# STATIC PRESSURE LOSS IN 12", 14", AND 16"

#### NON-METALLIC FLEXIBLE DUCT

A Thesis

by

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#### **ABSTRACT**

This study was conducted to determine the effects of compression on pressure drops in non-metallic flexible duct. Duct sizes of 12", 14" and 16" diameters were tested at a five different compression ratios (maximum stretch, 4%, 15%, 30% and 45%) following the draw through methodology in ASHRAE Standard 120 -1999 – Methods of Testing to Determine Flow Resistance of Air Ducts and Fittings. With the pressure drop data gathered, equations were developed to approximate the pressure loss at a given air flow rate for a given duct size. The data gathered showed general agreement with previous studies showing an increase in compression ratio leads to an increase in static pressure loss through the duct. It was determined that pressure losses for compression ratios greater than 4% were over four times greater than maximum stretched flexible duct of corresponding duct size. The increased static pressure losses can lead to decreased performance in HVAC systems. The findings of this study add to the existing ASHRAE and industry data for flexible duct with varying compression ratios.

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#### **CHAPTER I**

#### INTRODUCTION

As energy costs continue to rise, efficient usage of the HVAC system in commercial buildings offers a cost saving solution. Efficient usage of the system cannot be achieved, however, unless the system is installed properly. During the installation of the ductwork, contractors often use non-metallic flexible duct due to its ease of installation and relatively lower cost compared to rigid sheet metal ductwork. The non-metallic flexible duct allows an installing contractor to bend and compress the duct into whatever shape they need for a given area.

The enhanced flexibility of the flexible duct presents several problems to the efficiency of the whole building HVAC system. A significant problem can come from the unnecessary compressing of the flexible duct when it is installed. The Air Conditioning Contractors of America (ACCA) Manual D sets guidelines for the proper installation of non-metallic flexible duct. The ACCA guideline for installation of flexible duct calls for the duct to be fully extended along the straightest path possible. It is typical to observe installed flexible ductwork in commercial buildings that have compression ranging from 4% to 30% of the fully stretched length. The higher compression of the ductwork can lead to higher static pressure drop values. The higher static pressure losses increase the system's supply fan usage and the increase in the system's supply fan usage leads to higher energy bills for the consumer. In some cases, increased compression of the ductwork can lead to reduced comfort levels in rooms served by the compressed duct.

This study examines the effects of compression on the static pressure loss in 12", 14", and 16" diameter non-metallic flexible ducts. This study also intends to increase the design knowledge base for flexible duct installation and maintenance for commercial buildings. Proper knowledge of the effects of compression on static pressure loss will help designers and installers understand the negative effects compression can have on energy efficiency in buildings.

#### **CHAPTER II**

#### LITERATURE REVIEW

In preparation for this research project, it was necessary to review the literature related to this area of research to determine the existing level of the knowledge base for compression effects. To accomplish this, literature related to testing and research dealing with pressure measurements in ducts and duct systems was obtained and reviewed. In the review of this research, five sources were found which discussed material pertinent to the proposed project in the area of static pressure loss and nonmetallic flexible duct compression. The first source for static pressure loss and flexible duct was the Air Conditioning Contractors of America (ACCA) Manual D (ACCA 2009)<sup>4</sup>. This source contains calculations for flexible duct, but does not discuss compression. The second source, "Residential Ductwork and Plenum Box Bench Tests" from *IBACOS Burt Hill Project* (Kokayko et al. 1996)<sup>16</sup> reported the first data that took into account compression in flexible duct up to 10%. The third source was Abushakra et al.'s (2001, 2002, 2004)<sup>1,2,3</sup> laboratory study of pressure losses in residential air distribution systems for the Lawrence Berkeley National Laboratory Report as well as "Compression Effects on Pressure Loss in Flexible HVAC Ducts" in the *International* Journal of Heating, Ventilating, Air-Conditioning and Refrigeration Research. The efforts from these sources increased the previous flexible duct compression data up to 30%. The fourth source, "Static Pressure Loss in Nonmetallic Flexible Duct" is from ASHRAE Transactions, V. 113, from Weaver and Culp (2007)<sup>25</sup>, investigated similar compressions as Abushakra while increasing the compression data up to 45%. The fifth

source is from the ASHRAE Handbook of Fundamentals (2009)<sup>7</sup>. In the "Duct Design" chapter, methods to calculate pressure loss are provided along with a discussion on correction factors based upon percent compression of flexible duct.

ACCA Manual D (ACCA 2009)<sup>4</sup> gives the procedures for sizing complete duct systems. Manual D also contains static pressure loss charts for flexible duct. These charts do not include effects of compression. The source of the data used by ACCA was unknown and attempts to determine the origin of the data were unsuccessful. The rigid sheet metal duct data is taken from the American Society of Heating, Refrigerating, and Air Conditioning Engineers (ASHRAE) Handbook of Fundamentals Chapter 35-Duct Design (ASHRAE 2009)<sup>7</sup>.

Integrated Building and Construction Solutions (IBACOS) conducted research on flexible duct as part of the Burt Hill Project (Kokayko et al. 1996)<sup>16</sup>. This research covered the static pressure losses in straight run flexible duct, duct board triangle plenum boxes, and flexible duct elbows. These tests were performed on 6" 8", 10", and 12" diameter ducts. The straight run flexible duct tests were done using maximum stretched and 10% compression configurations in lengths of 25 feet on a flat surface. This testing showed the values of the 10% compression were 35% to 40% higher than that of the maximum stretched values. Triangular plenum boxes were tested with inlet diameters of 6", 8" and 10" and outlet diameters between 6" and 10". These boxes were tested in three different sizes: small, medium, and large. A small box had a minimum area for attaching the inlet duct of 2" greater than the inlet diameter. A medium box was 4" greater and a large box was 8" greater. It was found that the large boxes showed the

highest pressure loss, while the medium boxes showed the lowest. IBACOS tested flexible duct elbows of 6", 8", 10" and 12" over a range of radius to diameter from 0 to 2. It found that the "published data for flexible duct work elbows reasonably approximated the measured pressure losses for all ducts except 12" diameter" (Kokayko et al. 1996)<sup>16</sup>.

Abushakra at the Lawrence Berkeley National Laboratory (LBNL) investigated the effects of compression in non-metallic flexible ducts on static pressure loss (Abushakra et al. 2001, 2002, 2004)<sup>1,2,3</sup>. This research included tests on three sizes of flexible duct: 6", 8", and 10". These tests were conducted in three different compression ratios: maximum stretched, 15% and 30%. The researchers used a draw-through method of testing on the flexible duct as it rested on a flat floor surface. Through these tests the researchers discovered the published static pressure calculated values (ASHRAE 2009)<sup>7</sup> were 70% in error. The actual static pressure losses were higher than calculated values. Abushakra found the values used in the Air Conditioning Contractors of America (ACCA) Manual D for static pressure loss in flexible ducts were 17% to 24% lower than the measured values.

Weaver and Culp at Texas A&M University also investigated the effects of compression in non-metallic flexible ducts on static pressure in the report "Static Pressure Loss in Nonmetallic Flexible Duct" published in *ASHRAE Transactions* (Weaver and Culp 2007)<sup>25</sup>. As with the research by Abushakra, Weaver and Culp tested three sizes of flexible duct: 6", 8" and 10". The compression ratios investigated were increased in this research to 5 different compression ratios: maximum stretched, 4%,

15%, 30% and 45%. The test configuration for this research utilized a blow-through configuration as opposed to previous research which utilized a draw-through configuration. The research found correlation between previous research by Abushakra et al. and this research.

Prior to this work, researchers had looked at the idea of overall system testing using a balancing method for metal ducts, but not methods for deriving static pressure loss in flexible ducts. In 1961, Bricker's work testing for air systems and developing a proportional balancing method using the absolute branch values is detailed in the ASHRAE *Journal* publication "Field Checking and Testing of Ventilation and Air Conditioning Systems" (Bricker 1961)<sup>12</sup>. The article "Balancing Air Flow in Ventilating Duct Systems" published by Harrison in the *Institution of Heating and Ventilation Engineers* (IHVE) Journal in 1965 discusses concerns about various balancing methods and instrumentation (Harrison 1965)<sup>15</sup>. In "Duct System Pressure Gradient Diagrams and the Beer Cooler Problem" (Graham 1996)<sup>14</sup>, Graham discussed utilizing pressure gradient diagrams to look at pressure loss characteristics of HVAC systems.

Fellows, in his paper, "Power Savings through Static Pressure Regain in Air Ducts" (Fellows 1939)<sup>13</sup> discussed savings in power by using a static regain method to design air systems. Subsequent papers like Shieh Chun-Lun's "Simplified Static-Regain Duct Design" (Shieh Chun-Lun 1983)<sup>19</sup> and Scott's "Don't Ignore Duct Design for Optimized HVAC Systems" (Scott 1986)<sup>18</sup> revised the static regain method. In 1986, Tsal and Behls compared the commonly used duct design methods at the time (equal friction, static regain, velocity reduction and constant velocity) to optimal conditions to

determine the parameters that were necessary to design low life cycle cost systems (Tsal and Behls 1986)<sup>21</sup>. The static regain method was later challenged by Tsal and Behls in "Fallacy of the Static Regain Duct Design Method" (Tsal and Behls 1988a)<sup>22</sup> and the T-method was developed for system design. This T-method development was published in an *ASHRAE Transactions* paper (Tsal et al. 1988b)<sup>23</sup>.

Moody's "Friction Factor for Pipe Flow" (Moody 1944)<sup>17</sup> described his research into friction factors for water flow through pipes and airflow through ducts. From this research, friction factors using a surface roughness variable were defined for each case. This research produced the Moody diagram which allows the user to determine the coefficient of the friction factor using the Reynold's number and surface roughness. This friction factor is used as an input into the Darcy equation (2.1) to provide the head loss (Moody 1944)<sup>17</sup>.

$$\Delta P = 12 * f * \left(\frac{L}{D_h}\right) * \rho * \left(\frac{V}{1097}\right)^2$$
 (IP Units) (2.1)

where:

P = Pressure (in H<sub>2</sub>O)

F = Friction Factor (dimensionless)

L = Length (ft)

 $D_h$  = Hydraulic Diameter (ft)

 $\rho = \text{Density (lb/ft}^3)$ 

V = Velocity (ft/s)

The Darcy equation allowed for the calculations of pressure loss through pipes and rigid ductwork but is not valid for flexible duct due to inconsistencies in the internal geometry which are dependent on installed conditions.

Further research into the calculation of the friction factor lead to the Altshul-Tsal equation (2.2). This equation calculates the friction factor using surface roughness, diameter and the Reynold's number. This equation was derived from the research of Altshul and Kiselev in *Hydraulics and Aerodynamics* (Altshul and Kiselev 1975)<sup>6</sup> and Tsal in *HPAC* (Tsal 1989)<sup>24</sup> and eliminates the need to use the Moody diagram to calculate the friction factor.

$$f = 0.11* \left(\frac{12*\varepsilon}{D_h} + \frac{68}{\text{Re}}\right)^{0.25}$$
 (IP Units) (2.2)

Data from the proposed research project could be included in a "ductulator." In 1976, Trane introduced the *Explanation of the Trane Air-Conditioning Ductulator*. A "ductulator" is a device commonly used by industry as a source for pressure drop values. These devices are put out by manufacturers. These "ductulators" are available in both rigid and flexible duct versions (Trane Company 1976)<sup>20</sup>. The flexible duct versions only are valid for duct compressed to roughly 4%. They do not include compressions greater than 4% (Trane Company 1976)<sup>20</sup>.

Through prior research, ASHRAE has developed many standards that will be applicable to the proposed research. ASHRAE Standard 120-1999 provides the method of testing for determining flow resistances in ducts and fittings. This standard includes

design parameters for the construction of airflow chambers, for airflow testing setup and for analysis of data gathered during testing (ASHRAE 1999)<sup>8</sup>. This version of the standard was utilized for this study. At the time of this paper, this standard was updated in 2008. Review of the updated standard found that this study also meets the updated standard version. Standard 42.1 (ASHRAE 1986)<sup>9</sup> provides parameters for temperature measurements during testing. Similarly Standard 42.2 (ASHRAE 1987)<sup>10</sup> and Standard 42.3 (ASHRAE 1989)<sup>11</sup> provide parameters for airflow and pressure measurement, respectively.

Through this literature survey, it was discovered that there is a necessity for testing and validating static pressure losses in installed large diameter (12", 14", and 16") flexible duct. The research by LBNL (Abushakra et al. 2002)<sup>2</sup> tested smaller sized duct diameters and used a draw-through, negative pressure setup. Work by IBACOS (Kokayko et al. 1996)<sup>16</sup> only tested 10% compression and only tested with the duct fully supported. The research done in the area of whole system design methods only deals with a whole air system and not the static pressure losses in lengths of flexible duct. Ductulators have been found to only contain static pressure loss values up to roughly 4% compression. Static pressure loss testing which includes variable compression ratios for duct sizes greater than 10" has not been found in available published literature.

