1979). However, studies have shown that darker seeds yield higher percentage endosperm by mass and gum content was not affected by darkening of seeds. Guar seed coat color ranges in color from dull white to black. Seed coat color is reported to be affected by environmental conditions during seed germination (Liu et al., 2007). A trend that can be seen among the variation of seed coat colors is a variation of

hardness. White seeds are ‘harder’ than darker beans, which tend to absorb water slowly and have a lower germination rate, which is a concern for growers and buyers (Liu et al., 2007).

Guar seed processing equipment primarily originates in India, where the crop has been grown for many years. Specifics of unit operations in the process of producing refined guar splits are maintained as trade secrets. The general process (Figure 3) is to split the beans using a size reduction milling machine, sieve by size, roast and polish the split seeds to obtain polished ‘splits’(Figure 4).



**Figure 3. General process flow for producing refined guar splits.**

The milling machine splits the beans and removes the embryo from the endosperm. Sieving separates material based on size after splitting. After sieving, the split beans are roasted and polished to remove the seed coat. Many agricultural products such as soybeans are roasted prior to dehulling to separate the husk from the endosperm because the beans shrink at a faster rate than the husk, thus gently separating the two components. Roasting soybeans at 71°C (160°F) makes hulls fragile and allows easy separation from the kernels, thus making the hulling process more efficient (Moran,

1964). Similarly, it was expected that heating guar would increase the efficiency of the polishing step.



**Figure 4. Refined guar splits.**

Techniques for polishing, or finishing, grains exist, but little information is available in the literature for polishing guar. Removing the husks from endosperm seems to be the challenging step in processing guar. Patents have been filed in India for the process of dehulling, or dehusking, endosperm. Vishwakarma et al. (2003) developed a process for pretreating raw beans in a chemical aqueous solution to assist in separating hull from endosperm. A machine developed by Vishwakarma et al. (2015) involves pretreatment of guar seeds in an aqueous solution. Unsplit guar seeds are fed into the machine, dehused, split, and germ is separated after splitting of the seeds. The machine uses two parallel horizontal disks. One disk is stationary and one is rotating.



Centrifugal force causes the seeds to “roll” outward rubbing the husks off. A burr mill is then used to split the beans. A pin mill is used to separate germ from polished splits. Air aspiration is also used to separate lightweight material from heavier materials. Little information is available in academic literature on processing raw guar to produce refined guar splits.

The objective of this experiment was to develop a pilot-scale process for producing refined guar splits that will reach a minimum viscosity of 6500 cP and a ‘white’ color with the intention to scaling up to a commercial-scale. Equipment was identified and tested to perform operations of the process, similar to that shown in Figure 3. Equipment settings were analyzed and recommendations will be made for a commercial-scale process.

CHAPTER II  
DEVELOPMENT OF A PILOT SCALE PROCESS FOR PRODUCING REFINED  
GUAR SPLITS

**Objective**

The objective of Phase I of this project was to develop a pilot-scale process and identify machines for unit operations to obtain polished splits from raw guar beans with the intent to scale to commercial production rates in Phase II. The general process is to split the beans using a size reduction milling machine, sieve by size, roast and polish the split seeds to obtain polished ‘splits.’ Specific equipment was tested and settings were established for pilot-scale equipment. The desired outcome was for polished splits to reach a minimum viscosity of 6,500 cP when dissolved in water at a 0.92% solids concentration according to the Rhodia UV-9.0 method. A process using a disk attrition mill to split raw guar beans, mechanical and pneumatic separation of the germ from endosperm, and polishing of the husk from the endosperm yielded polished splits that, based on the Rhodia UV-9.0 method, yielded a final solution having a viscosity of  $11,340 \pm 1,670$  cP (mean  $\pm$  95% confidence interval).

**Introduction**

Guar (*Cyamopsis tetragonoloba*) is a warm-season leguminous crop used to produce guar gum. Guar was introduced into the United States from India in 1903, and production has been primarily concentrated in southern Oklahoma and north Texas. The

endosperm of the guar seed consists largely of a polysaccharide of galactose and mannose (guar gum), which can be extracted from the endosperm and used in various applications, including food production and as a thickening agent for hydraulic fracturing fluids. The husk and germ are insoluble and reduce the viscosity of guar gum solutions if they remain with the endosperm after processing. The meal that remains after extraction of the gum contains approximately 35% protein and is highly digestible, thereby making a good animal feed product (Undersander et al., 2015). In this study, different processes were evaluated to split and polish guar beans to obtain dehusked splits. A disk attrition mill and a tangential abrasion disk dehuller (TADD) were tested as methods to split and polish the beans. The final products were tested for viscosity to determine if the products would meet required quality specifications.

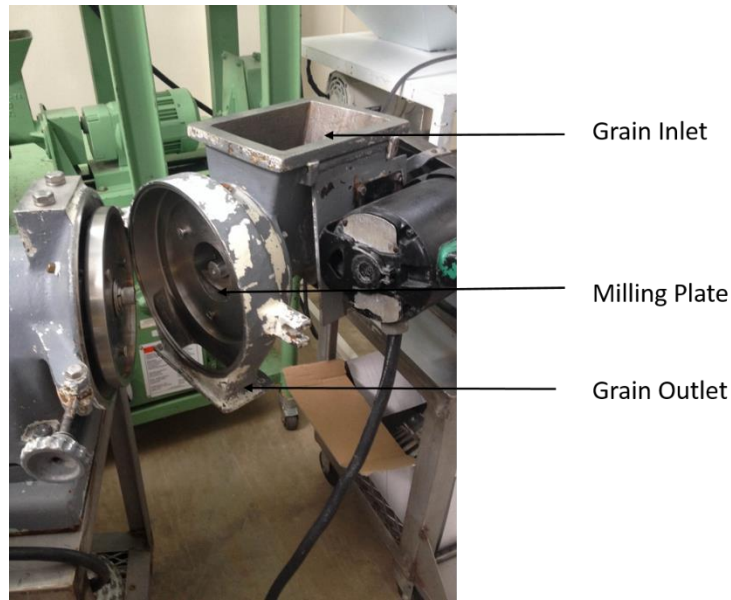
## **Methods**

### *Initial Aspiration*

Guar beans received from Alice, Texas; West Texas Guar; Knox City, Texas; and Bradley, Oklahoma, were aspirated prior to splitting and polishing to remove lighter foreign matter picked up during harvest, including sticks, leaves, seed pods, and dust. After aspirating, the guar beans underwent several experimental processes to remove the husks, split the beans, and separate the germ from the endosperm. The specific variety of guar from each supplier is unknown.