#### **CHAPTER III**

#### CHAMBER AND DUCT SUPPORT SETUP

For the testing of air flow resistance in ducts and fittings, ASHRAE Standard 120-1999 utilizes a flow measuring system. This study used an inlet multiple-nozzle chamber as the primary flow measuring system. To satisfy the requirements of this study, the chamber needed to be able to accommodate between 200 and 2500 cubic feet per minute (CFM) of air flowing through it.

To satisfy the air flow range requirement, multiple aluminum air flow nozzles were needed. The chamber used seven parallel nozzles to achieve the necessary air flow range. One 7" diameter nozzle, two 6" diameter nozzles, two 4" diameter nozzles, and two 3" diameter nozzles were mounted on to a 1/8" thick, 64" diameter piece of galvanized cold rolled steel. Seven holes of varying diameters were cut into the piece of galvanized steel to house the aluminum nozzles and 1/16" nitride rubber gaskets were placed between the interface of the nozzles and the steel to achieve a tight seal around the nozzle. The nozzles were attached to the steel plate using ½"- 20 x ¾" socket cap head screws and ½"- 20 grade C lock nuts. A bead of silicon caulking was laid around the edge of the interface to complete the seal. Figure 1 shows the nozzle board after completion.



Figure 1: Nozzle Board

ASHRAE Standard 120-1999 calls for square mesh wire screens to be used to settle the air flow. For this chamber, five 7' x 7' pieces of screen were cut into 64" diameter circles. Three different open area percentage screens were used: two at 45%, two at 55%, and one at 60%. A piece of Hanover pattern square mesh screen was used for the final 60% open area screen in the chamber. This screen gave a more rigid screen for the air to flow through before leaving the chamber.

The chamber was designed by David Cantrill and fabricated by M&M

Manufacturing Company. The chamber was designed to be constructed in sections to

allow the user to fix problems in the chamber without dismantling the whole chamber. Each section of the chamber was made from sixteen (16) gauge cold rolled galvanized steel and was painted with a black latex enamel to give the chamber a corrosion resistant outer layer. The chamber was cylindrical with an inner diameter of 60". Two inch high, 1/4" thick steel flanges were attached to each of the sections to allow for the sections to be attached to each other. A circular 1/4" bolt hole pattern was cut into each flange utilizing 12 holes in the pattern. Each section was attached to the next section of the chamber using ¼" hex head bolts and ¼" nuts. At each flange-flange interface, a flat circular piece of red silicon gasket was used to seal the chamber. The nine sections used to construct the chamber were as follows: two endcap-ring sections, three 36" long cylindrical sections, four 6" long cylindrical sections and one 36" cylindrical section with a door cutout. For the endcap-ring sections, a 30" diameter ring was attached to a 60" diameter endcap. The endcap-ring section allows various transition pieces to be attached at the entrance and exit of the chamber. The cylindrical section with a door cutout was designed with an interface fabricated into the section for a door to be placed in this section. This door was used to access the nozzles after the chamber was completely together.

The chamber was constructed in the following order (from entrance to exit): entrance endcap-ring section, 36" long section, 45% open area wire mesh screen, 6" long section, 55% open area wire mesh screen, 6" long section, 60% open area wire mesh screen, 36" long section, nozzle board, cylindrical section with door cutout, 45% open area wire mesh screen, 6" long section, 55% open area wire mesh screen, 6" long

section, 60% open area Hanover pattern screen, 36" long section, and an exit endcapring section. After bolting the chamber sections together, silicon caulking was placed around each interface and bolt hole to complete the seal of the chamber. Figure 2 shows an image of the chamber after construction. Four hollow rectangular sections were attached to the bottom of the completed chamber. Two of these sections allow for the use of a forklift to be utilized to move the chamber. Four 8" polyurethane-on-iron-center casters were attached to the remaining two hollow rectangular sections for movement of the chamber. Two of the casters swivel in all directions, while the other two stay rigid. The two swivel casters incorporate a brake that can be used to lock the chamber in place to restrict chamber movement.



Figure 2: Completed Chamber

A backward bladed, centrifugal fan blower system was used to supply air flow to the chamber. The blower system was capable of supplying up to 15,000 CFM air flow to the chamber. The rectangular blower exit was attached to the circular end of the chamber using a heavy polyurethane plastic sheet. This sheet dampened the vibrations from the blower system to minimize the vibration effects on the sensors in the system. A variable frequency drive (VFD) controlled the RPM of the blower. The VFD was controlled by a Visual Basic program. The program controls the VFD by sending a

voltage to the VFD which is proportional to the RPM of the blower. Figure 3 shows the blower and the VFD used.



Figure 3: Blower (left) and VFD (right)

A twenty (20) gauge galvanized steel duct transition piece was mounted to the exit of the chamber. This transition piece gradually changed the diameter of the system from the 30" diameter ring to the diameter of the duct to be tested. The slope of the transition cannot be greater than 7.5° as specified in ASHRAE Standard 120-1999. For this study, three transition pieces were manufactured with exit diameters of 12", 14" and 16".

The duct used for testing sat upon duct supports. The duct supports were made from 2" x 4" pine pieces cut to length. The supports consisted of three sections: a top section and two legs. The top section measured 6' in length and 24.5" in width. Starting from the front, 2" x 4" pieces are placed 24" apart on centers. Five lengths of 2" x 4" pine were used to make each leg. Each side of the leg used one 30" long piece and one 18" long piece. Two sets of three holes were drilled into each of the pieces used for the side of the leg. These holes allowed the support to be moved up or down to allow the duct to match the height of the transition piece attached to the chamber. An 18.5" long piece of 2" x 4" attached perpendicularly to each of the 30" long pieces to provide rigidity for the leg. The 30" and 18" long pieces attached to each other using a carriage bolt placed through one of the holes in each piece. Each leg assembly attaches to the top section with 2" wood screws. Twelve support sections were constructed to match the longest length of duct to be tested. Figure 4 shows a support without the lower legs attached.



**Figure 4: Duct Support without Lower Legs** 

The rigid duct testing entrance and exit sections are fabricated before any testing occurs. The entrance and exit section lengths do not change during the testing of a duct diameter. The entrance section was constructed from galvanized sheet metal duct. The length of the section must be greater than ten duct diameters to be in compliance with ASHRAE Standard 120-1999. The exit section was constructed from galvanized sheet metal duct with a length greater than four duct diameters. An entrance and exit section was constructed for each diameter of duct tested.

#### **CHAPTER IV**

#### **ELECTRONICS/SENSOR SETUP**

This study utilizes three different types of sensors to help analyze the air flow through the entire system. Temperature, humidity, and differential pressure sensors are used in this system. Table 1 identifies each sensor used and the specifications of each. All of the sensors utilize a 4-20 mA output signal that is sent to the monitoring system. Discussion of the monitoring system occurs later in this section.

**Table 1: Sensor Specifications** 

			#			%		Response
Sensor	Manuf.	Model	Used	Range	Units	Accuracy	Drift	(msec)
Diff. Pressure	Dwyer	607-0	1	0-0.10	in H2O	0.5% FS	0.5% FS/yr	250
Diff. Pressure	Dwyer	607-2	1	0-0.50	in H2O	0.5% FS	0.5% FS/yr	250
Diff. Pressure	Dwyer	607-3	1	0-1.0	in H2O	0.5% FS	0.5% FS/yr	250
Diff. Pressure	Dwyer	607-4	3	0-2.0	in H2O	0.5% FS	0.5% FS/yr	250
Diff. Pressure	Dwyer	607-7	1	0-5.0	in H2O	0.5% FS	0.5% FS/yr	250
Temperature	Dwyer	650-2	3	20-120	°F	0.3% FS	0.5% FS/yr	500
Humidity	Dwyer	RHT-D	1	0-100%	RH	2% RH	<1% RH/yr	5000-15000

The system uses three silicon-junction transistor temperature sensors to report the dry bulb temperature of the air as it passes through the system. A temperature sensor is mounted on the chamber before the nozzle board. This sensor reports the air temperature entering the duct system. A second temperature sensor is located three plus/minus one half duct diameters before the pressure tap that begins the duct testing

section. The third temperature sensor is located three plus/minus one half duct diameters after the pressure tap that ends the duct testing section. These two sensors report the entrance and exit temperature of the air in the test section, respectively.

The humidity sensor used in this system reports the relative humidity value.

Although the sensor has the ability to report both humidity and temperature, for this study, the sensor reports only humidity. The sensor uses a capacitance effect polymer element.

The system utilizes multiple differential pressure sensors to report the static pressures at multiple spots along the system. These pressure sensors use a diaphragm in the sensor housing to report the pressure readings. This diaphragm deflects under pressure which sends a voltage from the sensor to the monitoring system in proportion to the amount of deflection. The first use of the sensors measures the differential pressure across the nozzle board. The user uses this pressure reading to determine the amount of air flowing into the ducts. Three sensors are used to find the pressure across the nozzles. One sensor reads the pressure on the entrance side of the nozzles. This sensor reads the difference between the moving air static pressure and the standard air in the area of testing. Another sensor reads the same type of difference, but on the exit side of the nozzles. The third sensor reports the difference in pressure between the entrance side and the exit side of the nozzles. For the duct testing section, a similar system is used to measure the pressure loss through the test section. One sensor measures the difference in the static pressure entering the section against the standard air in the testing area.

Another sensor reads a same differential pressure at the exit of the test section. A third sensor measures the difference in the entrance static pressure and the exit static pressure.

The system uses piezometer rings attached to the pressure sensor by a length of silicon tubing to measure the pressure in the system. The piezometer rings used follow the specifications for piezometer rings in ASHRAE Standard 120-1999, Section 6.2. Section 6 of ASHRAE Standard 120-1999 also shows a figure of a piezometer as an example. This device functions as an averaging device for the four static pressure readings where installed. The monitoring system uses this one averaged value as the reported pressure reading. The piezometer ring is made of silicon tubing and mounts to the duct using four pressure taps. ASHRAE 120-1999, Section 6.3 and Figure 1 in Section 6 give the acceptable dimensions needed. The taps were made from 24 gauge copper plate and 1/4" outer diameter copper tubing. The copper plate is cut into sixteen 3" by 3" square pieces. Sixteen 1 inch pieces are cut from the copper tubing. The copper tubing pieces are soldered to the copper plate in the center of one side. After soldering the assembly is quenched in a water bath to cool and harden the soldered area. Once the assembly is cooled, a 1/8" hole is drilled through the copper plate. The center of the drilled hole is drilled at the center of the copper tube. The process repeats until all sixteen assemblies are finished. Before mounting the taps to the duct, four 3/32" holes are drilled into the duct at four equidistant spots around the duct. These four holes must be in a single plane. The tap assemblies mount to the duct using a layer of silicon caulking. The hole in the duct must line up with the tubing. The plate of the tap assembly contours to the shape of the duct. To secure the tap to the duct and to seal the

tap, aluminum duct tape is used. Once the taps are mounted to the duct, the piezometer ring attaches to each of the four taps. The single output of the ring attaches to the pressure sensor with a length of ¼" silicon tubing. The temperature sensors also mount using silicon caulking and aluminum duct tape. Figure 5 gives an example of the piezometer ring and temperature sensor mounted to the duct.



Figure 5: Piezometer Ring (left) and Temperature Sensor (right) Mounted

All of the sensors attach to the data acquisition (DAQ) system through a DAQ board. A piece of wire connects the negative terminal of the sensor to a designated channel of the DAQ board. A wire connects the next associated channel to the negative

terminal of the 12 volt - 1 amp power supply. To attach all of the sensors to the one negative power supply terminal, a piece of wire runs from the negative power supply terminal to a wing nut. The wires from the associated channels for each sensor run to this same wing nut. This cluster of wiring in the wing nut allows for multiple connections to the one power supply terminal. The positive side of the loop uses the same method with the wing nut. A single wire comes from the positive power supply terminal and meets with the wires from the positives of each sensor at the wing nut. A  $250\Omega$  (.05%) precision resistor placed between the two channels on the DAQ board completes the sensor loop for each sensor. This resistor converts the current output of the sensor to a voltage input to the DAQ system. A NEMA 1 case houses the pressure sensors, wiring, and DAQ board. The case protects its contents from dust and other contaminants. Figure 6 shows the sensor wiring diagram. Figure 7 shows a picture of the pressure sensors and Figure 8 shows the DAQ board wiring. The DAQ board connects to a DAQ card mounted in a computer. The board sends the voltage readings to the card which the computer uses to report the readings to the user.