### *Disk Attrition Mill*

The first method that was tested was a Bauer disk attrition mill (Figure 5; Model 1482; The Bauer Bros. Co. Manufacturing; Springfield, OH). Disk attrition mills are common in the grain processing industry, and commercial-scale equipment is easily obtainable. Prior to milling, beans from West Texas Guar were heated to aid in loosening the endosperm from the husks. Beans were heated at 54°C (130°F) and 71°C (160°F) using a batch pan drying oven using stainless steel pans (Model 062; SGM Corporation; Philadelphia, PA), and a control sample with no heat was also tested. Four different mill plates were initially tested for the splitting process. Plate spacing was adjusted subjectively prior to processing the material to yield the maximum number of splits without pulverizing the endosperm. Bauer Mill plate 6945 (plate 2 from appendix A) and a more aggressive plate (plate 4 from appendix A) performed poorly at splitting the beans. Two different mill plates were chosen for further testing, including a Bauer Mill plate 6929 (plate 1 from Figure 6) and a less aggressive plate (plate 3 from Figure 6).



**Figure 5. Disk attrition mill.**



**Figure 6. Plate 3 (left) is a less aggressive plate while plate 1 (right) is a more aggressive plate.**

Samples were heated in 4.5 kg (10 lbs.) batches. The first trials conducted were with “plate 1.” Samples were heated at 54°C (130°F) for 5, 10, 15, and 20 minutes and milled. The next trials were heated at 71°C (160°F) for 10, 15, and 20 minute intervals.

Samples were not milled directly after being removed from the oven. The material was stored in plastic bags to maintain moisture content. Moisture contents were determined on approximately 680 g (1.5 lbs.) samples using an oven drying method (ASABE, 2012). Moisture content samples were heated at 105°C for 24 hours, or until mass remained constant to determine moisture content. Samples processed with “plate 1” were being over-milled, such that it appeared the plate was grinding the material rather than splitting the beans. After these observations were made “plate 3” was tested. Visual inspection of samples after milling with “plate 1” determined that the heating intervals chosen did not affect the milling process. For these trials, the samples were heated at 71°C (160°F) for 15, 30, 45, and 60 minute intervals. All treatments were analyzed with single replicates. After milling, the samples were processed with an air aspirator to separate foreign material from splits (Figure 7). Air aspirators are commonly used in commercial-scale processing systems. Several trials were conducted to determine the appropriate operational parameters for this process. It was determined that the material would need to be processed with the aspirator twice after milling. Samples were aspirated once to remove dust generated during the milling process (air velocity ~ 3.81 m/s (750 fpm)) and a second time to separate un-split beans (air velocity ~ 6.6 m/s (1300 fpm)). These parameters are not directly applicable to a commercial scale aspiration system, however the separation is representative of what should be expected in a commercial system.



**Figure 7. Aspirator.**

Viscosity analysis was performed on samples (3 replicates from each treatment) after the milling and aspirating process and results showed that viscosity was below the minimum requirement. The Bauer mill successfully split the beans, but further processing was required to polish the husks from the endosperm. Beans from Bradley, OK, were used to analyze a polishing process. The beans were processed using the disk attrition mill without heating prior to milling. The samples were aspirated as described above to remove foreign materials that will negatively affect viscosity. A bran finisher (Figure 8; Chopin Technologies, Villeneuve-la-Garenne Cedex, France) was used to polish beans that were split with “plate 3.” Raw splits were heated at 71°C (160°F) for 30 minutes to loosen the husks and were then processed in the bran finisher. A single replication of the process was performed in this experiment.

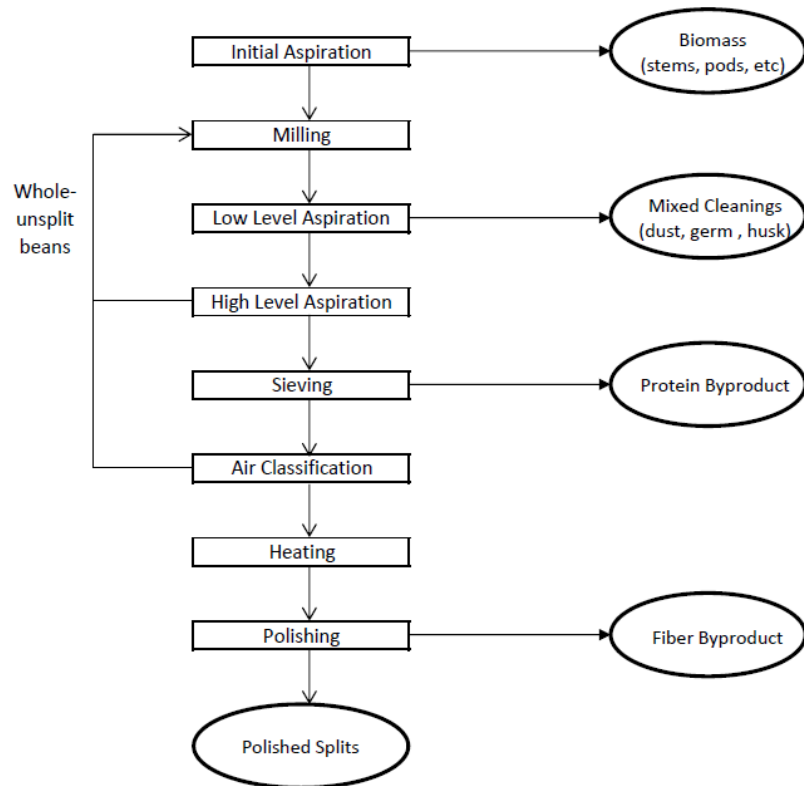
Based on previous viscosity observations, it was determined that further separation was needed to remove foreign materials from the samples after polishing.

Larger germ particles are very close in density to endosperm, thus the air aspiration machine was not effective at separating the germ from splits. Well-polished, clean splits were selected by hand from the final product for viscosity testing to determine if the described milling and polishing process would yield refined splits capable of meeting project objectives. In a commercial-scale facility, a mechanical separation process will be needed to separate guar splits from the germ before polishing. A vibratory conveyor was tested for this step, however the resulting separation was inadequate. Beans from Knox City, TX, were used to identify a separation process. Samples were milled, aspirated, and sent to Carrier Vibrating Equipment, Inc. where separation was achieved by sieving to remove the germ (a 3/16 inch mesh screen was used for the separation in phase 1) and air classification was used to remove un-split beans from guar splits. A process flow diagram for the tested process is shown in Figure 9.





**Figure 8. Chopin bran finisher.**



**Figure 9. Recommended process flow diagram for disk attrition mill process.**

### *Tangential Abrasion Disk Dehuller (TADD)*

The TADD mill was tested as an alternative to the disk attrition mill. As tested, the attrition mill did a good job of splitting the beans and separating the germ from the husked endosperm, but it did not remove the husks from the splits without additional processing (i.e., processing through the bran finisher). The TADD has eight abrasive disks that rotate inside a drum that holds the material (Figure 10). As the disks rotate, the beans are rubbed against the disks, husks are polished off, and the beans are split. TADD mills are very effective for polishing grains, but, to our knowledge, they are currently only commercially available at bench-scale. (Nutana Machine in Saskatchewan, Canada has previously produced a commercial-scale mill based on the same principle. They retain the plans for the mill and have expressed interest in selling the plans and/or manufacturing a commercial-scale mill for further testing).