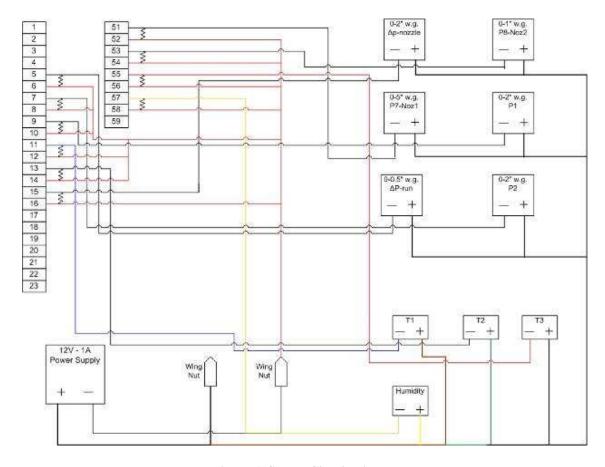


Figure 6: Sensor Circuit Diagram



**Figure 7: Differential Pressure Sensor Array** 

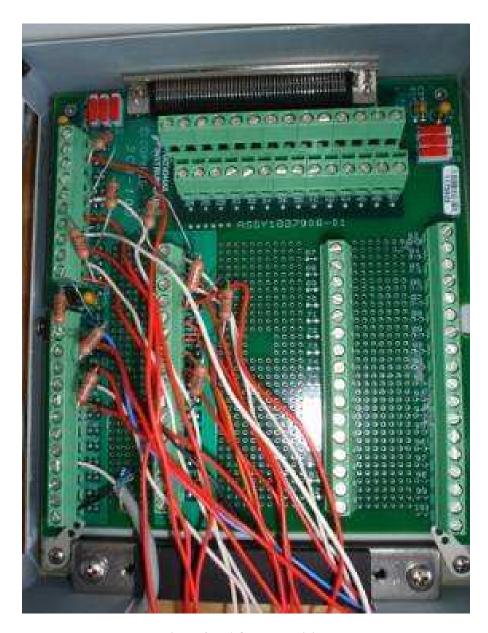


Figure 8: DAQ Board Wiring

#### **CHAPTER V**

# VISUAL BASIC MONITOR, FLOW CALCULATOR, AND TEST VERIFICATION

To control the measurements and operation of the system, a Visual Basic program was written. Figure 9 gives an example screenshot of the monitor window which gives the user control of the system.

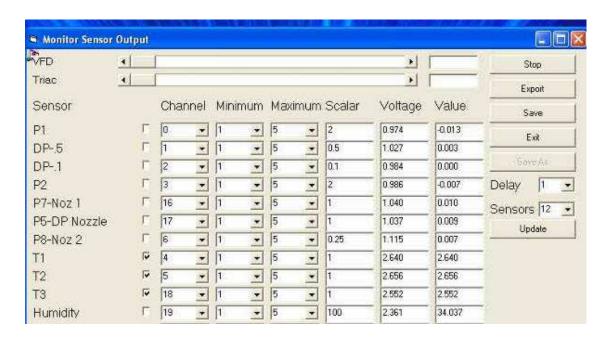


Figure 9: Visual Basic Monitor Window

The program setup allows for the VFD to be controlled with a slider. The movement of this slider changes the voltage sent to the VFD. The first column of the program allows for each sensor to be given a name. This allows the user to easily identify what each sensor outputs. The channel in which the sensor connects to the DAQ board goes into the second column. The third column identifies the minimum voltage outputted by the sensor. Because all of the sensors are on a 4-20 mA circuit with a  $250\Omega$ resistor, every sensor has a minimum voltage value of 1. The next column contains the maximum voltage output of the sensor. For the same reason as the minimum voltage, this voltage is 5. The scalar column allows the user to input the factor which scales the voltage value to give a true unit reading. For pressure sensors, the maximum pressure value of the sensors is inputted in the column. For the temperature sensors, 1 is inputted. For the humidity sensor, 100 is inputted. The 100 scalar converts the RH value from a decimal to a percentage. The next column reports the voltage outputted from the sensor itself. The final column gives the value outputted by the sensor in a true unit form except for the temperature sensors. For pressure the true unit is in H2O and for humidity it is %RH. The top button on the right of the monitor window allows the user to start and stop the monitor window's real-time sensor reporting. The next button exports the reported real-time values to an Excel spreadsheet for storage until data analysis.

An important tool used in the study is the flow calculator spreadsheet. This spreadsheet calculates the pressure drop across the nozzles necessary to achieve a certain air flow rate. Figure 10 shows an example of the spreadsheet used.

		No	szeles
With the state of	Dia. (in.)		Area (ft <sup>2</sup>
Nozzle 1	7	V	0.26
Nozzle 2	6	V	0.190
Nozzle 3	6	9	0.196
Nozzle 4	4	V	80.0
Nozzle 5	4	V	0.08
Nozzle 6	3	V	0.04
Nozzle 7	3	Q.	0.04
	A	ir Pi	roperties
T1(F)	3,003		70.075
T2(F)	3.09		72.250
T3 (F)	3.324		78.100
AP Noz	0.302		Nozzle Pressure Drop
Pb (in.HG) Internal	30.170		Barometric Pressure
Twb (F) wingen	51.200		Wet Bulb Temperature
Pnoz1	0.050		Static Pressure Before Nozzles
Tdb	71.163		Dry Bulb Temperature Average
Pe	0.372		Saturated Vapor Pressure
Pp	0.149		Partial Vapor Pressure
po (lb/ft^3)	0.075		Ambient Air Density
p5	0.075		In-Statiion Air Density
R	53.350		Gas Constant
A	0.999		Alpha Ratio
μ.	1.226E-05		Dynamic Air Viscosity
Υ	1.000		Expansion Factor
Re1	124497		Nozzle 1 Reynolds Number
Re2	106712		Nozzle 2 Reynolds Number
Re3	106712		Nozzle 3 Reynolds Number
Re4	71141		Nozzle 4 Reynolds Number
Re5	71141		Nozzle 5 Reynolds Number
Re6	53356		Nozzle 6 Reynolds Number
Re?	53356		Nozzle 7 Reynolds Number
C1	0.980		Nozzle 1 Discharge Coefficient
C2	0.978		Nozzle 2 Discharge Coefficient
C3	0.978		Nozzle 3 Discharge Coefficient
C4	0.974		Nozzle 4 Discharge Coefficient
C5	0.974		Nozzle 5 Discharge Coefficient
C6	0.971		Nozzle 6 Discharge Coefficient
C7	0.971		Nozzle 7 Discharge Coefficient
sumca	0.911		Sum of Coefficients
CFM	2000.941		Flowrate through Nozzle Bank

Figure 10: Flow Calculator Spreadsheet

The top box of this spreadsheet contains information about the nozzles used in each test. A "Y" is placed in the appropriate column for each nozzle that is open for the test. The next box contains the information concerning the air flow through the system. The user inputs values for the three temperature sensors, the barometric pressure, the static pressure before the nozzles, the wet bulb temperature, and the differential pressure. The three inputted temperature values average to give the dry bulb temperature. The spreadsheet uses these values in conjunction with formulas located in ASHRAE Standard 120-1999, Section 9 to find and output an air flow rate. The spreadsheet also reports each of the values calculated and subsequently used in the calculation of the air flow rate. From this spreadsheet, the user takes the differential nozzle pressure and uses it in conjunction with the monitor window to control the VFD.

The next tool used in this study comes in the form of the test verification spreadsheet (TVS). This spreadsheet contains all of the descriptive information about each test. Figure 11 shows an example of the test verification spreadsheet.

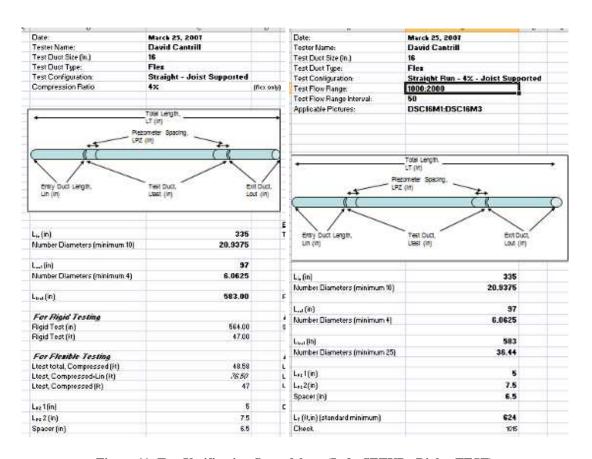


Figure 11: Test Verification Spreadsheet (Left: SETUP - Right: TEST)

The spreadsheet contains two similar worksheets. The first worksheet, entitled SETUP, contains the information from the setup of the duct. It gives the date of the test, the tester's name, the duct size to be tested, the type of duct tested, the configuration of the test, and the compression ratio if flexible duct is tested. The graphic within the worksheet shows a general configuration of the duct and the reduced names used in the spreadsheet. The appropriate dimensions are inputted where appropriate. The second worksheet, entitled TEST, contains the information necessary for the test. This

worksheet contains the basic dimensions from the SETUP worksheet. This worksheet differs from the other by the addition of the flow range, the flow range interval, and the applicable pictures taken for the test. A TVS is made for each test configuration that is tested. This allows individuals to recreate the tests if necessary.

## **CHAPTER VI**

## **AIRFLOW EQUATIONS**

The air flow rates used in the system were determined by measuring the static pressure loss across flow nozzles mounted on a nozzle board in the chamber. The flow calculator spreadsheet discussed in Chapter 5 was used to calculate the desired air flow rate using the measured static pressure drop across the nozzles. All equations used in the flow calculator spreadsheet are taken from ASHRAE Standard 120-1999, Section 9. The following are the user inputs into the flow calculator spreadsheet and the equations used to calculate air flow rates from the static pressure drop across the nozzles.

## **Inputs**

The following variables are either measured using the air flow test setup or are visually determined. IP units shown in parenthesis. SI units shown in brackets.

Dia<sub>i</sub> Diameter of each nozzle used in test. (in) [cm]

An<sub>i</sub> Area of each nozzle used in test.  $(ft^2)$  [m<sup>2</sup>]

 $\Delta P_{noz}$  Measured static pressure drop through nozzle bank. (in-H<sub>2</sub>O) [Pa]

 $T_{db}$  Dry bulb temperature of air within test duct. Calculated as average of  $T_1$  and  $T_2$ . (°F) [°C]

P<sub>b</sub> Barometric pressure. Taken from weather data for Easterwood Airport, which is located 8 miles from the test location. (in-Hg) [kPa]

 $T_{wb}$  Wet bulb temperature of air within test system. Calculated using psychrometric properties for air with inputs of dry bulb temperature ( $T_{db}$ ) and relative humidity (RH) from monitor program. (°F) [°C]

P<sub>noz1</sub> Static pressure in in-H<sub>2</sub>O recorded before nozzle bank (in-H<sub>2</sub>O) [Pa]

## **Equations**

(IP) = 
$$(2.96*10^{-3})T_{wb}^{2} + (1.59*10^{-2})T_{wb} + 0.41$$
 (in – H20)

(SI) = 
$$(3.25*10^{-3})T_{wb}^{2} + (1.86*10^{-2})T_{wb} + 0.692$$
 (kPa)

(IP) 
$$= P_e - \frac{(P_b(T_{amb} - T_{wb}))}{2700}$$
  $(in - H20)$ 

(SI) 
$$= P_e - \frac{(P_b(T_{amb} - T_{wb}))}{1500}$$
 (kPa)

$$\rho_{\rm o}$$
 Ambient Density of Air (6.3)

(IP) 
$$= \frac{70.75(P_b - 0.378P_p)}{53.35(T_{amb} + 459.67)} \qquad (\frac{lb}{ft^3})$$

(SI) 
$$= \frac{(P_b - 0.378P_p)}{0.287(T_{amb} - 273.2)} \qquad (\frac{kg}{m^3})$$

$$\rho_5$$
 Density of air within chamber (6.4)

(IP) 
$$= \rho_o \left( \frac{T_{amb} + 459.67}{T_{db} + 459.67} \right) \left( \frac{P_{noz1} + 13.63P_b}{13.63P_b} \right)$$
  $\left( \frac{lb}{ft^3} \right)$ 

(SI) 
$$= \rho_o \left( \frac{T_{amb} + 273.2}{T_{db} + 273.2} \right) \left( \frac{P_{noz1} + 1000P_b}{1000P_b} \right)$$
  $\left( \frac{kg}{m^3} \right)$ 

$$(IP) = 1 - \left(\frac{\Delta P_{noz}}{P_5 + 13.63 P_h}\right)$$

(SI) 
$$= 1 - \left(\frac{\Delta P_{noz}}{P_5 + 1000 P_h}\right)$$

(IP) = 
$$(11+0.018 T_5) 10^{-6}$$
  $(\frac{lbm}{ft*s})$ 

(SI) = 
$$(17.23 + 0.048 T_5) 10^{-6}$$
 (Pa\*s)

$$Y_n$$
 Expansion factor (6.7)

(IP) = 
$$\left[ 3.5 \, \alpha^{1.43} \left( \frac{1 - \alpha^{0.286}}{1 - \alpha} \right) \right]^{0.5}$$

(SI) = 
$$\left[3.5 \,\alpha^{1.43} \left(\frac{1-\alpha^{0.286}}{1-\alpha}\right)\right]^{0.5}$$

Re Reynolds Number of air within chamber (6.8)

(IP) = 1,363,000 
$$\left(\frac{d}{12}\right) (\rho_5 \Delta P_{noz})^{0.5}$$

(SI) = 70,900 
$$d \left( \rho_5 \Delta P_{noz} \right)^{0.5}$$

C<sub>i</sub> Discharge Coefficient (6.9)

(IP) = 
$$0.9965 - 0.00653\sqrt{\frac{10^6}{\text{Re}_d}}$$

(SI) = 
$$0.9965 - 0.00653\sqrt{\frac{10^6}{\text{Re}}}$$

ΣCa Sum of coefficients

$$= An_1 * C_1 + An_2 * C_2 + \dots + An_i * C_i$$
(6.10)

CFM Volumetric flow rate (6.11)

(IP) 
$$= 1097Y_n \sqrt{\frac{\Delta P_{noz}}{\rho_o}} \Sigma Ca \qquad (\frac{ft^3}{\min})$$

(SI) 
$$= 1414Y_n \sqrt{\frac{\Delta P_{noz}}{\rho_o}} \Sigma Ca$$
 ( $\frac{l}{s}$ )

## **CHAPTER VII**

## **TEST METHODOLOGY**

#### **Nozzle Board Leak Test**

Prior to assembly of the complete test setup, the nozzle board requires leak testing to ensure that leakage from seals and nozzles does not exceed allowable tolerances. The leak testing procedure is outlined in the following steps:

- 1. Leak testing is to occur on a monthly basis.
- 2. Seal blower end of chamber.
  - a. Use object cut to fit exit diameter.
  - b. Apply blue painter's tape to completely seal opening.
- 3. Open door to outlet side of nozzle board.
- 4. Seal all nozzles inside chamber.
  - a. Use nozzle caps to cover each nozzle outlet.
  - b. Apply tape to junction where cap and nozzle intersect with blue painter's tape to ensure a tight seal.
- 5. Attach air hose from flow measurement device (shown in Figure 12) to barbed air hose connection on chamber (shown in Figure 13).