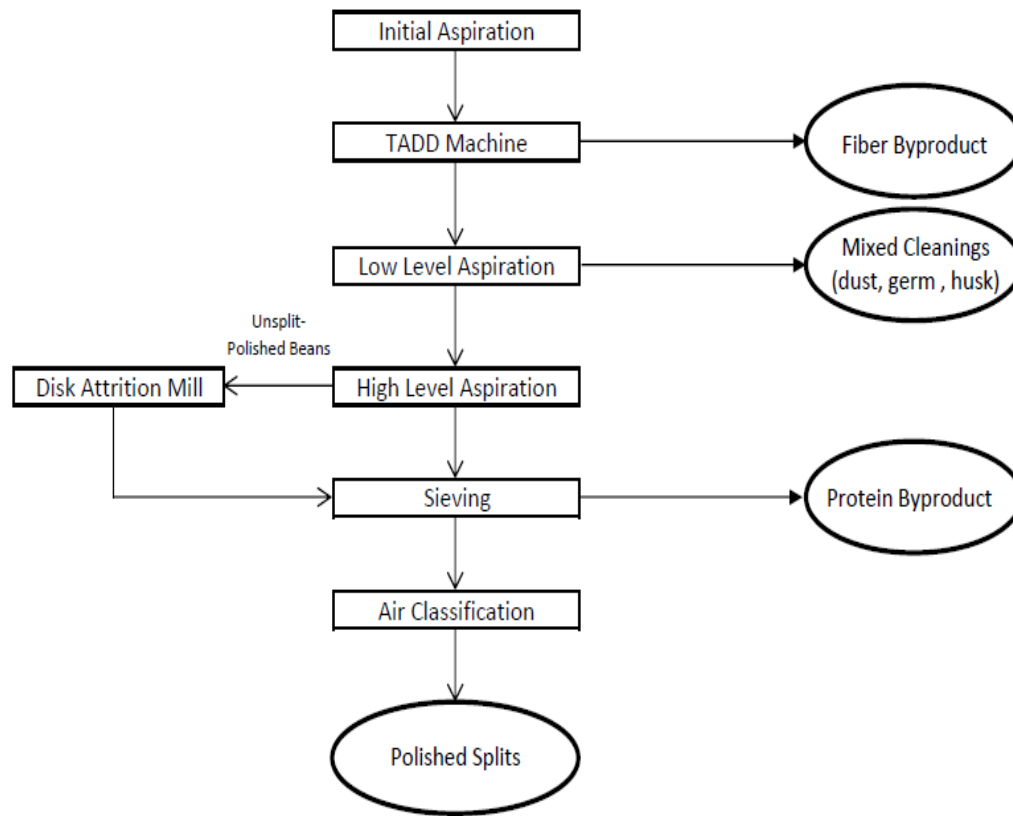


**Figure 10. Bench Scale Tangential Abrasive Disk Dehuller (TADD).**

Before processing on the TADD machine, five pound samples from West Texas Guar were heated at 82°C (180°F) for 60 minutes. Five pound samples were chosen due to the size limitation of the available TADD machine. Similar to the disk attrition mill process, the samples were not processed directly after heating. Preliminary tests were run to determine the degree of polishing needed in the TADD machine. Samples were initially processed in the machine for 3, 6, 9, 12, and 15 minutes, for a total of 5 trials (one replication per treatment). Samples were aspirated periodically to remove dust and fine materials, which degrade the performance of the mill as they buildup in the milling chamber. Visual inspection indicated that beans were not being adequately polished at shorter processing times. Samples from 12 and 15 minute trials were analyzed for viscosity. Both a bulk sample and a handpicked sample were analyzed from the beans that were processed for 15 minutes, but results from both were below the desired quality

(280 cP for the bulk sample and 3,590 cP for the handpicked sample with one replication from each).

After initial trials, samples were tested in which the effects of heating on processing time and viscosity were characterized. Samples from Bradley, OK, were used for the second set of tests to prevent further contamination of equipment from the dye used by West Texas Guar to mark their beans. These samples were processed in TADD until 30% and 40% mass losses were achieved. All samples were aspirated to remove whole beans that were not split in the processing (air velocity ~ 6.6 m/s (1300 fpm)). Figure 11 shows the process flow diagram for this process. The dehusked-but-unsplit beans were split using the disk attrition mill with “plate 3.” Viscosity was not conducted on these samples, tests were conducted to only evaluate if endosperm would be damaged in a splitting process after husks are removed.



**Figure 11. Recommended process flow diagram for TADD mill.**

### *Viscosity Testing*

The quality of polished splits was determined based on the Rhodia UV-9.0 method obtained from Solvay. This method is used to determine the viscosity of a water-guar gum mixture based on a 0.92% solids concentration. Samples were hydrated in approximately 500mL of water, and viscosity was measured using a Brookfield LV viscometer (LVDV-III, Brookfield Engineering Laboratories, Middleboro, MA). There were modifications to the water bath conditions and the shearing times to ensure complete hydration of the tested splits. To ensure the guar splits were fully hydrated and

dissolved, the splits were soaked for 30 minutes longer than specified in the hot water bath. Also, shearing times were increased by approximately 20 seconds to ensure that the components of the sample were uniformly distributed in the solution. Viscosity was measured after solution reached room temperature.

## Results and Discussion

### *Initial Aspiration Data*

Guar samples from four locations were provided by Southwest Agriculture.

Table 1 shows results of the initial aspiration. Useable yields of raw beans after initial cleaning varied substantially by source and have the potential to dramatically effect final yields of polished splits per unit of incoming product.

**Table 1. Initial aspiration results.**

<b>Sample</b>	<b>Initial Mass of Guar (lbs)</b>	<b>Mass of Cleaned Guar (lbs)</b>	<b>Trash (lbs)</b>	<b>% Mass Guar</b>
Alice, TX (variety 1)	28.3	23.5	4.85	82.9%
Alice, TX (variety 2)	58.0	55.0	3.04	94.8%
West TX Guar	45.6	44.8	0.76	98.3%
Bradley, OK	128	117	9.11	92.8%
Knox City (Sample 1)*	150.1	140.4	8.84	94.1%
Knox City (Sample 2)*	127.5	122.3	4.90	96.1%

\*Samples are from same batch

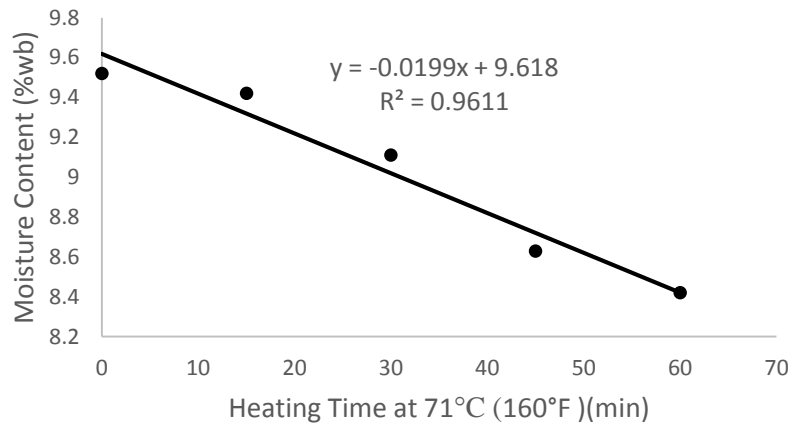
### *Disk Attrition Mill*

Two different plates and various heating conditions were tested in a disk-attrition-mill-based process. After milling, it was subjectively determined that a less aggressive plate (“plate 3”) was the best option for splitting the beans and removing the germ from the splits. The more aggressive mill setup (“plate 1”) pulverized rather than split the beans.