**Figure 12: Flow Measurement Device** 



Figure 13: Barbed Air Hose Connection

- 6. Attach other end of flow measurement device to hose connected to air supply (air compressor) using the quick release connection.
- 7. Open Monitor Window Program from computer desktop.
- 8. Press "Scan" button.
- 9. Turn knob on flow measurement device until the differential pressure sensor located on the inlet side of the nozzle board displays a value of approximately 0.100"  $H_2O$ .
- 10. Once the pressure reaches approximately 0.100" H<sub>2</sub>O, record the height of the top of the red ball within the flow measurement device cylinder.
- 11. This value is equivalent to the amount of air flow that is entering the system to maintain the described pressure. This value also represents the amount of leakage in the section tested.
- 12. This value is displayed in units of cubic feet per hour of Argon (CFH).
- 13. This value needs to be converted to cubic feet per hour of air.
- 14. A value of 1 is used to convert from cubic feet per hour of Argon to cubic feet per hour of air, given that the precise conversion factor from Argon to Air is 0.999.
- 15. The value is further converted to units of cubic feet per minute of air (CFM) using the conversion factor of 1 CFH = 60 CFM.
- 16. ASHRAE Standard 120 1999 does not state a maximum amount of leakage across the nozzle board.

- 17. Air leakage rates less than 1 CFM shall be considered acceptable for testing purposes, based on rule of thumb criteria.
- 18. There is an inversely proportional relationship between the air leakage rate and the accuracy of future readings during duct testing and thus lower leakage rates are desirable.
- 19. If the tested leakage value is below the maximum allowable leakage rate, testing may begin.
- 20. If the leakage is found to be greater than the maximum acceptable rate, sources of air leakage should be identified and sealed until the measured air leakage for the nozzle board falls below the maximum allowable rate.

#### **Preassembly of Duct**

Upon completion of the nozzle board leak test, the remainder of the test apparatus can be assembled. The preassembly of the duct only needs to be done when ready to test a new duct diameter. First, select the sheet metal transition piece that changes the duct diameter from the 30" diameter of the endcap-ring piece to the diameter of the duct to be tested. Slide the transition piece onto the collar of the chamber and screw the transition piece and collar together with self-tapping sheet metal screws. Using aluminum duct tape, tape the lateral joint where the collar and transition piece meet. Smooth out the tape to remove any air bubbles in the tape. Next, apply another layer of tape to this lateral joint staggered with the first layer and smooth out the tape to remove any air bubbles. Then, slide the premade duct entrance section for the

correct duct diameter onto the end of the transition piece. Tape the lateral joint using the same procedure used to tape the transition piece to the endcap-ring.

For rigid duct testing, slide the necessary length of rigid duct required for testing (minimum of 25 diameters) and tape each lateral joint in the manner used above. For flexible duct testing, attach the appropriate length of flexible duct required for testing (minimum 25 diameters) to the end of the entrance section. Tape the end of the plastic, flexible duct material to the end of the rigid entrance section. Figure 14 shows an example of the flexible duct connected to the entrance section.



**Figure 14: Flexible Duct – Entrance Section Joint** 

If multiple lengths of flexible duct are required, use a sheet metal collar to connect the lengths end to end and tape them onto the collar using aluminum tape. Next, fully stretch the entire length of flexible duct and mark equal, one foot sections. After placing the last length of duct (rigid or flexible) for testing, attach the premade duct exit section of the correct diameter. Tape the lateral joint in the manner used above.

## **System Leak Testing**

After completing the preassembly of the duct, the system needs to be leak tested. The leak test considers the chamber, transition piece, and duct sections as one complete system. This leak testing follows a similar procedure as the nozzle board leak test as follows:

- 1. This test should be done with each change of configuration.
  - a. Examples are rigid testing and flexible testing
  - b. Done any time there is a break in the setup.
- 2. Seal blower end of chamber and duct exit end of chamber.
  - a. Use object cut to diameter of exit.
  - b. Tape with blue painter's tape to ensure it is sealed.
- 3. Make sure chamber door is closed and sealed.
- 4. Attach air hose from flow measurement device (shown in Figure 12) to barbed air hose connection on chamber (shown in Figure 13).

- 5. Attach other end of flow measurement device to hose connected to air supply (air compressor) using the quick release connection.
- 6. Open Monitor Window Program from desktop.
- 7. Press "Scan" button.
- 8. Turn knob on flow measurement device until all pressure sensors are displaying a value of about 0.100°  $H_2O$ .
- 9. Once pressures reach about 0.100" H<sub>2</sub>O, record the height of the top of the red ball in the cylinder of the flow measurement device.
- 10. This value is the amount of air flow that is entering the system to maintain the described pressure. This value also equals the amount of leakage in the system.
- 11. This value is displayed in units of cubic feet per hour of Argon (CFH).
- 12. This value needs to be converted to cubic feet per hour of air.
- 13. Because the multiplier to convert from Argon to air is 0.999, the multiplier used is 1.
- 14. The value is converted to units of cubic feet per minute of air (CFM) using the relationship of 1 CFH = 60 CFM
- 15. ASHRAE Standard 120 1999 requires that the maximum amount of leakage in the system is 0.5% of the minimum air flow that will be tested.

- 16. For example, if the lowest air flow to be tested is 200 CFM, the maximum amount of leakage for the system is 1 CFM.
- 17. If the tested leakage value is within the acceptable range, testing may begin.
- 18. Otherwise leak sources should be identified and sealed until the standard leak rate is no longer exceeded.

## **Flexible Duct Compression Setup**

For compression testing of the flexible duct, determine the amount of compression that each one foot section of flexible duct needs to be compressed to create the correct compression amount for the entire test section. Next, place a tape measure or yardstick on the support structure alongside the duct. Compress each one foot section the amount determined above. If conducting board supported tests, lay 2' x 8' pegboards on top of wooden support structure and set the flexible duct on top of them. Take multiple pictures along the compressed test area to show duct is at correct compression ratio. Figures 15 through 17 show examples of the pictures taken for a 12" 4% compression board supported test. Take a picture of the end of the test duct to document that the test duct length meets the necessary minimum of 25 diameters. Figure 18 shows an example of this for a 12" board supported maximum stretched duct test. The appropriate TVS should be completed for each test at this time.



**Figure 15: Example Photograph of Test Setup Entrance Section** 



Figure 16: Example Photograph of Test Setup from Above



Figure 17: Example Photograph of Test Setup from Side



Figure 18: Example Photograph Showing Length of Test Section

## **Operation**

To start the testing process, turn on the data acquisition PC and open the Visual Basic monitor program and the flow calculator spreadsheet. Next, determine the air flow range to be tested. Determine which nozzles need to be used for the set of tests using the flow calculator spreadsheet. Input an upper limit for the differential pressure and vary the nozzles that are opened until the upper limit of the intended air flow range is given. The author used a differential pressure of no greater than 2.5" w.g. when determining the nozzles to be used. Once the necessary nozzles are found, open and remove the chamber door. Place nozzle endcaps on the nozzles that will not be used. Place blue painter's tape around the joint where the caps and the nozzles meet to seal the nozzles. Replace and close the chamber door ensuring an airtight seal. Next, plug the VFD into a 480V outlet and turn the outlet on. Press the RUN MODE button on the VFD until the green "manual" light lights up. Next, press the RUN button on the VFD. This will cause the blower to start rotating at a low RPM. Figure 19 shows the interface of the VFD and the buttons used above.



Figure 19: VFD Interface

Next, press the "Scan" button in the monitor window. Using the flow calculator spreadsheet, determine the pressure drop that corresponds with the air flow rate to be tested. Input the temperature voltage readings from the monitor window. Input the correct nozzles used for the test. Input the barometric pressure found on the NOAA website for Easterwood Airport in College Station, TX:

(http://www.srh.noaa.gov/ifps/MapClick.php?CityName=College+Station&state=TX&si te=HGX). Using the dry bulb temperature given in the calculator and the humidity value

from the monitor window, calculate the wet bulb temperature using a psychrometric computer program. This program is a simple psychrometric calculation program that determines wet bulb temperature using dry bulb temperature and relative humidity as inputs. Input the wet bulb temperature from the psychrometric program into the flow calculator spreadsheet. Input values for the nozzle differential pressure until the air flow rate is at the desired flow rate to be tested.

Using the nozzle differential pressure value from the flow calculator spreadsheet, move the VFD slider bar on the monitor window until the value for the differential pressure across the nozzles on the monitor matches the value of the nozzle differential pressure from the flow calculator spreadsheet. Once the value of the nozzle differential pressure becomes stable (varies less than  $\pm 0.005$ " w.g.), press the "Export" button. This opens an Excel spreadsheet and exports sensor values for each time step. For this study, the time step used was one second. After the required number of data points has been taken (50), press the "Stop" button that used to read "Export" in the monitor window. This button will return to reading "Export." Press the "Save As" button and name the file and place it in the appropriate folder of the PC's hard drive. Next, close the Excel file. Repeat the process beginning with the flow calculator for the next flow rate to be tested. Repeat until all flow rates in the desired range are tested. If testing rigid duct, this ends the testing procedure. For flexible duct testing, the compression amount of the duct needs to be changed to the next compression to be tested. Then, the process is repeated beginning with the test flexible duct test setup section above.

## **CHAPTER VIII**

## **ANALYSIS METHODOLOGY**

After the data collection phase ended, the data was analyzed and trended. To begin the analysis, the Excel spreadsheet that contains the lowest flow rate for the compression ratio tested was opened. The data points for each column of data which contained approximately 50 values were averaged to one value for each column. The spreadsheet was resaved to include the averaged values. Figure 20 provides an example of the averaged value row. The next flow rate spreadsheet in the range was opened and averaged as above. This process was repeated until each flow rate in the range was averaged.

Another spreadsheet was created to contain the averaged values from each set of approximately 50 flow rate measurements collected in the range tested. The spreadsheet contains the averaged data. Figure 8-2 shows the setup of this spreadsheet. The first two rows of the spreadsheet contain the conversion factors used to convert the pressure drop across the test section and the air flow rate from IP units to SI units. These spreadsheets contain data in both units. The fourth row includes the length of duct tested associated with the test range being analyzed. The fifth row contains the length of rigid sheet metal duct contained in the total test length. The seventh row of the spreadsheet contains the sensor names, flow rate in both sets of units, and the differential pressure across the test section in both IP and SI units. Rows 8 and higher contain the averaged and analyzed data in ascending order starting with the lowest flow rate in the test range. Table 2 describes the organization of columnar data from the spreadsheet in Figure 21.