Moisture content decreased linearly with increased heating time (Figure 12), but no trends were observed between moisture content after heating and yield of splits and husks, indicating that heating prior to milling is unnecessary. After aspiration it was determined by visual inspection that the splits were not being polished enough with the milling process alone. A bran polisher was used to polish the husks from the heated splits. After polishing, three samples of polished splits (from Bradley, OK beans) were handpicked from the final product stream and analyzed for viscosity. The resulting viscosity was  $15,390 \pm 1,890$  cP (mean  $\pm$  95% confidence interval based on 3 replications), indicating that the process shown in Figure 9 is capable of meeting product quality specifications assuming the separations process adequately separates the germ and husk from the endosperm

Samples from Knox City were milled, aspirated, and sent to Carrier Vibrating Equipment, Inc. for separation of germ and un-split beans from the raw splits. Splits separated by Carrier were heated at 82°C (180°F) for 60 minutes followed by polishing. Three samples were picked and analyzed for viscosity using the Rhodia UV-9.0 method

and yielded an average viscosity of  $11,340 \pm 1,670$  cP (mean  $\pm$  95% confidence interval), exceeding project objectives of minimum viscosity of 6500 cP.



**Figure 12. Moisture content versus heating time.**

#### *Tangential Abrasion Disk Dehuller (TADD)*

The TADD was tested as a method to split the beans and polish the splits in one step. Tests were conducted with heated and unheated samples from Bradley, OK. Samples were processed until 30% and 40% of the raw bean mass was polished off. Heating the samples reduced the time required to reach the desired mass loss and the percentage of un-split beans. Samples were aspirated to remove the whole beans that were not split during the process.

Table 2 shows the processing time, percent whole beans from each sample, and handpicked viscosities (3 replications for viscosity). No statistically significant



differences were seen between viscosities from the four treatments, but additional replicates are needed to achieve a desired statistical power of 0.80. The processing time required to achieve the desired mass loss decreased with addition of a heating step prior to milling. Also, percent mass of beans that were un-split during polishing was decreased with the addition of a heating step.

This process was also capable of meeting product quality specifications (assuming the separations process adequately separates the germ and husk from the endosperm) and shows promise for improvement through optimization. The next stage in the development of this process would be mechanically separating the germ and husks from polished splits (using the process developed by Carrier) and then determining yields and product viscosities on the fully-mechanized process. Due to time and funding constraints, samples after aspirating were not able to be sent to Carrier for the separation step.

**Table 2. Process data for TADD machine.**

<b>Treatment</b>	<b>Target Mass Loss (%)</b>	<b>Processing Time (min)</b>	<b>Mass Loss Achieved</b>	<b>Percent Mass of Unsplit Beans</b>	<b>Viscosity (cP)<sup>[a]</sup></b>
Heated	40%	15	38.4%	10.5%	19,630 ± 3850
	30%	12	30.0%	12.7%	19,380 ± 2660
Unheated	40%	28	40.1%	21.4%	20,130 ± 905
	30%	20	30.9%	32.7%	17,730 ± 1350

[a] Mean ± 95% confidence interval

## **Conclusion**

The two processes explored both yielded polished guar splits which exceeded the required quality specifications. Viscosity results from the TADD exceeded project objectives when analyzing handpicked samples. Heated and unheated samples reached viscosities of  $19,630 \pm 3850$  and  $20,130 \pm 905$  cP, respectively. Although the results from the TADD are promising, commercial-scale equipment is not readily available. All of the equipment required for processing guar using the disk attrition mill is commercially available, and the final quality of the polished splits exceeded the project objectives when processing beans from Knox City. Viscosity of handpicked samples were  $15,390 \pm 1,890$  cP and viscosities for samples are mechanized separation were  $11,340 \pm 1,670$  cP (mean  $\pm$  95% confidence interval). Thus, the process described using the disk attrition mill (Figure 9) is recommended for the initial scale up. Optimization of the commercial-scale equipment (in particular heating and polishing processes) is also recommended to ensure efficient and quality controlled operation of the commercial-scale plant. Furthermore, additional plate designs for the disk attrition mill should be investigated.

## CHAPTER III

### A PROCESS FOR PRODUCING REFINED GUAR SPLITS

#### **Introduction**

Guar (*Cyamopsis tetragonoloba*) is a warm-season, annual, leguminous crop that was introduced to the United States in 1903. Commercial production of guar in the US began in the 1950's and has been concentrated in the Texas Panhandle and Oklahoma (Undersander et al., 2015). Guar is known for its drought tolerance, which makes it ideal for arid climates and, as a legume, is excellent for improving soil properties in a crop rotation program if seed are effectively inoculated (Undersander et al., 2015).

The primary use for guar is the production of galactomannan gum, or guar gum. Guar seed is composed of three main components: seed coat, endosperm, and embryo. Guar gum is produced from dehulled endosperm, which accounts for 35-42% of the seed weight (Goldstein et al., 1959). Guar gum is used as a thickening agent and a stabilizer in many industries, including food production, pharmaceuticals, and drilling operations (Mudgil et al., 2014). Guar processing equipment primarily originates in India, where most of the global guar production is centered. Methods for processing guar into refined guar splits are maintained as trade secrets, but the general process is to split the seeds using an attrition mill, sieve to separate by size, roast, and then polish to remove the husks. The husks and germ are insoluble and reduce the viscosity of guar gum solutions if they remain with the endosperm after processing. The meal that remains after

extraction of the endosperm contains approximately 35% protein and is highly digestible, thereby making a good animal feed product (Undersander et al., 2015).

Guar seed coats range in color from dull white to black. Darker seeds are believed to be of a lower quality (less gum content) than lighter seeds and are often sold at lower prices than lighter beans. However, studies have shown that darker seeds yield higher percentage endosperm by mass, and gum content is not affected by darkening of seeds (Liu et al., 2007). However, darker beans may not be as desirable for making light-colored foods (e.g., cream cheese or ice cream) or other products where color is an aesthetic concern.

The objective of this experiment was to design an experimental process to produce refined guar splits. Tests were conducted to analyze attrition mill settings for splitting the beans, heating intervals, and methods for polishing split beans. Refined splits were analyzed for quality by measuring viscosity and color of a 0.92% solids solution. Quality metrics desired by industry are not available in literature, however, based on feedback from several end users, the current experiments were designed to achieve a target viscosity of at least 6500 cP and a white color based on the three dimensional “CIE” system (Commission Internationale de l’Eclairage). Information regarding color parameters were not provided during initial development of the pilot-scale system.

## **Methods**

### *Processing*

Guar beans obtained from a commercial elevator were aspirated prior to heating, splitting, and polishing to remove lightweight foreign matter picked up during harvest, including sticks, leaves, seed pods, and dust. After aspirating, the guar beans were weighed into 2.27 kg (5 lbs.) samples to be heated. Samples were dried at 93°C (200°F), 121°C (250°F), or 149°C (300°F) for 10, 20, or 30 minute intervals with a batch drying oven (Model 31-350ER; Quincy Lab, INC.; Chicago, Ill). Higher heating temperatures were tested than those used previously to determine if higher heating temperatures would positively affect quality parameters.

It was predicted that heating time and temperature would be significant in the predictive models for the viscosity and processing time. Many agricultural products such as soybeans are roasted prior to dehulling to separate the husk from the endosperm because the beans shrink at a faster rate than the husk, thus gently separating the two components. Roasting soybeans at 71°C (160°F) makes hulls fragile and allows easy separation from the kernels, thus making the hulling process more efficient (Moran, 1964). Similarly, it was expected that heating guar would increase the efficiency of the polishing step.

After heating, the samples were processed with a Bauer Disk Attrition Mill (Model 1482; The Bauer Bros. Co. Manufacturing; Springfield, OH). A mildly abrasive plate (Bauer Mill plate 6908) was used for the splitting process (Figure 13). Plate

spacing was adjusted subjectively prior to processing the material to yield the maximum number of splits without pulverizing the endosperm.

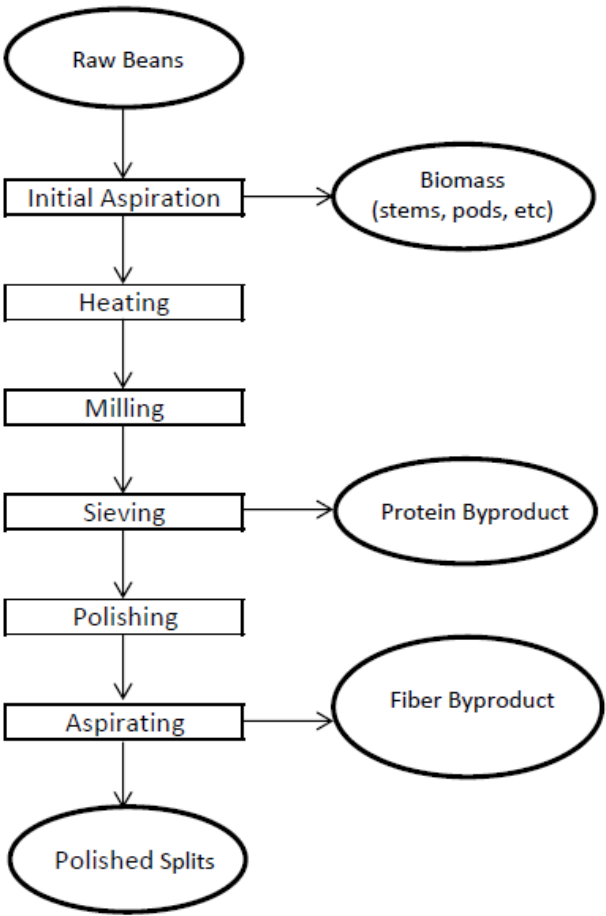


**Figure 13. Bauer mill plate 6908.**

After the splitting process, it was determined by visual observation that further processing was necessary to remove fines from the samples and polish the husks from the endosperm. Samples were sieved on a Ro-Tap mechanical sieve (Model RX-94; W.S. Tyler; Mento, OH) according to ASTM Standard C136M. Sieves were tested, and a number 12 sieve was selected for sieving fine particles from the split beans.

Sieved samples were polished using a tangential abrasive disk dehuller (TADD) until target mass losses of 20%, 30% or 40% were achieved. The TADD has six abrasive disks that rotate inside a drum that holds the material. As the disks rotate, the

beans are rubbed against the disks, and the husks are polished off. Samples were aspirated periodically to remove dust and fine materials, which degrade the performance of the mill as they buildup in the milling chamber. The process flow diagram for the tested process is shown in Figure 14. While the TADD is not readily available on a commercial-scale, the Chopin bran finisher discussed in chapter 2 for polishing is limited in scale and variability compared to a commercial bran finisher.



**Figure 14. Process flow for experimental procedure.**

### *Quality Measures*

Refined splits were added to approximately 150mL of water and placed in a water bath for thirty minutes. The solution was then sheared for one minute using a Waring blender (Model 31BL92, Dynamics Corporation of America, New Hartford, CT). After shearing, the solution was placed in an 85°C water bath (Type 89032-226, VWR International, West Chester, PA) for approximately one hour. After one hour, visual inspection was used to ensure that all solids were hydrated, and soaking times were adjusted if needed. Solutions were sheared for a second time, and water was added to reach a solids concentration of 0.92%. After water was added, the solutions were placed in a water bath at room temperature to cool and allow the solutions to stabilize. Viscosity was measured using a Brookfield LV viscometer (LVDV-III, Brookfield Engineering Laboratories, Middleboro, MA) after the solutions reached room temperature.

After viscosity tests were conducted, solution colors were analyzed with a spectrophotometer (Model LSXE; Hunter Associates Laboratory; Reston, Va.) to determine if differences in heating intervals and polishing affected color. The equipment was calibrated prior to analyzing samples each day using a calibration kit (Hunter Laboratory; Reston, VA). Approximately 150mL of solution was transferred to a glass sample cup which was then placed on the instrument for analysis. A light source illuminates a sample to be measured, and the light reflected by the object passes through a grating where the light is split into its spectral components. A diode array measures the wavelength of the components, and the instrument measures sample color against an



internal reference standard. Color is defined in a three dimensional space consisting of lightness, saturation, and hue. These parameters are mathematically converted to a three dimensional spherical space (the commission internationale de l'Eclairage or "CIE") that is easier to discuss. The CIE includes lightness ( $L^*$ ), red-green ( $a^*$ ), and blue-yellow ( $b^*$ ) parameters, which were used for statistical analysis. A pure white sample, which is most desirable for many food applications, would have values of  $L^*$ ,  $a^*$ , and  $b^*$  of "zero."

### *Experimental Design*

A two-level, three factorial response surface experimental design with three center points was used to develop predictive models relating heating time, heating temperature, and target mass loss during polishing, to polishing time, viscosity and color of the refined guar split solution (Table 3). Factorial designs are used in experiments where it is necessary to investigate the effects of factors on a response variable, which include main effects and interactions (Myers and Montgomery, 2002). A full-factorial response surface design was chosen to efficiently collect response data for the factors of this experiment.