4	Α	В	С	D	Е	F	G	Н	- 1	J	K	L	M
1	Time	Date	P1	DP5	DP1	P2	P7-Noz 1	P5-DP Noz	P8-Noz 2	T1	T2	T3	Humidity
23	3:40:42 PM	9/18/2006	0.052	0.044	0.045	0.006	0.155	0.026	0.107	0.533	0.541	0.561	70.048
24	3:40:44 PM	9/18/2006	0.051	0.044	0.045	0.004	0.15	0.02	0.102	0.533	0.539	0.562	70.064
25	3:40:45 PM	9/18/2006	0.067	0.059	0.053	0.005	0.168	0.028	0.12	0.533	0.541	0.563	70.106
26	3:40:46 PM	9/18/2006	0.043	0.036	0.036	0.005	0.149	0.026	0.098	0.529	0.539	0.562	70.061
27	3:40:47 PM	9/18/2006	0.049	0.041	0.044	0.007	0.152	0.024	0.103	0.532	0.542	0.561	70.053
28	3:40:48 PM	9/18/2006	0.055	0.049	0.043	0.002	0.158	0.028	0.11	0.532	0.541	0.562	70.095
29	3:40:50 PM	9/18/2006	0.049	0.042	0.04	0.003	0.148	0.026	0.098	0.532	0.54	0.563	70.138
30	3:40:51 PM	9/18/2006	0.049	0.042	0.042	0.006	0.154	0.028	0.107	0.533	0.541	0.561	70.138
31	3:40:52 PM	9/18/2006	0.045	0.036	0.038	0.007	0.155	0.026	0.104	0.533	0.541	0.563	70.015
32	3:40:53 PM	9/18/2006	0.048	0.042	0.042	0.004	0.153	0.027	0.104	0.531	0.54	0.562	70.082
33	3:40:54 PM	9/18/2006	0.058	0.051	0.048	0.007	0.159	0.028	0.113	0.533	0.54	0.562	70.072
34	3:40:56 PM	9/18/2006	0.046	0.039	0.039	0.007	0.156	0.024	0.105	0.532	0.54	0.562	70.08
35	3:40:57 PM	9/18/2006	0.047	0.039	0.039	0.005	0.147	0.028	0.098	0.533	0.54	0.562	70.054
36	3:40:58 PM	9/18/2006	0.051	0.046	0.04	0.003	0.155	0.029	0.107	0.533	0.539	0.562	70.116
37	3:40:59 PM	9/18/2006	0.051	0.042	0.046	0.008	0.153	0.027	0.105	0.532	0.54	0.561	69.993
38	3:41:00 PM	9/18/2006	0.052	0.047	0.044	0.003	0.147	0.025	0.101	0.532	0.543	0.562	70.163
39	3:41:01 PM	9/18/2006	0.044	0.036	0.04	0.008	0.149	0.028	0.099	0.533	0.539	0.562	70.102
40	3:41:03 PM	9/18/2006	0.054	0.047	0.045	0.005	0.158	0.026	0.109	0.533	0.54	0.561	70.125
41	3:41:04 PM	9/18/2006	0.046	0.039	0.039	0.006	0.153	0.028	0.101	0.533	0.54	0.562	70.104
42	3:41:05 PM	9/18/2006	0.061	0.054	0.052	0.005	0.157	0.029	0.109	0.535	0.538	0.56	70.117
43	3:41:06 PM	9/18/2006	0.059	0.051	0.046	0.006	0.158	0.027	0.109	0.533	0.539	0.561	70.107
44	3:41:07 PM	9/18/2006	0.05	0.043	0.042	0.004	0.15	0.025	0.104	0.532	0.54	0.562	70.128
45	3:41:09 PM	9/18/2006	0.055	0.047	0.046	0.005	0.152	0.027	0.103	0.535	0.541	0.561	70.108
46	3:41:10 PM	9/18/2006	0.055	0.046	0.047	0.007	0.158	0.027	0.107	0.533	0.541	0.561	70.109
47	3:41:11 PM	9/18/2006	0.054	0.046	0.047	0.006	0.15	0.026	0.1	0.534	0.542	0.562	70.109
48	3:41:12 PM	9/18/2006	0.039	0.032	0.038	0.007	0.145	0.023	0.095	0.533	0.54	0.561	70.102
49	3:41:13 PM	9/18/2006	0.06	0.051	0.049	0.007	0.165	0.028	0.117	0.531	0.539	0.562	70.155
50	3:41:15 PM	9/18/2006	0.049	0.042	0.043	0.006	0.15	0.031	0.102	0.533	0.54	0.561	70.073
51	3:41:16 PM	9/18/2006	0.06	0.052	0.045	0.005	0.158	0.028	0.108	0.532	0.541	0.561	70.165
52	3:41:17 PM	9/18/2006	0.043	0.034	0.037	0.007	0.15	0.028	0.101	0.533	0.54	0.56	70.056
53	3:41:18 PM	9/18/2006	0.046	0.036	0.04	0.009	0.156	0.027	0.104	0.533	0.541	0.562	70.078
54			0.051269	0.043615	0.043173	0.005808	0.153385	0.026904	0.104558	0.5325	0.540115	0.561865	70.06581

Figure 20: Example of Averaged Row

**Table 2: Analysis Spreadsheet Column Descriptions** 

Column	Value	Comment
A	Blank	
В	CFM	Air flow rate in IP units
С	DP-100	Differential pressure drop per 100 feet of duct in IP units The value of this column is calculated by taking the differential pressure measured across the test section and subtracting the calculated pressure drop across the rigid length.
D	L/s	Airflow rate in SI units
Е	Pa/m	Differential pressure drop in SI units
F	P1	Static pressure measurement at entrance of test section
G	DP5	Differential pressure measurement across test section with 0.5 in wg maximum sensor
Н	DP1	Differential pressure measurement across test section with 0.1 in wg maximum sensor
I	P2	Static pressure measurement at exit of test section
J	P7-Noz 1	Static pressure measurement at entrance of nozzle bank
K	P5-DP Noz	Differential pressure across nozzle bank
L	P8-Noz 2	Static pressure measurement at exit of nozzle bank
M	T1	Voltage reading of temperature probe at entrance of test section
N	T2	Voltage reading of temperature probe at exit of test section
0	Т3	Voltage reading of temperature probe at airflow chamber
P	Humidity	Humidity reading in airflow chamber
Q	Blank	
R	Rigid-100	Differential pressure drop per 100 feet of rigid duct in IP units
S	Rigid	Differential pressure drop per length of rigid duct in IP units

1 in H20	)	=	= 8.164 Pa/m														
1 CFM		=	0.4719 L/s														
Test Length:		49	49														
Rigid Length:		1.58															
CFM		DP-100	L/s	Pa/m	P1	DP5	DP1	P2	P7-Noz 1	P5-DP No.	P8-Noz 2	T1	T2	T3	Humidity	Rigid-100	Rigid
	009	0.090	47	0.74	4 0.049	0.043	0.044	0.018	0.193	0.078	0.113	0.506	0.526	0.570	31.9	0.0457	0.0007
	038	0.096	490	0.79	0.052	0.046	0.046	0.018	0.206	0.083	0.120	0.501	0.522	0.558	32.3	0.0481	0.0008
	100	0.111	51	0.9	0.060	0.053	0.053	0.018	0.231	0.092	0.136	0.499	0.521	0.555	33.2	0.0535	0.0008
	128	0.113	533	2 0.92	0.061	0.054	0.054	0.018	0.243	0.097	0.142	0.499	0.521	0.553	32.6	0.0561	0.0009
	167	0.123	55	1 1.01	0.066	0.060	0.059	0.019	0.260	0.104	0.152	0.495	0.517	0.549	33.3	0.0597	0.0009
	229	0.136	58	1.11	1 0.073	0.065	0.064	0.016	0.284	0.115	0.167	0.497	0.518	0.549	33.3	0.0656	0.0010
	289	0.150	608	3 1.22	0.080	0.072	0.068	0.016	0.316	0.127	0.186	0.499	0.520	0.551	33.0	0.0717	0.0011
	360	0.168	642	2 1.37	7 0.089	0.081	0.074	0.017	0.354	0.141	0.208	0.500	0.521	0.556	32.9	0.0791	0.0013
3	397	0.177	655	9 1.45	0.094	0.085	0.076	0.017	0.372	0.148	0.219	0.506	0.525	0.574	32.3	0.0831	0.0013
	475	0.196	69	5 1.60	0.104	0.094	0.080	0.018	0.409	0.165	0.241	0.509	0.528	0.582	32.2	0.0918	0.0015
	484	0.199	70	1.62	2 0.105	0.096	0.081	0.018	0.418	0.167	0.246	0.511	0.531	0.570	32.3	0.0929	0.0015
	518	0.209	71	5 1.71	0.111	0.101	0.082	0.018	0.440	0.175	0.259	0.512	0.532	0.572	32.3	0.0968	0.0015
	591	0.230	75	1 1.88	0.121	0.111	0.085	0.019	0.482	0.192	0.284	0.514	0.534	0.582	32.3	0.1056	0.0017
	645	0.246	77	3 2.0	0.129	0.119	0.087	0.019	0.512	0.205	0.303	0.515	0.535	0.581	32.3	0.1123	0.0018
2	677	0.260	79	1 2.12	0.136	0.125	0.089	0.019	0.537	0.213	0.316	0.516	0.536	0.587	32.3	0.1163	0.0018
	739	0.276	82	1 2.25	0.145	0.133	0.089	0.020	0.571	0.229	0.338	0.518	0.537	0.585	32.3	0.1244	0.0020
	777	0.288	83	2.35	0.151	0.139	0.090	0.019	0.598	0.239	0.354	0.519	0.538	0.585	32.3	0.1294	0.0020
	831	0.305	864	4 2.49	0.160	0.147	0.090	0.019	0.632	0.253	0.375	0.520	0.539	0.588	32.3	0.1367	0.0022
	885	0.327	89	2.67	7 0.170	0.157	0.091	0.019	0.670	0.268	0.397	0.520	0.540	0.590	32.3	0.1442	0.0023
	938	0.344	91	5 2.8	0.179	0.165	0.092	0.020	0.711	0.283	0.422	0.521	0.541	0.583	32.3	0.1518	0.0024
1 1	996	0.362	942	2.96	0.188	0.174	0.092	0.019	0.748	0.301	0.444	0.522	0.541	0.585	32.2	0.1603	0.0025

Figure 21: Example of Analysis Spreadsheet

After the analysis spreadsheet has been completely filled in, a chart was created in Microsoft Excel to describe the flow rate as a function of pressure drop per unit length. The "Scatter with only Markers" type of chart was used for the analysis. The first data series contains data in IP units with the flow rate plotted on the x-axis and the pressure drop plotted on the y-axis. The second data series contains the data in SI units. The flow rate values were input on the x-axis and the pressure drop values were included on the y-axis. A set of dual unit axes was then established. The IP axes were set with the x-axis labeled as "CFM" and the y-axis labeled "H<sub>2</sub>O/100 ft." A second set of axes was established in the SI units with the upper x-axis labeled as "L/s" and the right side y-axis labeled as "Pa/m". The chart was placed in a separate worksheet within the spreadsheet. It was necessary to plot the second data series onto a secondary set of axes to create a dual unit chart. The process was as follows:

#### 1. Select the second data series.

- 2. Under format data series options, select the data to be plotted on the secondary axis. This introduces another vertical axis on the right side of the chart. This axis was named "Pa/m".
- 3. Add another horizontal axis to the chart. This axis is displayed at the top of the chart. The name of this axis will be "L/s".
- 4. Change the secondary axes' value range to match that of the primary axes' values. For the vertical axis, right click on the axis and select "format axis." In the option windows, change the minimum and maximum values to be the minimum and maximum values of the primary axis multiplied by the appropriate conversion factor. Select the option that the horizontal axis crosses at the maximum axis value.
- 5. Repeat step 4. for the secondary horizontal axis.
- 6. Select the second data series. In the data series options, select the options for the line and markers to be none. This will "hide" the secondary data series as it will overlap the primary data series.
- 7. Trend the data to show the relationship between flow rate and pressure drop. Select the primary data series, right click to bring up the options menu and select "add trend line." In the add trend line window, select the trend type to be "Power" and select the option to display the equation on the chart. Once the trend line is plotted, right click on the trend line equation and select "format trend line label." In the "numbers" category, select "scientific" and set the decimal places to four. This trend line equation gives the relationship in a mathematical

form of Δp=C\*Q<sup>n</sup>. In this equation, Δp refers to the pressure drop, C is a coefficient, Q is the flow rate, and n is an exponent. The value for n is assumed to be 2, but it fluctuates in actual applications. Figure 22 shows an example of the chart plotting the relationship between flow rate and pressure drop. Tables 5, 6 and 7 in Appendix A provide the approximated equation of the data for all duct sizes and compression ratios. The table also provides the coefficient of determination or "R-squared" value for each equation. This value shows how "well" the curve fits the actual data.

8. The analysis spreadsheet is saved into a new folder entitled "Analysis."

This process was repeated until each compression ratio was analyzed and charted. The analysis data for each compression ratio was then plotted on the same graph to allow for comparison of each compression ratio. A new spreadsheet was created to plot the data together in a single chart. The spreadsheet's first two rows consist of the same conversion factors as in the individual compression ratio analysis spreadsheet. The rest of the spreadsheet consists of the analyzed data from each tested duct setup. The first set gives the rigid duct data. The next set gives the maximum stretched flexible duct data. The remaining sets of data give the 4%, 15%, 30% and 45% compression ratio data. All of the data sets are presented in both IP and SI units. Figure 23 shows an example of the spreadsheet.