Table 3. Factors of interest for experimental design.

Factor	Variable	Coded Variable		
		-1	0	1
Heating temp (°C)	A	93	121	149
Heating time (min)	B	10	20	30
Target Mass Loss (%)	C	20	30	40

Statistical analysis was conducted using Design Expert (v. 9.0.1.3, Stat-Ease Inc., Minneapolis Minn.) Power transformations were applied to the data according to the Box-Cox methodology (Myers and Montgomery, 2002), and analysis of variance (ANOVA) was used to determine which independent variables affected response models based on hierarchal practices using a significance level of  $\alpha=0.1$ .

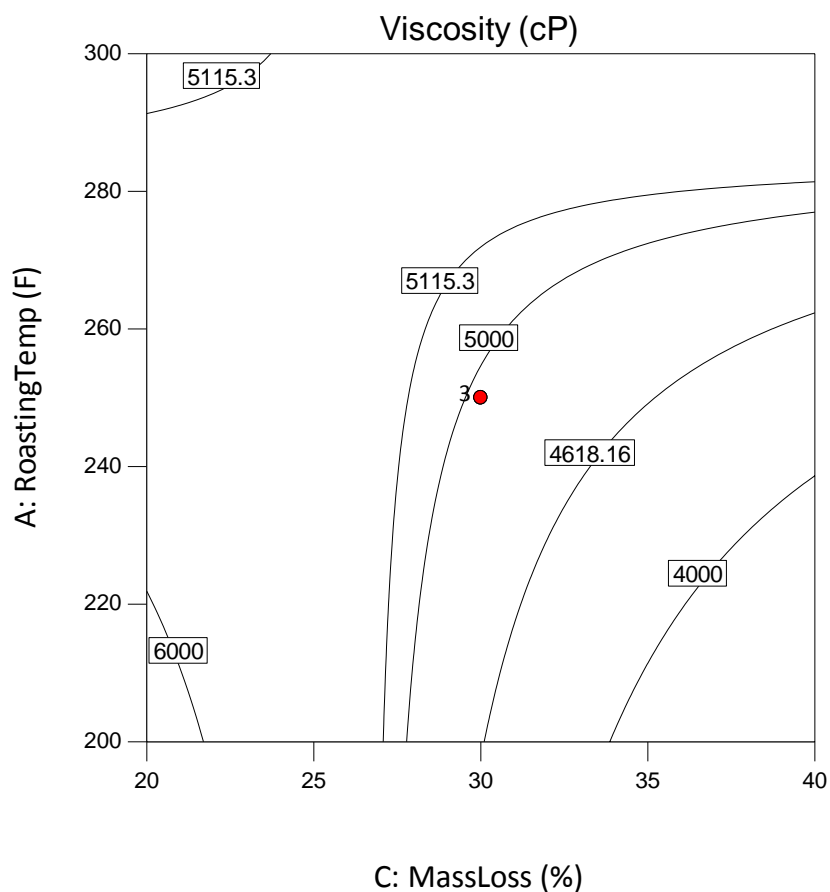
## **Results**

### *Viscosity*

The target viscosity of 6500 cP was not reached during initial trials, likely due to impurities (germ, husks, etc) in the samples which lower the viscosity of the guar gum solution. The mass yield of refined splits after processing was between 31% and 57%, and endosperm accounts for 35% to 42% of the bean mass, which also implies that there were impurities present. Prior to polishing, samples were sieved for two minutes to

remove fines from the samples. After polishing, an additional sieving step of one minute was added to remove more foreign materials and an increase in viscosity was seen for all samples. The target viscosity was reached for some of the samples. Mass yield of refined splits after additional sieving was between 27% and 55%.

The average viscosity for initial trials was  $2364.95 \pm 310.49$  cP. After additional sieving, maximum viscosity of 6508.2 cP was reached at 121 °C (250 °F), 20 min of heating time, and 30% mass loss. The average viscosity after additional sieving was  $4968.85 \pm 893.2$  cP. Interaction of heating temperature and target mass loss were found to significantly affect viscosity (Figure 15). The design point of 30% mass loss and 121 °C (250 °F) is indicated by the red dot on the figure. At higher heating temperatures, viscosity increased as target mass loss increased. At lower temperatures, additional polishing time reduced the viscosity. It is possible that the lower heating temperatures did not loosen the husks and endosperm was removed during polishing rather than husks.



**Figure 15. Effect of heating temperature and mass loss on viscosity.**

*Color*

Results for  $a^*$ ,  $b^*$ , and  $L^*$  after initial trials were 20.9, -0.57, and -0.46, respectively. After additional sieving, the interaction of heating temperature and target mass loss were found to significantly affect the lightness ( $L^*$ ) color parameter (Figure 16). At lower heating temperatures, increased polishing resulted in a “whiter” sample indicating that husk material was removed during polishing. At higher heating temperatures, increased mass loss resulted in a “less white” sample. Longer processing

time is required to remove more mass during polishing (Figure 17). Additional heat exposure in the polishing chamber likely darkened the samples.

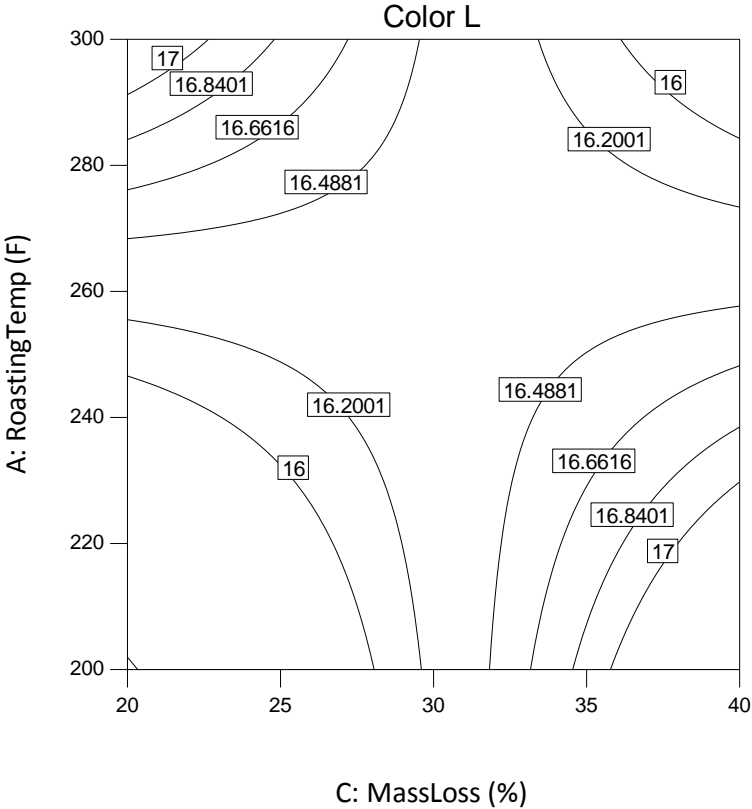
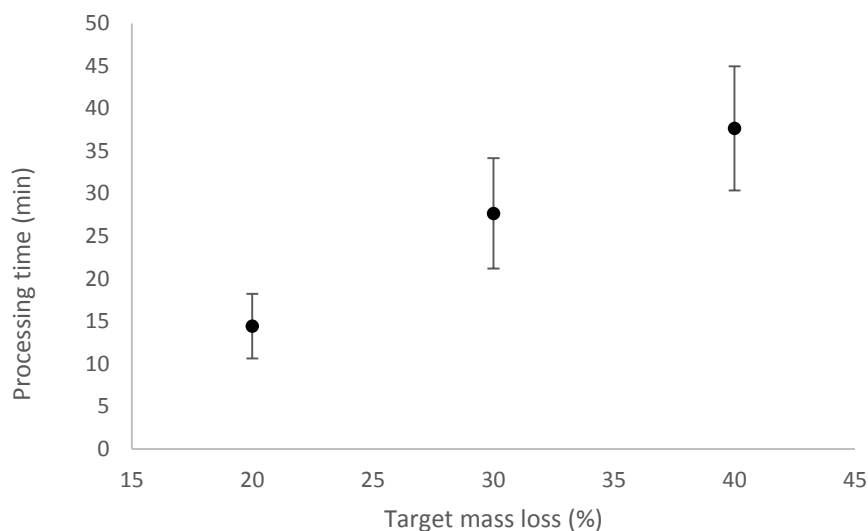
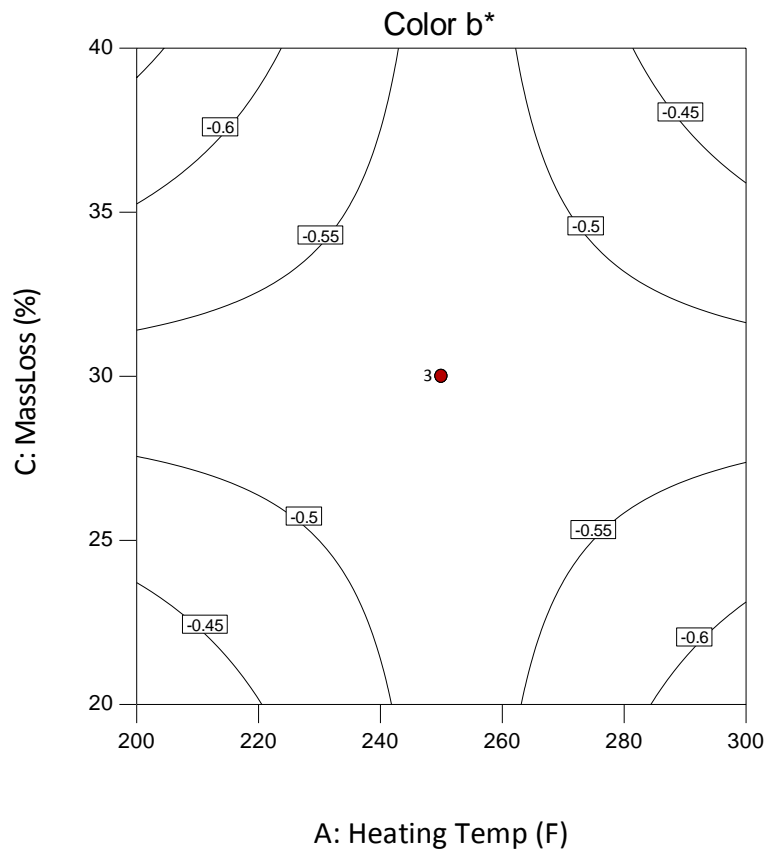


Figure 16. Effect of heating temperature and heating time on L\*.



**Figure 17. Processing time vs target mass loss during polishing.**

The interaction of heating temperature and target mass loss was significant to the model for  $b^*$  (Figure 18). The design point of 121 °C (250 °F) and 30% mass loss is shown on the figure. At higher heating temperatures, additional processing time increased the value of  $b^*$  toward zero, which results in a “whiter” sample. At lower temperatures, increased processing time decreased the value of  $b^*$ . It is expected that the husks are not as brittle at lower temperatures and endosperm is removed as well as husks during polishing, having a negative effect on  $b^*$ . There were no significant factors in the model for the color parameter  $a^*$ .



**Figure 18. Effect of heating temperature and heating time on b\*.**

Table 4 shows ANOVA results for response factors with significant factors for each response. No transforms were applied the response models. The resulting predictive models for the L\* and b\* color parameters were different than expected. It was expected that a higher target mass loss and increased heat exposure, more husks would be removed, which would result in “whiter” samples. Indication of the color becoming whiter would be an increase in L\* while a\* and b\* approach zero, but instead at lower heating temperature, L\* was positively affected by increased polishing time and

b\* was negatively affected by increased polishing time. L\* was negatively affected by increased polishing at higher temperatures and b\* was positively affected by increased polishing at higher heating temperatures.

**Table 4. ANOVA table for response factors.**

<b>Response Factor</b>	<b>Significant Factors</b>	<b>df</b>	<b>F-value</b>	<b>p-value</b>	<b>Mean Square Error</b>
Viscosity	A*C	1	4.9	0.0625	4.02E+06
Color L	A*C	1	7.4	0.0298	8.3
Color b	A*C	1	5.36	0.0537	0.12

Averages for L\*, a\*, and b\* were 16.4, -0.27 and -0.52, respectively. It is expected that increased heat exposure made the husks brittle and more were removed during polishing but the samples were darkened with increased heat exposure, causing the unexpected predictive models. The beans used for this experiment contained both dark and light beans. Processing samples with a uniform color would remove some variation from the experiment.

### **Summary and Conclusion**

The objective this experiment was to develop and analyze a pilot scale system to produce refined guar splits that will reach a minimum viscosity of 6500cP as well as a white color using the CIE system. The CIE includes lightness (L\*), red-green (a\*), and



blue-yellow ( $b^*$ ) parameters, which were used for statistical analysis and communication of results. Predictive models were developed to determine the effect of heating temperature, heating time, and mass loss during polishing on quality and processing parameters. Viscosity and color of a guar gum-water solution were measured and processing time during polishing was measured. This experiment used disk attrition, heating, polishing, and sieving to produce refined guar splits. Disk attrition was nearly 100% effective in splitting the beans and separating germ from split beans but not removing the husk, which negatively effects both viscosity and color. Polishing was achieved with a tangential abrasive disk dehuller.