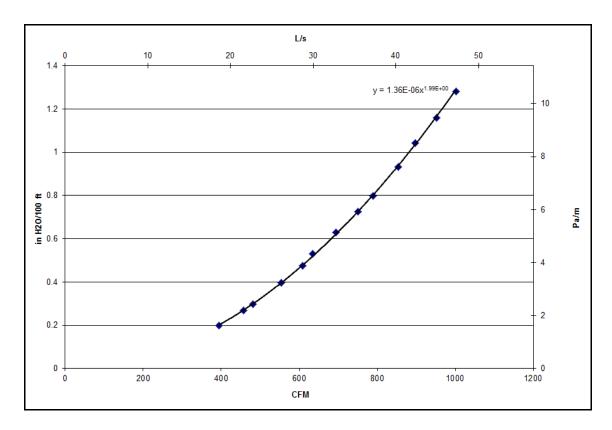


Figure 22: Example of Analysis Chart

1	in H2O/100 ft	=	8.164	Pa/m												
1	CFM	=:	0.4719	L/s												
	Rigid							Max								
						Board		0.000		Joist						
CFM	in H2O/100 ft	L/s	Pa/m		CFM	in H2O/100 ft	L/s	Pa/m	CFM	in H2O/100 ft	L/s	Pa/m				
389	0.044	184	0.36		413	0.047	195	0.39	412		194	0.42				
454	0.055	214	0.45		453	0.054	214	0.44	452		213	0.48				
489	0.062	231	0.51		506	0.068	239	0.55	510		241	0.57				
557	0.075	263	0.61		531	0.076	251	0.62	538		254	0.69				
605	0.090	285	0.73		598	0.095	282	0.77	598		282	0.82				
647	0.098	305	0.80		639	0.102	302	0.83	647		305	0.95				
690	0.114	326	0.93		701	0.133	331	1.09	691		326	1.12				
759	0.120	358	0.98		742	0.133	350	1.09	755		356	1.24				
803	0.145	379	1.19		774	0.144	365	1.18	801		378	1.54				
847	0.168	400	1.37		856	0.186	404	1.52	836		395	1.64				
895	0.184	422	1.50		895	0.100	422	1.70	896		423	1.90				
946	0.203	446	1.65		938	0.203	443	1.90	934		441	2.07				
1005	0.229	474	1.87		997	0.254	470	2.07	986		465	2.25				
1005	0.223	414	1.07		331	0.234	410	2.01	300	0.215	400	2.23				
	Board			1%	Jo	ist				Board		15	%	Joist		
CFM	in H2O/100 ft	L/s	Pa/m	CFM	in H2O/100 ft	L/s	Pa/m		CFM	in H2O/100 ft	L/s	Pa/m	CFM	in H2O/100 ft	L/s	Pa/m
396	0.068	187	0.55	367	0.059	173	0.48		390		184	0.68	402		190	0.7
445	0.085	210	0.69	448		211	0.72		437		206	0.84	438		207	0.9
483	0.096	228	0.78	494		233	0.83		487		230	1.12	475		224	1.1
529	0.120	250	0.98	540		255	0.99		570		269	1.52	542		256	1.4
607	0.160	286	1.30	592		279	1.27		617		291	1.76	595		281	1.7
632	0.164	298	1.34	638	0.167	301	1.36		636		300	1.88	648		306	2.0
706	0.211	333	1.72	717	0.211	338	1.72		686		324	2.17	685		323	2.2
770	0.249	363	2.03	760		359	1.88		750		354	2.61	742		350	2.6
808	0.282	381	2.30	806	0.230	380	2.23		808		381	3.10	802		378	3.1
865	0.329	408	2.69	831	0.273	392	2.30		840		396	3.36	846		399	3.5
917	0.343	433	2.80	917	0.202	433	2.76		891		420	3.76	886		418	3.8
952	0.343	433	3.13	917		450	3.10		942		445	4.21	939		443	4.3
999	0.421	471	3.44	1012		478	3.43		992		468	4.21	994		469	4.8
333	0.421		5.44	1012	0.421	-110	5.45		332	0.571	400	4.00	334	0.555	403	7.0
			3	10%								45'	%			
	Board				Jo	ist				Board				Joist		
CFM	in H2O/100 ft	L/s	Pa/m	CFM	in H2O/100 ft	L/s	Pa/m		CFM	in H2O/100 ft	L/s	Pa/m	CFM	in H2O/100 ft	L/s	Pa/m
383	0.122	181	1.00	406	0.150	192	1.23		394		186	1.64	389	0.207	184	1.6
437	0.162	206	1.32	458	0.189	216	1.55		458		216	2.20	442		209	2.1
492	0.202	232	1.65	493	0.220	233	1.80		481		227	2.44	494		233	2.5
533	0.244	252	1.99	551	0.279	260	2.28		554		261	3.23	525		248	3.0
611	0.324	288	2.64	605	0.336	285	2.74		609		287	3.89	587		277	3.
647	0.364	305	2.97	651	0.389	307	3.18		634		299	4.34	651		307	4.5
692	0.414	327	3.38	702	0.462	331	3.77		695		328	5.15	695		328	5.
729	0.465	344	3.80	733	0.510	346	4.16		751		354	5.93	737		348	5.
793	0.552	374	4.51	809	0.626	382	5.11		790		373	6.53	803		379	6.
829	0.606	391	4.95	843	0.671	398	5.48		854		403	7.62	852		402	7.
899	0.720	424	5.88	886	0.746	418	6.09		898		424	8.52	897		423	8.
953	0.802	450	6.55	957	0.746	452	7.15		952		449	9.46	952		449	9.
987	0.864	466	7.05	982		463	7.15		1002		443	10.47	987		466	10.5
301	0.004	400	1:05	302	0.919	403	1.51		1002	1.203	413	10.47	301	1.207	400	10.

Figure 23: Example of Multiple Series Analysis Spreadsheet

The complete sets of data are then plotted in a new chart. The process for setting up the chart is similar to the setup of the individual compression ratio chart. The chart type remains the "Scatter with Straight Lines and Markers" chart type. For each of the flexible duct data sets, the 45% compression plotted data is the data in SI units. The primary axes names stay the same as before. For this chart, the legend was placed at the bottom of the chart. Every flexible duct data set was selected and chosen to be plotted on the secondary axes. The secondary axes' names are the same as the individual

graph's secondary axes' names. As with the previous chart discussed, the scale of both secondary axes needs to be converted to the correct minimum and maximum compared to the primary axes. This spreadsheet was saved into a new subfolder under the folder of the corresponding duct diameter. Figure 24 shows an example of the chart.

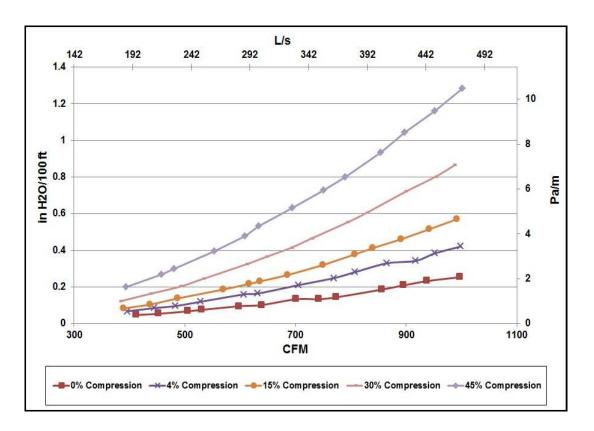


Figure 24: Example of Multiple Series Analysis Chart

## **CHAPTER IX**

# NON-METALLIC FLEXIBLE DUCT COMPRESSION EXPERIMENTAL RESULTS\*

The results of this study are presented as the static pressure drop across the tested duct as a function of the flow rate for each of the three duct sizes tested. The static pressure loss through a rigid sheet metal duct is given as a baseline for comparison in each of the graphs with pressure loss of flexible ducts of the same diameter. The testing consisted of the following six configurations: rigid sheet metal, maximum stretched flexible duct, 4% (natural) compressed flexible duct, 15% compressed flexible duct, 30% compressed flexible duct, and 45% compressed flexible duct. The test flow rates for each configuration were developed based on manufacturer recommendations. Each comparison chart shows both the board supported and joist supported results for each flexible duct compression. Figures 25, 26 and 27 each illustrate the variation in pressure loss as a function of flow rate for a given duct diameter; while Figures 28 through 33 illustrate the relationship between pressure loss and flow rate for a given duct compression.

<sup>\*</sup>Part of data reported in this chapter is reprinted with permission from "Pressure Losses in 12", 14" and 16" Non-Metallic Flexble Ducts with Compression and Sag" C. Culp and D. Cantrill, 2009. *ASHRAE Transactions*, V. 115, Pt. 1. Copyright 2009 by ASHRAE.

# **Duct Size Comparisons**

The 12" duct size was tested for flow rates between 400 cfm and 1000 cfm.

Figure 25 gives the results of the compression configuration testing for the 12" duct. At 400 cfm, the static pressure loss for 45% compressed, joist supported duct was 3.5 times greater than the static pressure loss of the maximum stretched duct. At 1000 cfm, the static pressure loss for the 45% compressed joist supported duct is over 4 times the static pressure loss as compared to the maximum stretched configuration.

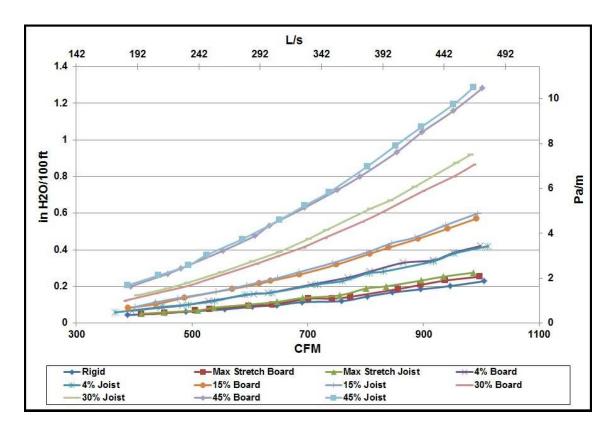


Figure 25: 12" Duct Results

The 14" duct size was tested at air flows from 500 cfm to 1500 cfm. Figure 26 shows the comparison of compression ratios for the 14" duct. The static pressure loss at 500 cfm for 45% compressed joist supported duct was over 4.2 times the static pressure loss for the maximum stretched duct. At 1500 cfm, that difference in magnitude increased to over 4.7 times.

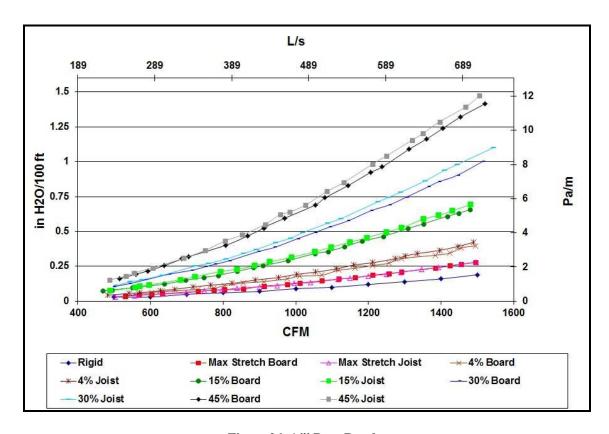


Figure 26: 14" Duct Results

The testing for the 16" duct was performed at an air flow rate range of 1000 cfm to 2000 cfm. The 16" duct testing results are presented in Figure 27. The 45% compression data for this duct size consists of two different configurations. The first configuration used three sections of flexible duct to comply with the minimum test length of 25 duct diameters as required by ASHRAE 120-1999. All other tests performed on this duct size used only two sections. After performing the test and analyzing the data, the 45% compression static pressure results were less than the 30% compression static pressure results.

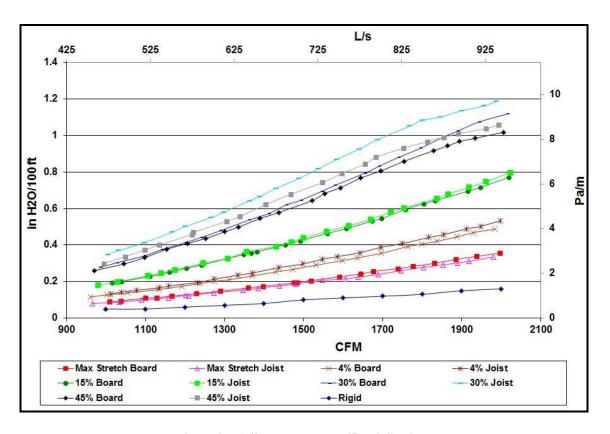


Figure 27: 16" Duct Results - 45% 3-Sections

The 45% compression test was repeated using two flexible duct sections which does not meet the ASHRAE 120-1999 requirements for duct length. In the new test, the 45% compressed duct results were greater than the compressed duct results for the 3 section tests. It was observed that they were still lower than those of the 30% compressed duct results. The pressure drop of the 45% compressed, joist supported duct was over 5.2 times the static pressure loss of the maximum stretched duct at 1000 cfm. At 2000 cfm, the static pressure drop of the 45% compression, joist supported duct was over 4 times the maximum stretched duct. The cause of this issue was not determined during this study. Figure 28 shows the results of all tests using two sections.