It was expected that heating time, heating temperature, and degree of polishing would significantly affect solution viscosity and color, however heating time had no effect on the quality metrics. Viscosity was affected by heating temperature and target mass loss during polishing. At higher temperatures, increased polishing time positively affected viscosity. At lower temperatures, viscosity was negatively affected by increasing polishing time (and, therefore, mass removed). Additional polishing at lower temperatures likely removed endosperm in addition to husks, which resulted in lower viscosities. Color parameters had mixed results.  $L^*$  was negatively affected by increased polishing at lower temperatures. At higher temperatures,  $L^*$  was positively affected by additional polishing time.  $B^*$  was positively affected by increased polishing time at higher temperatures and negatively affected by increased polishing time at lower temperatures. It was expected that increased heat exposure would result in a whiter color, indicating that more husks was removed during the polishing step, but color had

mixed results. The samples used for this experiment contained both light and dark beans. Dark beans have a darker endosperm which could have caused the unexpected color results. Raw seed color, therefore, is expected to have a significant effect on the value of guar seed and the ability of processors to reach target colors. Viscosity was positively affected by increasing polishing intervals. Splits that were exposed to longer polishing resulted in higher viscosity, which indicates that more husks were removed during the polishing step, but this came at the expense of split yield.

The desired viscosity of 6500cP was reached during this experiment under certain conditions. Mass yields of refined splits indicated that there were impurities in the samples used for analyzing viscosity and color, which likely caused low viscosity results and unexpected color results. Impurities in a sample greatly affect the viscosity of guar gum solutions. Viscosity drastically decreases by any impurities that are in the sample. Thoroughly cleaning and polishing splits is critical to achieving a consistently high viscosity.

The process developed in this experiment is commercially scalable. Increasing polishing time increased viscosity but reduced mass yield. Increased heating temperature had some desirable effects on viscosity and color but additional heating will increase energy costs. Quality metrics from end users could be used to develop desirability functions for significant process parameters in order to determine the degree of polishing and heating intervals that should be used. Process parameters can be optimized to reduce processing costs and maximize yield based on desired quality.

## CHAPTER IV

### SUMMARY AND CONCLUSION

Quality metrics for guar gum desired by industry are not available in literature, however, based on feedback from several end users, the current experiments were designed to achieve a target viscosity of at least 6500 cP. Results from phase I showed that the target viscosity can be reached with the two designed processes. The first method that was tested was a disk attrition mill. Samples were split, heated, separated to remove foreign matter, and polished to remove husks. The second method that was tested was a tangential abrasive disk dehuller (TADD). Samples from both methods exceeded the project objectives when polished splits were handpicked. Bulk samples were also analyzed; however, foreign material (i.e. husks and embryo) in the samples lowered the solution viscosity. Additional cleaning was needed to remove more foreign materials and produce cleaner samples. Parameters of the heating and polishing processes were not optimized in this experiment.

The objective of the second experiment was to develop and analyze a pilot scale system to produce refined guar splits that will reach a minimum viscosity of 6500cP as well as a white color using the CIE system. The CIE includes lightness ( $L^*$ ), red-green ( $a^*$ ), and blue-yellow ( $b^*$ ) parameters, which were used for statistical analysis and communication of results. Predictive models were developed to determine the effect of heating temperature, heating time, and mass loss during polishing on quality and processing parameters. Viscosity and color of a guar gum-water solution were measured

and processing time during polishing was measured. The desired viscosity of 6500cP was reached during this experiment under certain conditions. Viscosity was affected by heating temperature and target mass loss during polishing. At higher temperatures, increased polishing time positively affected viscosity. At lower temperatures, viscosity was negatively affected by increasing polishing time. The average viscosity after was  $4968.85 \pm 893.2$  cP. Color parameters had mixed results.  $L^*$  was negatively affected by increased polishing at lower temperatures. At higher temperatures,  $L^*$  was positively affected by additional polishing time.  $B^*$  was positively affected by increased polishing time at higher temperatures and negatively affected by increased polishing time at lower temperatures. Averages for  $L^*$ ,  $a^*$ , and  $b^*$  were 16.4, -0.27 and -0.52, respectively. It was expected that increased heat exposure would result in a whiter color, indicating that more husks were removed during the polishing step, but color had mixed results. Analysis of variance (ANOVA) was used to determine which independent variables affected response models based on hierarchal practices using a significance level of  $\alpha=0.1$ .

Mass yields of refined spits indicated that there were impurities in the samples used for analyzing viscosity and color, which likely caused low viscosity results and unexpected color results. Impurities in a sample greatly affect the viscosity of guar gum solutions. Viscosity is drastically decreased by any impurities that are in the sample. Thoroughly cleaning and polishing splits is critical to achieving a consistently high viscosity. In phase I, handpicked samples and bulk samples from a mechanical separation process were analyzed for viscosity. These samples exceeded the project

requirements. In phase II, bulk samples were analyzed for viscosity. The separation technology used in phase I to separate germ and split beans was able to be used in phase II due to funding constraints from the project sponsor. Sieving was used in conjunction with air aspiration to remove contaminants, however some impurities were in the samples, which lowered the viscosity.

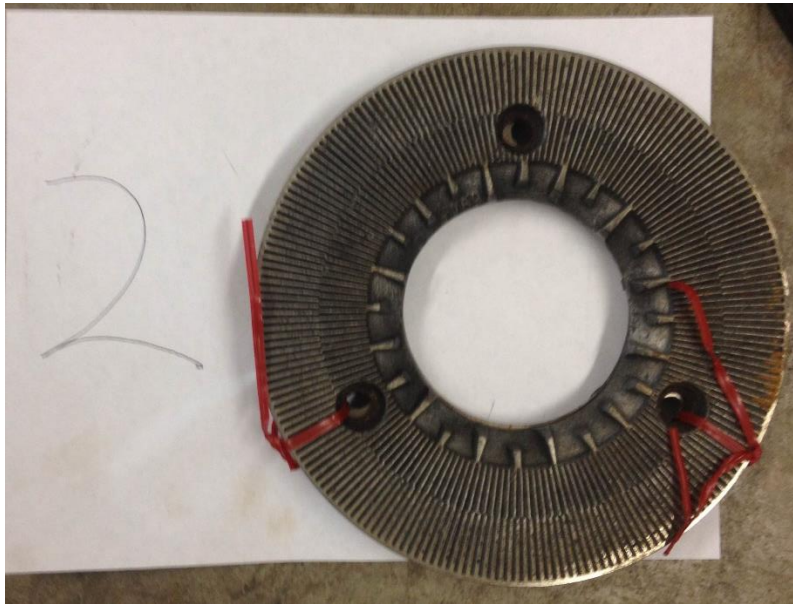
Increasing polishing time increased viscosity but reduced mass yield. Increased heating temperature had some desirable effects on viscosity and color but additional heating will increase energy costs. Quality metrics from end users should be obtained to determine the degree of polishing and heating intervals that should be used. Process parameters can be optimized to reduce processing costs and maximize yield based on desired quality. Darker splits are not as desired by end users and are often purchased at a discounted rate from processors. Viscosity is not affected by raw bean color, however darker splits from dark beans will reduce the value of refined splits.

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APPENDIX A

ADDITIONAL DISK ATTRITION MILL PLATES



**Figure 19. Bauer disk attrition mill plate 6945.**



**Figure 20. Bauer disk attrition mill "plate 4."**