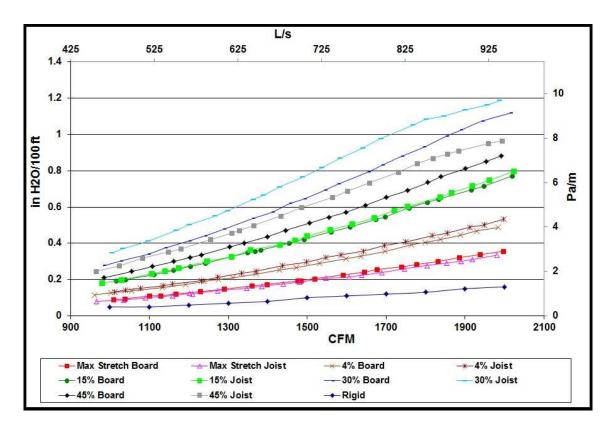


Figure 28: 16" Duct Results - 45% 2-Sections

## **Compression Comparisons**

For this comparison, the results of the maximum stretch flexible duct tests are shown for each duct size. It can be seen that the pressure drop for each flow range is similar between the three duct sizes. The difference comes from the flow ranges. As the duct size increases, the flow rate range increases to maintain the same pressure drop. Figure 29 shows the comparison of the maximum stretch configurations for each duct size.

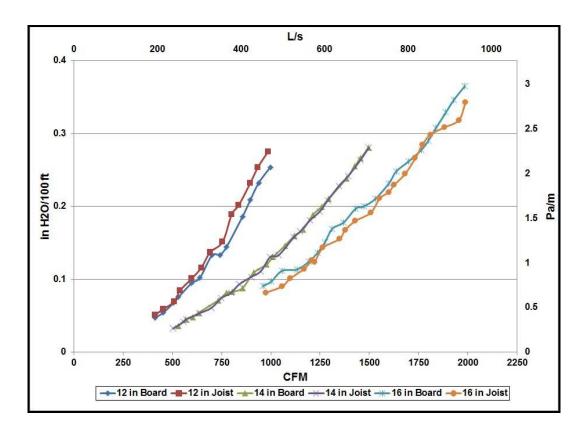


Figure 29: Maximum Stretch Results

As with the maximum stretch results, the 4% compression results show a similar pattern with the pressure loss being roughly similar between the tests. Figure 30 shows the comparison of the 4% compression configurations.

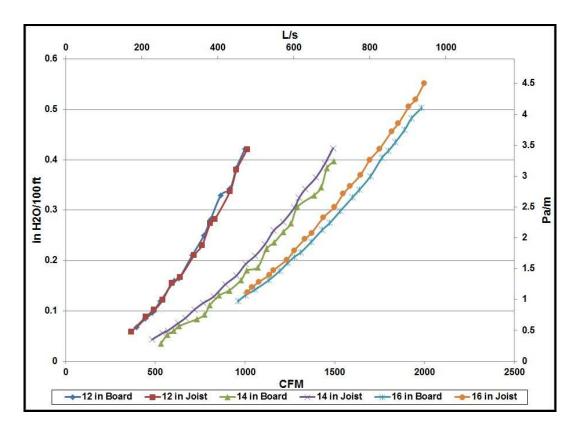


Figure 30: 4% Compression Results

The 15% compression results show a continuation in the pressure loss pattern shown in previous compression comparisons. Figure 31 shows the 15% compression comparison.

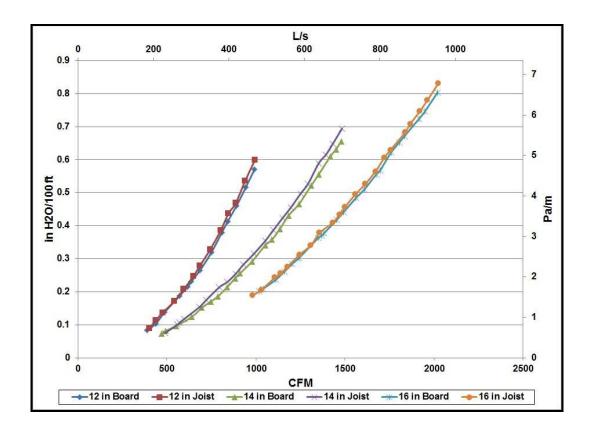


Figure 31: 15% Compression Results

The pressure loss pattern continues to be seen in the 30% compression comparisons. Figure 32 shows the 30% compression comparison.

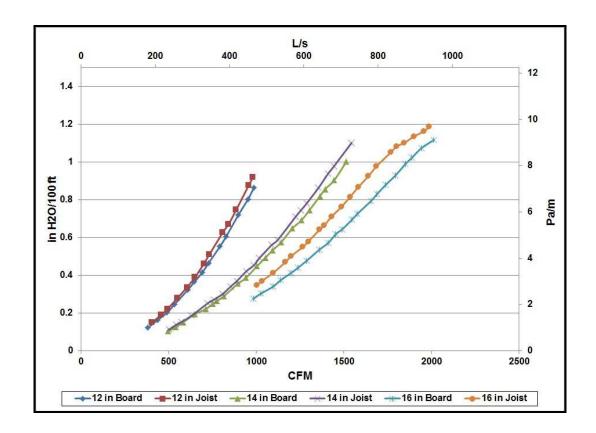


Figure 32: 30% Compression Results

For the final compression comparison, the pressure loss pattern continues to be present and is consistent with the previous compression comparisons. Figure 33 shows the 45% compression comparison.

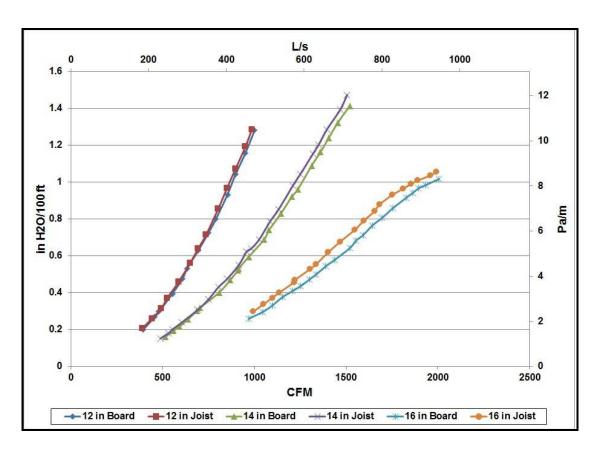


Figure 33: 45% Compression Results

## **CHAPTER X**

#### **ERROR ANALYSIS**

Potential errors in this study arise from multiple sources including sensor inaccuracies, excessive air leakage in system, compression irregularities, random error and various other sources. Multiple measures were undertaken during the design, setup and data collection phases in an effort to minimize errors in the study.

For sensor accuracy error minimization, all sensors selected to be used in the test setup had an accuracy of no greater than 2% of full scale. Relevant specifications for all the sensors utilized in this study can be found in Table 1. All sensors came with NIST-traceable calibration certificates. An analysis of the sensor accuracies was performed to review their contribution to the errors in the data.

The following inputs were utilized in the analysis:

 $\Delta P_{noz}$  Measured pressure differential across nozzle board (in  $H_2O$ ) (Pa)

Sensor accuracy – 0.5% FS

Sensor error -  $\pm .0025$  in H<sub>2</sub>O

 $T_{db}$  Dry bulb temperature determined by average of  $T_1$  and  $T_2$ . (°F) (°C)

Sensor accuracy – 0.3% FS

Sensor error -  $\pm 0.6$ °F

Pb Barometric pressure collected from weather data from Easterwood

Airport (in-Hg) (kPa)

Sensor accuracy – unknown

Assumed sensor error – 1 in-Hg

 $T_{wb}$  Wet bulb temperature determined using pyschrometric properties of air using dry bulb temperature and relative humidity (°F) (°C) Sensor accuracy – Based upon error of humidity sensor – 2% FS Sensor error -  $\pm 1.6$ °F

T<sub>amb</sub> Ambient temperature of testing area at time of test. (°F) (°C)

Sensor accuracy - 0.3% FS

Sensor error -  $\pm 0.6$ °F

 $P_{noz1}$  Static pressure prior to nozzle board. (in  $H_2O$ ) (Pa)

Sensor accuracy – 0.5% FS

Sensor error -  $\pm .0025$  in H<sub>2</sub>O

Applying these sensor errors to the input values in the Flow Calculator Spreadsheet presented in Chapter 4, minimum and maximum CFM error is found. These CFM values are then inputted into the curve-fit approximation equations to find maximum and minimum pressure drop per 100 ft. The differences between the maximum pressure drop and the measured press drop and the minimum pressure drop and the measured pressure drop are found. These values are then divided by the measured pressure drop to find the estimated error. For all of the data collected over all compressions and duct sizes, the maximum calculated error was never greater than  $\pm 3.8\%$ . The largest observed pressure loss in any of the tested configurations was 1.47 in  $\rm H_2O/100$  ft. which corresponds to a calculated error of 0.056 in  $\rm H_2O/100$  ft.

Error potential from excessive air leakage was minimized by performing total system air leakage tests prior to data collection. This process was previously detailed in Chapter 7 – Test Methodology.

To minimize the potential impact of random error during the data collection phase, the DAQ board registers values for each sensor based upon the individual sensor's response time as shown in Table 3. For each flow rate, the DAQ board reports values every second for a total of 50 seconds. The average of these 50 values provides the data points used in the data analysis.

It is believed that the majority of the error in this study fell into the category of compression irregularities. As discussed earlier, the amount of compression in the ductwork was based upon the length of duct at a maximum stretch position. For a 30 foot maximum stretch piece of flexible duct, the length of the flexible duct after 45% compression was 16.5 feet. Approximate uniformity of the flexible duct's vapor barrier along the length of the compressed ductwork was observed during the setup. Unfortunately, there was not a way to verify the uniformity of the single-helix duct liner. This uncertainty in the uniformity of the interior duct liner leads to variations in repeatability and the potential for error in the testing.

## **CHAPTER XI**

#### COMPARISON WITH PREVIOUS WORK

#### Lawrence Berkeley National Laboratory (LBNL) Research

Research performed at Lawrence Berkeley National Laboratory (LBNL) examined the effects of compression on the static pressure loss in flexible duct (Abushakra et al., 2004)<sup>3</sup>. This research utilized a draw-through configuration to test compression ratios of maximum stretch, 15% and 30%. This research tested these compression ratios for 6", 8" and 10" duct diameters. Due to the tested duct sizes and the draw-through configuration, the data from LBNL and this study cannot be directly compared. Review of the results for the three compression ratios tested at LBNL provide evidence for increased pressure loss with increasing compression ratio, which was consistent with the results of this study.

## Texas A&M University Research

Research performed at Texas A&M University also examined the effects of compression on static pressure loss in flexible duct (Weaver and Culp, 2007)<sup>25</sup>. Two main differences in this research as compared to the LBNL research are the use of a blow-through configuration in place of a draw-through configuration and the addition of two compression ratios (4% and 45%). The setup and compression ratios in this previous Texas A&M research is similar to the setup and compression ratios of this study. Because this previous research also utilized the three smaller duct diameters, direct comparison of results could not be performed. As with the LBNL research, review

of the data from the Texas A&M research also shows increased pressure loss at increased compression ratios.

# **Trane Ductulator** (Trane Co. 1976)<sup>20</sup>

The data from this study was also compared to the values included in a Trane ductulator, which is commonly used in industry. The ductulator uses inputs of flow rate and duct size to calculate estimated static pressure loss. Compression of ductwork was not a variable in the most ductulators. Based upon the data from this study and the study by Kevin Weaver, recent ductulators have incorporated some flexible duct compression as a variable. Excessive errors are possible when using this method for flexible duct design due to its inability to account for the duct compression ratio. Table 4 compares the ductulator values with data from this study at representative flow rates along with an error factor. Error between the ductulator values and the measured values is determined using the following equation:

$$Error = \frac{\Delta P_{Measured}}{\Delta P_{Ductulator}} \tag{11.1}$$

**Table 3: Ductulator Comparison** 

	Flow	Maximum Stretch	4% Compression	15% Compression	30% Compression	45% Compression
	CFM	in H <sub>2</sub> O				
Ductulator						
12"	500			0.055		
14"	800			0.064		
16"	1200	0.070				
Measured						
12"	500	0.068	0.106	0.139	0.216	0.320
14"	800	0.083	0.117	0.194	0.280	0.409
16"	1200	0.133	0.178	0.279	0.408	0.402
Error						
12"	500	1.236	1.927	0.527	3.927	5.818
14"	800	1.297	1.828	3.031	4.375	6.391
16"	1200	1.900	2.543	3.986	5.829	5.743

## **CHAPTER XII**

#### DEVELOPMENT OF PRESSURE DROP CORRECTION FACTORS

The currently accepted method to determine the pressure loss through flexible duct includes estimating the compression amount and applying a correction factor for the flexible duct. This method can be found in the ASHRAE Handbook of Fundamentals (ASHRAE, 2009)<sup>7</sup>. The results of this research are intended to provide additional information to be incorporated into this current methodology.

Research performed at LBNL (Abushakra et al., 2004)<sup>3</sup> developed correction factors for 6", 8" and 10" duct diameters for compression ratios of maximum stretch, 15% and 30%. This research will add correction factors for 12", 14" and 16" duct for the five compression ratios tested.

The first step in the development of pressure drop correction factors (PDCF) for this study was to develop power-law models for each compression ratio for each duct size. This was done by plotting the pressure loss per 100 ft. values versus their corresponding flow rate. Once all values of pressure loss versus flow rate at plotted for a given compression ratio, a power equation trend line is mapped onto the plotted data. This trend line's equation represents the power-line model for the given compression and duct size. The power-line model can be utilized to estimate the pressure loss per 100 ft. for a given flow rate and is characterized by the following general equation:

$$P = C * Flow^n (12.1)$$

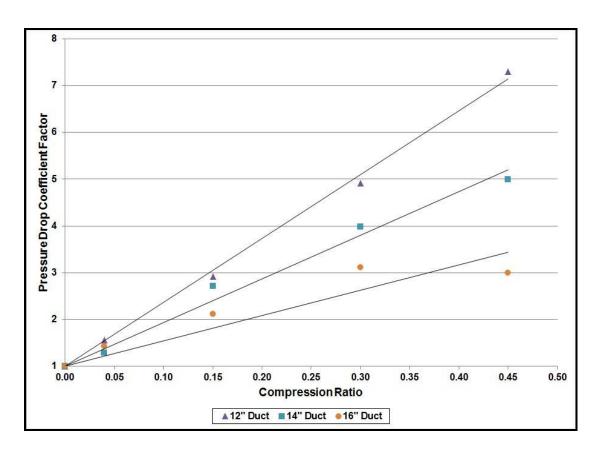
The equation contains a coefficient of C, the flow rate in CFM, and an exponent, n. The value of the exponent (n) is typically assumed to be two. In actual applications, this value fluctuates around the value of two.

Once these equations are determined, they can be used to develop the PDCF.

The PDCF is a multiplier which can be used to estimate the static pressure loss in flexible duct under compression. The PDCF is calculated, for a given flow rate, as the ratio of the compressed pressure loss to the maximum stretched pressure loss:

$$PDCF = \frac{\Delta P}{\Delta P_{MS}} \tag{12.2}$$

where  $\Delta P$  is the pressure loss at a particular compression and  $\Delta P_{MS}$  is the pressure loss at a maximum stretched position. For this study, a representative flow rate was chosen for each duct size to develop the PDCFs for each compression ratio. For 12" duct, the PDCFs were developed based upon a flow rate of 400 cfm. For 14" duct, the PDCFs were developed based upon a flow rate of 600 cfm. For 16" duct, the PDCFs were developed based upon a flow rate of 1000 cfm. Figure 34 shows the PDCFs developed in this study. These PDCFs were incorporated into the existing PDCFs in the ASHRAE Handbook of Fundamentals (ASHRAE, 2009)<sup>7</sup>.



**Figure 34: Pressure Drop Correction Factors** 

## **CHAPTER XIII**

#### **DISCUSSION**

The results from this study demonstrate the importance of proper installation of non-metallic flexible duct in actual applications. The compression of flexible duct has the potential to increase the duct static pressure loss by as much as five times that of fully stretched duct. This demonstrates that proper installation of duct systems becomes just as important as duct system design.

A factor that was found to affect the amount of pressure drop was the geometric configuration of the duct. Industry standards call for the duct to be installed straight. Any amount of change in the duct from being completely straight will increase the pressure loss through the duct. A straight duct introduces the air flow to the minimal amount of surface area. Any change in that path of air flow results in exposure to greater interior surface areas. The compression amount changes the effective diameter of the duct. With an increase in compression ratio comes a decrease in the diameter that the air flow encounters. This decrease in diameter directly increases the static pressure loss. This effect is less noticeable in larger duct diameters as compared to smaller duct diameters.

The compression of the flexible duct creates small pockets in the geometry of the inner duct between the metal wire helix. The air flow into these pockets can create vortices within the air stream which causes greater turbulence in the air flow. This increase in turbulence within the air stream results in increased pressure loss in the duct.

#### **CHAPTER XIV**

### CONCLUSIONS

This research collected static pressure loss values for various compression configurations for 12", 14", and 16" non-metallic flexible duct. Conclusions gathered from this research are as follows:

- 1. Installation of non-metallic flexible duct in straight run configurations should be as close to a fully stretched manner as possible. If the flexible duct cannot be installed fully stretched, it should have no greater than 4% compression as set forth in the installation instructions by the ADC (ADC 2003)<sup>5</sup>.
- 2. For duct compression greater than 4%, flexible duct can have pressure drops four to ten times the pressure drop in rigid sheet metal ducts.
- 3. Flexible duct installed at compressions greater than 4% demonstrate potential for decreased airflow and system performance in commercial HVAC systems.
- 4. Any time flexible duct is utilized in a HVAC system, the duct should be properly sealed using the methods specified by the ADC. Proper sealing of the ductwork will reduce the amount of air leakage in the system which will in turn lower the supply fan usage in the HVAC system.

## **REFERENCES**

- 1. Abushakra, B., D. Dickerhoff, I. Walker and M. Sherman. 2001. Laboratory Study of Pressure Losses in Residential Air Distribution Systems. *Lawrence Berkeley National Laboratory Report LBNL-49293*, Berkeley, CA.
- 2. Abushakra, B., D. Dickerhoff, I. Walker and M. Sherman. 2002. A Study of Pressure Losses in Residential Air Distribution Systems. *Proceedings of the ACEEE Summer Study 2002*, American Council for an Energy Efficient Economy, Washington, D.C., *Lawrence Berkeley National Laboratory Report LBNL-49700*, Berkeley, CA.
- 3. Abushakra, B., I. S. Walker, M. H. Sherman. 2004. Compression Effects on Pressure Loss in Flexible HVAC Ducts. *International Journal of Heating*, *Ventilating, Air-Conditioning and Refrigeration Research*, V. 10 (3), pp. 275-289.
- 4. ACCA. 2009. *Residential Duct Systems. Manual D.* Air Conditioning Contractors of America, Washington, DC.
- 5. ADC. 2003. Flexible Duct Performance and Installation Standards, 4<sup>th</sup> Edition. Air Diffusion Council, Shaumburg, IL.
- 6. Altshul, A.D. and P.G. Kiselev. 1975. *Hydraulics and Aerodynamics*. Stroisdat Publishing House, Moscow, USSR.
- 7. ASHRAE. 2009. *ASHRAE Handbook of Fundamentals*. American Society of Heating, Refrigerating and Air-Conditioning Engineers, Atlanta, GA.

- 8. ASHRAE. 1999. ASHRAE Standard 120, Methods of Testing to Determine Flow Resistance of HVAC Air Ducts and Fittings, June 1999. American Society of Heating, Refrigerating and Air-conditioning Engineers, Atlanta, Georgia.
- 9. ASHRAE. 1986. ASHRAE Standard 42.1, Standard Method for Temperature Measurement, June 1986. American Society of Heating, Refrigerating and Air-Conditioning Engineers, Atlanta, GA.
- 10. ASHRAE. 1987. ASHRAE Standard 42.2, Standard Methods for Laboratory Airflow Measurement, June 1987. American Society of Heating, Refrigerating and Air-Conditioning Engineers, Atlanta, GA.
- 11. ASHRAE. 1989. ASHRAE Standard 42.3, Standard Method for Pressure Measurement, January 1989. American Society of Heating, Refrigerating and Air-Conditioning Engineers, Atlanta, GA.
- 12. Bricker, E.J. 1961. Field Checking and Testing of Ventilation and Air Conditioning Systems, *ASHRAE Journal*, May, pp. 10-72
- 13. Fellows, J.R. 1939. Power Savings through Static Pressure Regain in Air Ducts, *HPAC*, V.11 (4) pp. 219-222
- 14. Graham, J.B. 1996. Duct System Pressure Gradient Diagrams and the Beer Cooler Problem, *Heating, Piping and Air Conditioning*, August, pp. 63-66, 80. 15. Harrison, E. 1965. Balancing Air Flow in Ventilating Duct Systems, *IHVE Journal*, V. 33, pp. 201-226

- 16. Kokayko, M., J. Jolton, T. Beggs, S. Walthour, and B. Dickson. 1996. Residential Ductwork and Plenum Box Bench Tests. *IBACOS Burt Hill Project 95006.*-13. Pittsburgh, PA
- 17. Moody, L.F. 1944. Friction Factor for Pipe Flow. *ASME Transactions*, Vol. 66, pp. 671-678.
- 18. Scott K.B., 1986. Don't Ignore Duct Design for Optimized HVAC Systems, *Specifying Engineer*, No. 62, January, 1986.
- 19. Shieh Chun-Lun. 1983. Simplified Static-Regain Duct Design Procedure, *ASHRAE Transactions*. V.89 (2a), pp. 78-94.
- Trane Company. 1976. Explanation of the Trane Air Conditioning Ductulator.
   Product Explanation. Trane Co, Carrollton, TX.
- 21. Tsal, R.J. and H.F. Behls, 1986. Evaluation of Duct Design Methods. *ASHRAE Transactions*, Vol. 92 (1A), pp. 347-361.
- 22. Tsal, R.J. and H.F. Behls. 1988a. Fallacy of the Static Regain Duct Design Method, *ASHRAE Technical Data Bulletin*, ASHRAE, Atlanta, GA
- 23. Tsal, R.J., H.F. Behls, and R. Mangel 1988b. T-Method Duct Design Part I: Optimization Theory *ASHRAE Transactions*, V. 92, Part 1A
- 24. Tsal, R.J. 1989. Altshul-Tsal Friction Factor Equation. *Heating, Piping and Air Conditioning*, July, 1989.
- 25. Weaver, K., and C. Culp. 2007. Static Pressure Loss in Nonmetallic Flexible Duct, *ASHRAE Transactions*, V. 113, Part 2.

# **APPENDIX A**

**Table 4: 12" Duct Equations** 

Compression Test	Equation	R-squared Value	
Max Stretch Board	Δp = 4.19e-7*(Q^1.93)	0.996	
Max Stretch Joist	Δp = 2.96e-7*(Q^1.99)	0.996	
4% Board	Δp = 4.47e-7*(Q^1.99)	0.999	
4% Joist	Δp = 6.93e-7*(Q^1.92)	0.998	
15% Board	Δp = 3.84e-7*(Q^2.06)	0.999	
15% Joist	Δp = 4.06e-7*(Q^2.06)	0.999	
30% Board	Δp = 5.59e-7*(Q^2.07)	1	
30% Joist	Δp = 5.93e-7*(Q^2.07)	1	
45% Board	Δp = 1.36e-6*(Q^1.99)	1	
45% Joist	Δp = 1.45e-6*(Q^1.99)	1	

**Table 5: 14" Duct Equations** 

Compression Test	Equation	R-squared Value	
Max Stretch Board	Δp = 2.09e-7*(Q^1.93)	0.998	
Max Stretch Joist	Δp = 1.96e-7*(Q^1.94)	0.999	
4% Board	Δp = 1.96e-7*(Q^1.99)	1	
4% Joist	Δp = 2.04e-7*(Q^1.99)	0.999	
15% Board	Δp = 4.83e-7*(Q^1.93)	0.999	
15% Joist	Δp = 3.93e-7*(Q^1.97)	0.999	
30% Board	$\Delta p = 4.09e-7*(Q^2.01)$	0.999	
30% Joist	Δp = 4.14e-7*(Q^2.02)	1	
45% Board	Δp = 5.98e-7*(Q^2.01)	1	
45% Joist	Δp = 5.70e-7*(Q^2.02)	1	

**Table 6: 16" Duct Equations** 

Compression Test	Equation	R-squared Value	
Max Stretch Board	Δp = 7.05e-8*(Q^2.03)	1	
Max Stretch Joist	Δp = 7.53e-8*(Q^2.02)	0.999	
4% Board	Δp = 1.18e-7*(Q^2.01)	0.999	
4% Joist	Δp = 9.57e-8*(Q^2.04)	1	
15% Board	Δp = 1.48e-7*(Q^2.03)	1	
15% Joist	Δp = 1.34e-7*(Q^2.05)	1	
30% Board	Δp = 2.87e-7*(Q^2.00)	0.999	
30% Joist	Δp = 9.63e-7*(Q^1.86)	0.993	
45% Board - 2 Sections	Δp = 1.73e-7*(Q^2.05)	1	
45% Joist - 2 Sections	Δp = 4.42e-7*(Q^1.93)	0.997	
45% Board - 3 Sections	Δp = 4.10e-7*(Q^1.95)	0.996	
45% Joist - 3 Sections	Δp = 8.68e-7*(Q^1.86)	0.991	